

BOOK52R

Notes:

10149 on bottom edge

Blank pages: page opposite page 1, 147, 148, inside back cover sheets

-page 111 has 2 (8.5x11) sheets stapled to it

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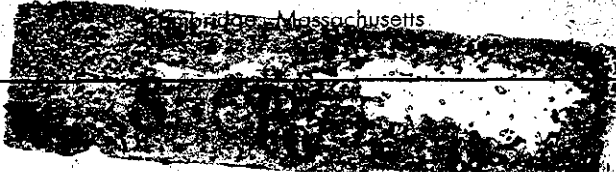
COMPUTATION BOOK

NAME	Number
F-05	24

Course *Solution Experiments #36-150* ^{*data books #2*}

Used from *11/25* 1947, to *5/12/48* 19

HARVARD COOPERATIVE SOCIETY
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SECRET

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CLASSIFICATION CANCELLED
DATE 6/3/60
For the Atomic Energy Commission
Jack H. Kahn for the
Chief, Declassification Branch

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RESTRICTED DATA

"This document consists of 154 pages.
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correct documentation
5-25-60

SECRET

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Experiment

Pg

75	10" Reactor	Tamped	$k_{eff} = 127.4$	52
76	8" "	"	$= 127.4$	53
77	8" "	Untamped	$= 127.4$	54
78	9" "	Tamped + Cd	$= 127.4$	55
79	9" "	Tamped	$= 127.4$	57
80	9" "	Untamped	$= 127.4$	58
81	7" "	Tamped	$= 127.4$	59
82	6 1/2" "	"	$= 127.4$	60
83	5 1/2" "	"	$= 175$	62
84	8" "	Untamped	"	64
85	8" "	Tamped	"	65
86	8" "	" (wept top)	"	66
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102	9" "	Tamped	"	88
103	12" "	H ₂ O tamper; Cd shielded	"	89
104	12" "	Untamped	"	90
105	12" "	Tamped	"	91
106	10" "	untamped	"	92
107	10" "	tamped	"	93
108	10" "	untamped	320	94
109	10" "	tamped	"	95
110	9" "	Cd + tamper	"	96
111	9" "	tamped	"	97
112	8" "	"	"	98
113	12" "	untamped	"	99
114	12" "	tamped	"	100
115	8" "	untamped, double wall	84 (?)	102
116	8" "	tamped	85 (?)	103
117	8" "	"	? (~300)	104
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to examine effect of moving void in reactor with 2cc source holder in solution with 60cc source in tamper

k_{eff} values very uncertain

Experiment 37

6" Reactor Tamped $H/H \approx 45$ ^{43.87}

11/25/47

Personnel: Callihan
 Cronin
 Fox
 Williams

8:00 Installation of 4" storage cylinder in place of #1 3" storage cylinder. Leak tested

9:45 Dilution of solution to $H/H \approx 45$

Broken stud on 8" reactor replaced.

11:30 Measurement of solution Heights in Storage cylinders

	# 2	# 3	# 4	# 5	# 6	# 9
	71.3	71.3	75.0	71.4	74.6	70.6
manometer	31.6	31.5	28.0	31.3	28.5	32.1
Ht.	39.7	39.8	47.0	40.1	46.1	38.5
Density	1.63	1.68	1.64	1.67	1.67	1.63
Ht. in storage cyl.	72.4	70.2	84.8	71.0	81.3	70.0
Ht. in 6" Reactor	18.1	17.5	21.2	17.7	20.3	17.5

Trip levels - #3 - 91x100; #4 - 91x100.

Instrument Scales:
 3 - 100
 4 - 10
 5 - 1
 R.E - 25mv.

1:35P Initial Counts - # I 13.5 # II 13.0

Filling dead volume from #6.

Experiment 37 (Cont)

11/23/47 1/40P H = -0.1 cm.		I	II	C/c		
		14.5	15.0	I	II	
		<u>14.5</u>	<u>14.0</u>			
1:30	H = 4.1 cm	16.5	17.5	0.88	0.83	{ #6 empty Tampers + night glass checked. Filling from #9.
1:55	= 10.1 "	25.5	25.0	0.57	0.58	
2:13	= 15.5 "	30.0	30.5	0.483	0.476	
24	= 20.5 "	33.5	35.0	0.433	0.414	#9 Empty.
34	= 27.7 "	41.5	41.0	0.350	0.354	Filling from #2
50	= 36.6 "	47.0	46.0	0.309	0.315	#2 Empty.
3:02	= 45.0 "	54.0	53.0	0.269	0.274	Filling from #3
13	= 54.7 "	57.0	59.0	0.258	0.246	#3 Empty.
29	= 64.9 "	65.5	65.0	0.221	0.223	Filling from #5
46	= 74.0 "	73.0	71.5	0.199	0.206	Filling from #4.
4:40	"	73.5	73.5			
4:40	= 0.3 "	15.0	15.0			

DRAIN	#3 - 20.1 cm in reactor	#6 = 17.2 cm in 7" reactor
#4 - 20.4 " " "	#8 = 17.4 " "	
#5 - 20.0 " " "	#9 = 17.1 " "	
#6 - 13.1 " " "	11.2 " "	
#8 - 20.0 " " "	17.1 " "	
#9 - Dead volume	-	

All solution was at sometime during this afternoon out of its storage cylinder & mixed with a quantity from other cylinders. The entire batch should now be homogeneous.

Conclusions.

6" reactor, tamped, H₁ = 45 not critical (M = 4 at H = 74 cm) & is probably infinitely safe.

$$H = 74.0 + 2.6 = 76.6 \text{ cm}$$

$$H/x =$$

Experiment 38 Nov. 26, 1947.

7" - Tamped-Cadmium, $H/X \approx 45$. ^{43.87}

Beck.
McLendon.
Quinn
Crosin.

8:20 AM Completing alignment and checking of 7" reactor.
Instrument #5 out of Commission; Quinn repairing.

12:50 PM. #5 still out; all others in good condition. Experiment to proceed. McLendon out.
Instruments checked.

Solution	Counting Rate		CpK		
	#1	#2	#1	#2	
12:52 "Background"	12.5	13.			
12:59 "Zero" 0.7 cm	13.0	12			From cyl #9
	13.0	11.5			
1:06 10.0 cm	18.5	18.0	.70	.667	From cyl #3.
1:14 20.0	24.	24	.57	.50	Cyl. 3 empty at 15. Adding from #4.
1:20 30.2	26.	25.5	.50	.47	adding from 4. Empty at 29.8 cm.
1:28 39.9	28.5	26.	.455	.46	adding from 8.
1:35 50.1	28.5	27.	.455	.445	Bothkus & McLendon came in
1:44 60.1	27.5	26.5		.4	

Drawback -
 #3 15.6
 #4 15.0
 #5 16 in #5
 #6 15.0
 #8 9.4
 #9. dead volume.

Conclusion - Will not get ∞ —
 CHB

Experiment 39 - 7" Untamped - $H/x \approx 45$

Nov. 26, 47.

43.87

Beck,
Fox
Cromin
McLendon
(Bartkus.)

Instruments checked.

	Solution Level	Counting Rate		I % \bar{I}		
		#1	#2			
2:32.	0.3 "zero"	118	109.3			
		118.5	109.0.			
	10.0.	90.5	85.0	1.3	1.27	Emptying #8
2:47	20.0	146.0	134.5	.81	.81	from #6
2:55	30.0	166.5	151.5	.70	.72	6 empty at 25; from 5. Fox departed.
3:01	40.3	172.5	159.5	.69	.69	from 5. (empty)
3:12	60.1	175.5	159.5	.685	.69	from #4, and from 3.

Drainback:

#3	15 cm.
#4	15
#5	15
#6	15
#7	
#8	9.
#9	dead volume.

11/30/48 DC.

$$H = 60.1 + 1.9 = 62.0 \text{ cm}$$

$$H/x = 43.9$$

$$\rho_{\text{app}} = 1.65$$

$$\text{wt } \rho_{\text{K}} = 32.6 \approx 0.538 \text{ g/cc}$$

$$V = 15.39 \text{ L} \quad \left. \begin{array}{l} \text{Actual} \\ \text{Measurement} \end{array} \right\}$$

$$M = 8.28 \text{ kg}$$

$$\text{Estimated } V_c = H_c = M_c = \infty$$

Conclusion: Does not go at ∞

11/28/47

NH₄/N₄ det^{SA} on

Sample from solution ~ 30 before dilution.

28

1.8110 gm sol
0.8861 gm Opicid

27

1.4253 gm sol
0.6909 gm Opicid

Calc NH₄/N₄ approx = 31.12

31.82

avg = 31.47

samples sent to analytical lab for accurate analysis.

Lab Results 12/11/47

27 wgt of U = 0.5831 gm wgt Opicid = 0.6890
N₄/N = 32.0

28 wgt of U = 0.7475 wgt Opicid = 0.8833
N₄/N = 31.39

8/21/47

Experiment 40

7" Reactor.

Tamped
 $M_{TC} = 45.43.87$

Vision
 Melendow
 Callahan

Replaced solenoid in safety rod support.*

Trip point #3 - 93x100
 *4# 90x100

3:08P Filling dead volume from #9
 3:15P $H = 0.2$ cm

I	14.5	15.0
F	14.0	14.0

Scales #3 - 100
 #4 - 10
 #5 out of order
 Read - - -

3:25P

$H = 2.9$ cm.

Tamped checks - Filling from #8.

3:27P

$H = 5.1$ cm.

19.5 19.5

I 0.732
 COTC F 0.744

3:32P

$H = 10.2$ cm

30.0 30.5

0.477 0.476

#8 empty.

39

$H = 13.5$

39.0 37.0

0.366 0.392

Filling from #6.

49

$H = 17.5$

51.5 50.5

0.277 0.287

57

$H = 21.0$

68.0 65.0

0.210 0.223

4:06

$H = 25.0$

106.5 102.5

0.134 0.141

Filling from #4

13

$H = 27.5$

158.0 153.5

0.098 0.094

24

$H = 29.5$

304.0 297.5

0.047 0.049

35

$H = 30.6$

550.5 527.0

0.026 0.028

55

$H = 31.0$

Critical with 9cm control rod below solution surface.

5:06

$H = 0.0$

14.5 16.5

Drain Cases

#3	15 cm in 7" (not used today)	= 11 cm in 8" reactor
#4	15 " " "	= " " "
#5	15 " " " (not used today)	= " " "
#6	14.7 " "	= 11 " "
#8	9.3 " "	= 7 " "
#9	Dead volume	

11/17/48 DC - $30.8 + 1.9 = 32.7$ cm = H_c
 corrected for bottom
 7" Stainless, Tamped
 $M_{TC} = 43.8743.9$
 $S_{90} = 1.65 \frac{33.6}{100} = 0.538$ gm/cc
 $M_{TC} \% = 0.222 = 0.422$ gm/cc
 $V_C = 8.12$ R
 $M_C = 3.43$ Kg. 4.37 Kg.

Conclusions -

7" reactor, tamped, $M_{TC} = 45$ critical at $H = 30.8 \pm 0.2$ cm
 Due to difficulty in aligning 7" reactor it is suggested that in future the
 two tamped experiments be done consecutively - DC 1211

* Current
 Carrying capacity of Cd rod solenoid is 4.8 amps. Current through Cd rod and
 dump valve solenoid, in parallel, each with plunger, is 3.5 amps. Therefore
 it is recommended that 5 amp fuses be used in the trip circuit.

12/47

Experiment 41

8" Reactor

$H_x = 45.87$

Temper + Cd Shielding.

Manfitt

Callahan
Crosin

Trip points #3 93x100
#4 94x100

Scales #3 - 100
#4 - 10
#5 - 1

R-E - 50 ms.

#II - out of order

c/c.

12:45P Filling from #9.

:53 H = 1.0 cm "Zero Count" #9 empty

I
14.0
12.0
13.0
14.5
15.0

1:02 H = 5.0 Filling from #8

1:10 = #8 empty

:13 = 10.2 Filling from #3

20.5
21.0

25 = 15.0

22.0
22.5

35 = 19.3

34.5

#3 empty

43 = 25.1

42.5

Filling from #5

51 = 30.9

53.0
55.0

#5 empty

2:02 = 37.6

75.5

Filling from #6.

= 0.0

13.0
12.5

0.882.

0.627

0.469

0.377

0.306

0.245

0.236

0.172

Drain: #3 - 10 cm in 8" reactor

4 - 11 cm "

5 - 10 cm in 8" reactor.

6 - 11 cm in 8" reactor

8 - 10 " " "

Conclusion: Maxima possible height maintaining temping = 37.6 cm. $M \approx 6$; Probably would go critical; Decided to repeat with 35" cylinder - to be fabricated.

12/21/47

Experiment #42

8" Reactor

$M_x = 45$ 4387

Tamped.

Cromin
Moffitt
Callahan

(Lowest pulse selector ^{level} on #II - seems ok).

Time	H =	I	II	Zero Count	Filling from #8	Scale
3:46P	0.0 cm.	16.0	13.5			#3 - 100
		15.5	14.0			#4 - 10
		15.75	13.75			#5 - 2
4:44	5.0	23.0	21.5	0.685	0.639	RE - 100 ms
4:00	8.0	35.0	30.0	0.451	0.459	
4:08	10.4	48.0	43.5	0.324	0.316	#8 Empty.
4:17	12.5	66.0	60.0	0.239	0.230	Filling from #3
4:24	15.0	103.0	95.5	0.153	0.144	
4:33	17.0	176.0	157.0	0.090	0.088	
4:44	18.0	259.0	224.0	0.061	0.060	Filling from #4
4:51	18.7	397.0	361.5	0.040	0.039	
5:05	19.0	475.5	419.5	0.033	0.033	
18	19.2 (source out)					
	19.3					Not quite critical.
30	19.3 (source out)					
33	19.5					Critical with 8 cm Cd rod below solution level.
48	0	15.5	14.0			

DRAIN BACK: #9 has dead volume -

Balance of solution is distributed in an unknown way among #3, 4, 5, 6 + 8. It is necessary to measure the solution heights in these cylinders since they were filled simultaneously when a cotton pin fell out of #4 + it could not be closed. It is suggested that better keep be provided.

Conclusions:

8" Reactor, Tamped, $M_x = 45$ - Critical at $H = 19.4 \pm 0.1$ cm.

11/1/48 $19.4 + 1.45 = 20.9 = H_c$ corrected for bottom -

$H_c = 43.87 + 3.9$

8" Stainless, Tamped.

$\rho_{\text{sol}} = 1.65$ $\rho_{\text{air}} = 0.0012$ $\rho_{\text{Cd}} = 0.538$
 $W_{\text{Cd}} = 0.226 = 0.22 \text{ gm} \times 1 \text{ cc}$

$V_c = 6.78 \text{ L}$

$M_c = 2.86 \text{ kg} \cdot 3.65 \text{ kg}$

3/3/49 adding 1 cm zero correction because of "dead" 8" cylinder -

$H_c = 21.9 \text{ cm}$

$V = 7.10 \text{ L}$

$M = 3.82 \text{ kg}$

Beck
Morfit
Cronin

27.6
4.7
32.3

8-11:30 Removing 8" cylinder; installing, adjusting 9"

Solution Levels in Storage Cylinders

# 3	4	5	6	8	9
74.4	77.2	75.9	76.6	57.7	73.1
28.4	25.7	27.0	26.4	43.5	Dead Volume. 29.5
46.0	51.5	52.9	50.2	14.2	43.6

X 17.3

80 cm	89	92.	87.	25.	76. height in 3" cyl.
-------	----	-----	-----	-----	-----------------------

X 9/81 for 9" cyl.

8.9	9.9.	10.	9.7	2.8	Dead Volume. Height in 9" cyl.
-----	------	-----	-----	-----	--------------------------------

Solution Levels	Counting Rate		C/c		Ref is Off. #3 on 100; #4 on 10; #5 on 1, Rec. Mon. O.K. Background counts on 1 and 2-
	#1	#2	#1	#2	
11:30 AM "Background"	12	11.			
	12	11.5			
	11.5				
	12	11.5			
11:55 16 cm "zero"	11.5	10.5			Dead Volume filled from #9.
12:15					#8 empty at 3.6.
12:22 10.2 cm	22	20.5	.523	.512	#6 empty at 13.8. adding from #5.
12:22 15.0	34.5	31.5	.332	.334	
	33.1	33.4			
12:30 20.0	60.0	55	.192	.191	adding from #5.
12:38 25.1	148.	132.5	.077	.079	#5 empty at 23.1. Adding from 4. #4 on 20 scale.
12:44 26.5	250	228.5	.046	.046	#5 on 5; #4 on 50 scale.
12:54 27.5	450	411.5	.025	.0256	#4 on 100 scale.
	462	415.5	.025	.025.	

11:05
12:5
27.6 Not critical, but close.
27.7 Above critical -

Drum Back-

# 3	4	5	6	8	9
8.9	10	7.6	7.6	7.6	Dead Volume.

Conclusion: Critical at 27.65 cm, ± .025

11/17/48 DC
27.65 + 1.15 = 28.8 cm Mc - Corrected for bottom -
9" Stainless Tamped and (C) shielded
 $H/\lambda = 43.87 \approx 43.9$
 $w/4\% K = 0.225 \text{ g/cm}^3 \times 1.65 \text{ cm}^3 = 0.371 \text{ g/cm}^3$
 $\Delta T = 1.65$
 $V_c = 11.82 K$
 $M_c = 4.44 \text{ kg } 6.36 \text{ kg}$

Experiment 44. - 9" Tamped. $H/x = 43.87$

2:45 Preparations ready for Tamped.

#3 on 100, #4 on 10, #5 on 2. Process monitor OK; Read out.

#3 drops out at 94 on 100, #4 at 90 on 100 scale.

Solution Levels	Counts	gk		
		#1	#2	
2:50. "zero" 0.3cm	14. 13			
	14.5 13.5			
2:55 9.0 cm.	40.5 36.0	.345	.36	From #8. Empty at 9.0
3:01 14.0	119.5 106.5	.117	.122	From #5. #4 on 20 scale.
3:12 15.5	226. 207.	.062	.061	#4 on 50, #5 on 5
3:20 16.2	412. 376.	.034	.035	
3:30 16.5	705. 650.	.0198	.020	
	717. 647.			
3:45. 16.6	Not critical; But close.			
3:50. 16.7	Critical.			

Drain Back:

#3	#4	#5	#6	#8	#9
8.9	10.	7.6	7.6	7.6	Dead Volume.

Conclusion: Critical at $16.65 \pm .05$

11/17/48 DC - $16.65 + 1.15 = 17.8$ cm He corrected for bottom -

$$H/x = 43.87 \quad 43.9$$

9" Solen less Tamped.

$$\text{at } q = 1.65 \quad 326 \quad 0.538$$

$$\text{with } q/x = 0.236 = 0.422 \text{ gm/cm}^3$$

$$V_c = 7.30 \text{ L}$$

$$M_c = 3.08 \text{ kg. } 3.93 \text{ kg.}$$

12/4/47 13

Experiment 45 9" unstamped $\frac{N_H}{N_X} \approx 45$ 43.87
 Cronin
 Morfitt
 Murray

9:00 Took samples for N_H/N_X & specific gravity*

9:15 Instruments - Scales: #3-100 #4-10 #5-2, Reed ng., process mount. etc.
 (strip 88), (strip 88)

9:40 Measurement of specific gravity: $\rho = 1.667$ for $N_H/N_X \approx 45$

Filling from	time	Soln. level	C_1	C_2	$(1/m)_1$	$(1/m)_2$	comments
#9	9:50	-3mm	98	81 (NG)			
			94.5	96			
			95.5	94			
	10:00	Filling from #8					
	10:13	7.10	70	68.5			
	10:17	9.1	89.5	89.			Red in
							Red out
	10:23	11.61	122.5	113.5	.775	.837	Filling from #6
	10:35	15.0	165.5	160.5	.574	.542	
	10:40	17.3	202.5	193	.468	.492	#6 Empty
	10:48	20.05	248	229.5	.383	.414	Filling from #3
	10:55	23.0	288.5	267.5	.3295	.355	
	11:01	27.0	357	334.5	.266	.284	
	11:10	29.4	406.5	376	.234	.253	#3 Empty
	11:18	32.8	480.0	441	.198	.215	Filling from #5
	11:23	35.7	545.5	505.5	.175	.188	#5 Empty
	11:35	37.8	615.5	565	.1545	.168	Filling from #4
	11:42	41.0	731	665	.130	.143	#4 Empty
	11:50	41.0	720	664			Check pt.
	11:53	39.5	668	607.5			Drained into #7

Drain Back:

#4	#3	#5	#6	#8.0	#9
10.0	9.0	7.5	7.5	7.0	d.v.

11/30/48
 $H = 39.5 + 1.2 = 40.7$ cm
 $H/Y = 43.9$ $S_{pp} = 1.65$
 $Wt\% Y = 32.6 = 0.538$ $\frac{g}{cc}$
 $V = 16.70$ R
 $M = 8.98$ kg
 Estimate:
 $H_c = 7.75$ cm
 $V_c = 7.31$ R
 $M_c = 7.17$ kg

Background Count

#1 100 #2 95

* 11/19/48 Data from Cronin notes:
 Dial 35 Gross 10.5111 gm
 Tare 8.9733
 Net 1.5378 gm oxide
 3.7302 gm solution.
 $H/Y = 43.79$
 Dish 24 Gross = 9.7553 gm
 Tare = 8.7138
 Net 1.0415 gm oxide from
 2.5316 gm sol
 $= H/Y = 43.96$

Conclusion: 9" unstamped cylinder, $N_H/N_X \approx 45$
 probably does not go critical at indefinite extension

Experiment #46 6 1/2" Tamped

spg. 1.667
 {43.79, 43.87} 12/4/47

Cronin
 Morrill
 Murray

2⁴⁰ Ready to go. Filling dead volume from #9

Prelim. counts 12 1/4, 12 1/4
 11 3/4, 11 3/4

Soln. Heights of Reactor Heights

#3	#4	#5	#6	#8	#9
13.6	15.2	11.3	11.3	10.6	Dead Volume

Background Counts @ 0.2 cm Ave.

#1	13.5, 12.0	12.5	12.5
#2	12.0, 12.0	12.25 ⁺	12.0

Filling from:	Time:	Soln level	C ₁	C ₂	(C ₁ /C ₂)	(C ₁ /C ₂)	Remarks
#9	3:00	4.0					#9 Empty
#8	3:04	10.2	25.5	24.5	.490	.490	
#8	3:15	17.1	34.0	31.0	.368	.387	#8 Empty
#6	3:26	25.1	51.5	47.0	.242	.255	
#6	3:32	30.1	76.0	67.5	.165	.178	#6 Empty
#5	3:36	32.7					
#5	3:45	40.0	142.5	128.0	.0878	.0938	
#5	3:57	44.1	386.5	338.5	.032	.036	#5 Empty
#4	4:11	45.3					
	4:20	Critical with Rd @ 36 cm			S @ ∞		
DRAIN #4		44.85 45.0		48.0			
	4:30	Critical with Rd @ 40.8			S @ ∞		
DRAIN #4	4:37	44.8					
		Not Critical					

DRAIN BACK	#3	#4	#5	#6	#8	#9
	13.6	15.1	12.0	16.1	16.	dv.

Conclusions: Estimated best critical point for 6 1/2" cylinder, N_H/N_X ≈ 45, tamped, is 44.9 ± .05 cm.

Note: Calculated N_H/N_X's appear in upper right hand corner of this page.

11/17/48 bc 44.9 + 2.2 = 47.1 cm - He corrected for bottom -
 N_H = 43.87, 43.9
 6 1/2" Stainless, Tamped
 spg = 1.65

32.6
 0.226 = 0.538
 with N_X = 0.226 = 0.422 gm/lcc
 V_c = 10.08R
 M_c = 4.20 kg 5.42 kg

Experiment 47 10" Reactor Cd shielded Tamped ¹⁵
 $NH/\mu x = 43.87$
 12/5/47

11:00 Start of experiment
 Soln Height in 10" Reactor
 #3 #4 #5 #6 #8 #9 (From Drain back) Macklin Morfitt
 5.7 6.3 5.0 6.7 6.7 dead Vol.

Trip Points - #3 at 90 on 100 scale
 #4 at 86 " " "

Instruments:
 #3 on 100 scale
 #4 " 10 scale
 #5 " 2 "
 Process Monitor

			Background Counts at 0.9cm avg. =		#1	#2		
	Cylinder	Soln.	C ₁	C ₂	c/c ₁	c/c ₂	Remarks	
11:03	#9	0.9	11 1/2	11.0	11.5	11.0	Stopped to eat lunch	
			11.5	11.0				
12:20	#9						Cyl. empty	
12:30	#8	5.1	14.5	14.0	.793	.786		
	#8	7.2	—	—	—	—	Cyl empty	
12:32	#6	10.0	30.5	24.5	.377	.449		
			27.5	25.5	.419	.431		
12:54	#6	12.1	38.5	35.5	.299	.310	not emptied	
1:05	#4	13.90	52.0	46.0	.221	.239		
1:13	#4	16.50	85.5	78.0	.135	.141	not emptied	
1:25	#5	18.50	155.5	136.5	.074	.081		
1:35	#3	19.50	269.0	236.5	.0427	.0465		
1:45	#3	19.90	387.0	339.0	.0297	.0326		
2:07	#3	20.20	source pull not quite critical					
2:08	"	20.3	"	"	"	"		
2:14	"	20.4	"	"	"	"		
2:30		20.6	Critical at this point with tamped 3mm above Soln.					

Drain back:
 3 4 5 6 8 9
 5.7 6.3 5.0 6.7 6 dead Vol.

11/17/48 DC 20.5 + 0.9 = 21.4 cm He corrected for bottom -
 10" Stemless, Tamped and Cd shielded
 $H/\mu x = 43.87$ 43.9
 $\mu_{Cd} = 0.225$ $\mu_{He} = 0.422$ $\mu_{Cd} / \mu_{He} = 0.536$ $\mu_{Cd} = 0.536 \times 0.422 = 0.226$
 $\mu_{Cd} = 1.65$
 $V_c = 10.84 \text{ cc}$
 $M_c = 4.77 \text{ g}$ 5.83 kg.

Checkman
 $H/\mu x = 44$; 10" Reactor - Tamped plus Cd shield - critical at 20.5 ± 0.1 cm.

Experiment 48. — $\frac{43.87}{\cancel{44}} 10''$ cylinder, Tamped.

Dec. 5, 1947.

Beck 3:00 — Removing column, preparing for Tamped Expt.
 Moffitt.
 Cronin.

Instrument checked OK.

Background:

#1 #2
 14.0 13.0

#4 on 10, #3 on 100, #5 on 1. Proc monitor OK. Feed not operating.

Solution Level	Counting Rate		c/p	
	#1	#2	#1	#2
3:30 0.3 "zero"	14.0	13.		
	14.5	14.		
3:35 7.0	34.0	31.5	.427	.445
3:45 11.0	95.	83.0	.153	.169
3:50 13.0	237.	210.5	.061	.065
4:00 13.6	436.	390.5	.033	.036
4:07 13.75	Not critical, but close.			
4:13 13.80	"	"	"	"
	13.90	"	"	"
4:20 14.0				

Drain Back

3 4 5 6 8 9
 5.5 6.5 5.0 6.7 6 dead Vol.

Conclusion: Critical at 13.95 ± 0.05 cm
 c/sub

11/17/48 Dec $13.95 + 0.93 = 14.9$ cm — He corrected for bottom.

10% Stainless tamped

HW = ~~42.87~~ 43.9

app = $\frac{1.65 \times 326}{0.256} = 0.538$
 wt + vol = $0.256 = 0.722$ gm/cc.

Vc = 7.55 R

Mc = 4.06 kg.

Experiment 49. 10" Cylinder [untamped] $H/x = 43.87$

Beck
 Macklem } 8:30 making preparations for 10" untamped.
 Fox
 Umin }
 Olsen } 9:30 making repairs on #5 instrument.

Trip points #3 at 88 on 100, #4 at 89 on 100.
 #3 set on 100, #4 on 10 scale, #1 & #2 ok, process monitor ok.

	Selection Level	Counting Rate		Co/C	
		#1	#2	#1	#2
9:40	Background	115	102		
		115.	99.5		
9:48	0.2 "zero"	114.5	97.0		
		114.	100.		
10:08	10.2	153	128.	0.745	0.78
		148.5	133.5		
10:19	15.1	277.5	245.5	0.41	0.41
10:26	20.0	476.5	413.0	0.24	0.24
10:36	27.4	815	717.	0.14	0.14
Source pulled up to reduce reading on instruments.					
10:47	24.3	397.	398.	0.14	0.14
10:56	26.5	879.	773.	0.07(?)	0.07(?)
Source pulled higher - (above solm level).					
11:02	26.5	221.	188.5		
new zero = 27. Counts/min ("")					
11:22	31.2	Not critical but close.			
11:30	31.6	Above critical			
	31.5	Above critical			

Drain back

#3	#4	#5	#6	#8	#9
5.0	7.4	7.6	7.1	7.0	Dead Val.

11/17/48 DC 31.4 + 0.93 = 32.3 cm H₂O corrected for bottom -
 10" Stainless untamped
 H/x = 43.87 43.9
 op_{air} = 1.65 $\frac{32.3}{0.74} = 0.534$ gm³/cc
 wt of air = $\frac{0.534}{0.74} = 0.722$
 V_c = 16.36 L
 M_c = 8.80 kg

Conclusion: Critical at 31.4 ± 0.1 cm.

18 12/11/47

Exp. 41b

$H/\lambda = 43.87$

8" Reactor Tamped with Cd Shield

Callihan
Cronin
Fox
Moffitt

Note: This reactor is now 36" long since there was doubt as to whether a longer cyl. might not be critical see Exp 41 p. 9 this book.

8:30 AM

Counters were turned off on arrival

Background (no solution) #1 #2
10 10
12.5 11

Estimated Heights (8" Cylinder)

#3 #4 #5 #6 #8 #9
7.8 11.6 11.9 11.1 10.9 Dead Vol.
Counts @ 0 cm.

#1 Erratic - 16, 16.5, 15, 12.5, 16. Use 16
#2 10, 10, 10 Use 10

Time	Solution Level	Counting Rate		Recip. Mult.		Comments
		#1	#2	#1	#2	
10:54	Dead Vol.					#9 Empty
10:57	4.9	18	12.5	.890	.800	Filling #8
11:08	12.1 12.0	25	21.5	.640	.465	#8 Empty
		26.5	19.5	.615	.512	From #6
11:23	23.2	40.5	34.0	.395	.294	#6 Empty
11:32	27.5	44.5	41.0	.360	.244	From #5
11:42	34.6	61.0	53.0	.262	.189	#5 Empty
		60.0	53.0	—	—	
11:53	38.0	72.5	69.5	.222	.138	From 3
12:01	45.2	108.5	108.5	.120	.092	3 empty @ 42.1, From 4
12:10	47.5	187	165.5	.097	.060	From 9
12:23	48.6	261	227	.061	.044	
12:35	49.0	318.5	280.	.050	.036	
12:40	49.5	Not Critical				
12:45	49.7	Not Critical				
12:50	49.9	Not Critical				
12:52	50.1	Critical with Tanager 1mm above soln. - Actually slightly super crit.				

Drain Back #4 #3 #5 #6 #8 #9 Background #1
11.6 7.8 11.9 11.1 12.0 Dead Vol. 11.0

Conclusion: Critical @ 50.0 ± 0.05 cm.

11/17/48 DC 50.0 + 1.5 = 51.5 cm. He corrected for bottom.
 $H/\lambda = 43.87$
8" Stainless, Tamped and Cd shielded

Exp. 50a

8" Reactor Untamped with Cd. Shield $H/X = 43.87$

2:30PM	Background	#1	#2		Callihan Cronin Fox Mortitt
	dead Vol. filled	115.5	97.5	Use 98.0	
		115.5	99.0		

Time	Soln Level	Counts		Recip. Mult. %		Comments
		#1	#2	#1	#2	
2:36	13.0	141.0	126.5	.820	.774	#8 Empty
2:45	23.7	216.0	194.5	.536	.504	#6 Empty
<p>At this point in the experiment the ionization chambers read ≈ 18 on the "50" scale & the source was pulled to 15 cm. The chamber reading dropped to 09 at this point. The above count was then repeated: #1: 102 #2: 88.5. Since the multiplication had already been determined at this point, corresponding "backgrounds" were calculated: #2: 44.6 #1: 55.7.</p>						
3:10	[From #5] 32.5	S=15 213.0	192.5	.257	.232	Calculated from "new" bgd.
		S=0 259.5	233.5	.445	.420	#5 Empty @ 35.0
3:27	40.2	S=0 279.5	250.0	.413	.392	From #3
<p>The source was reset @ 0 cm & the experiment continued in the usual way. The above attempted method does not appear generally feasible.</p>						
3:32						#3 Empty @ 42.0
3:37	53.5	294.0	267.5	.393	.366	#4 Empty
<p>The tamper which (Cd in bottom) was at 72 cm was lowered to 61.0 The count was repeated:</p>						
		301.0	274.4			
<p>Tamper was then lowered into contact:</p>						
		306.0	283.0			

Drainback

#4	#3	#5	#6	#8	#9
11.5	7.0	11.2	11.5	not drained	not drained

Conclusions Not Critical @ Infinite Height.

Exp 41b
 $\text{rel. } \rho_{\text{or}} = \frac{0.326}{0.226} = 0.538$
 $\rho_{\text{or}} = 1.65$
 $V_c = 16.70R$
 $M_c = 8.98 \text{ kg}$

Experiment 50 b
8" Reactor Untamped

$$k_{eff} = 43.87$$

Callahan
Cronin
Fox
Morfitt

Time	Soln. Height	Counting Rate		Recip. Mult		Comments
		#1	#2	#1	#2	
4:27	12.1	113.0	97.0	1.02	1.01	From #6
4:34	20.0	168.5	149.5	.686	.651	#
4:40	24.5	189.	173.	.610	.567	#6 Empty
4:47	30.2	214.	190.	.540	.516	#5 Empty @ 39.6
4:52	—	—	—	—	—	From #3
4:55	42.5	238	213	.485	.460	#3 Empty
5:05	53.3	248.5	223	.465	.439	#4 Empty

NB → 9" cyl.

#9	#8	#4	#5	#3	#6	#7	#1
7.5	7.5	10 cm.	6.5 cm.	5.0 cm	5.0	12 cm	Lead Vol.

Background Count: 109.0 89.0
Slightly Different. Do not change basic shape or position of curve.

Conclusion: In the untamped case without Cd shielding, the solution is "safe" than with shielding. Neither case was critical or would be predicted to be critical at infinite height. The relationships between the unshielded & Cd shielded untamped results was the expected one.

(JMM)

$$H = 53.3 + 1.5 = 54.8 \text{ cm}$$

$$k_{eff} = 43.9 \quad \rho_{eff} = 1.65$$

$$k_{eff} \rho_{eff} = 32.6 = 0.538 \text{ per/cc}$$

$$V = 17,817.77 \text{ L.}$$

$$M = 9.56 \text{ Kg.}$$

} Actual
Mass.

Estimated $H_c = M_c = V_c = \infty$

Calc. Dilution to $\frac{H}{X}$ approx 60 from $\frac{H}{X} = 43.87$

cyl.	Ht.	Vol (calc)	Add DD water
#1	dead Vol	3,497.7	1,252.1 gms (4" cylinder)
#3	5	1,285.0	461.3
#4	10	2,570.0	922.6
#5	6.5	1,670.5	599.6
#6	5.0	1,285.0	461.3
#7	12.0	3,084.0	1107.3 (4" cylinder)
#8	7.5	1,927.5	691.97
#9	7.5	1,927.5	691.97
		32,567.9	9,555.9 total
		<u>x 1.667</u>	
		54,290.6	.8 gms

This quantity of water has not yet been added to these cylinders.

Wgt. Samples sent to laboratory for corrosion checks one in material balance boat

$\frac{NH}{X}$ from repeat samples: #1 Cor #35 = 3.7061 gms soln
1.5211 gms oxide

$$\frac{H}{X} = \frac{80.43 + 36.28}{44.15}$$

34.73% U

#2 Cor #24 2.6123 soln
1.0854 oxide
35.16% U

$$\frac{H}{X} = \frac{79.45 + 36.28}{43.17}$$

#3 Cor #38 2.1184 soln
0.8897 oxide

$$\frac{H}{X} = \frac{78.60 + 36.28}{42.42}$$

35.54% U

Area 3" storage cylinder

12/15/47

Expt. No.	Calc. Vol.	Sol. Ht.	gms. H ₂ O to add	measured Sampled density after dilution
1	3502 cc	24.4	1183	1.501
3	1536	19.0	1169 519 (1.51-)	1.501 ^{no change added}
4	3032	37.5	1025	1.478
5	2182	27.0	738	1.490
6	1616	20.0	546	1.492
7	4347	30.3	1469	1.485
8	2579	31.9	872	1.484
9	2644	32.7	894	1.486

12-16-47

	ΔH	Sol. Ht. (1.987)	Ht in 8" Reactor
1 (4)	28.8	57.2 cm.	= 14.2
3	29.6	58.8 "	= 8.5 cm
4	41.2	81.8 "	= 11.8
5	30.8	61.2 "	= 8.9
6	24.4	48.5 "	= 7.0
7 (4)	36.4	72.4 "	= 18.0
8	47.4	74.3 74.3	= 10.8
9	38.2	75.9	= 11.0

12/15

Replaus #2-3" with 4" storage cylinder -
Scrubbed pit.
Diluted solution to H₂O = 60.

* See pg 34 this book for information on resulting concentration.

Experiment 51

8" Reactor.

CD Shielding plus H₂O tampering.
HX = ~~60~~ 62.6

12/16/47

Williams
Crown
Joy
Callahan

Trap points - #3 - 89410
#4 - 89410

Scales : #3 - 100

4 - 10
5 - 1

R.E - 25 ms.

Filling from #9

10:15 "Background" I II
11.5 10.5
10.5 10.0
11.0 10.0

10:35 H = 0.7 cm 9.5 10.0
10.0 10.0
10.0 10.0 (M⁻¹)
10.0 10.0

#9 empty

10:40

I II
#43 H = 8.6 cm 17.0 15.5 0.59 0.645

Filling from #3.
#3 empty.

#50 H = 12.7 cm 22.0 21.5 0.455 0.465

Filling from #1

Blow-back to mix solution -

11:10 H = 17.7 cm 27.5 27.0 0.364 0.370

15 = 22.6 ~~30.5~~ ~~37.0~~

#1 empty, Filling from #6.

20 = 24.8 39.5 37.0 0.253 0.270

26 = 29.3 49.5 45.5 0.202 0.220

#6 empty

33 = 38.3 83.0 ~~75.5~~ ~~76.5~~ 0.120 0.132

Filling from #5, #5 empty.

43 = 42.6 132.5 120.5 0.075 0.083

Filling from #8

52 = 46.1 327.5 298.0 0.031 0.034

12:14

= 47.0 635.0 566 0.016 0.018

~~some empty~~

Filling from #4.

20 = 47.0 (pours out - tamper 8mm above liquid surface - critical) -

Drain back

cm in 8" reactor

#4	To	45.4 cm	13.4	X
#8	To	42.6	2.8	X
#5	To	30.0	12.6	>
#6	To	19.4	10.6	<
#1	To	5.0	14.4	
#3	To	0.0	5.0	X
#7			18.0	<

Conclusion:

8" HX = 60, CD + H₂O tampering - critical at 46.95 ± 0.05 cm.

D.C.

11/17/48

46.95 + 1.45 = 48.4 cm - He corrected for bottom

ρ_{app} = 1.50

HX = 67.6 - 62.7

wt % X = 0.264 26.4 = 0.396 g_w/cc

8" Stainless stamped and CD shielded

V_c = 15.69 R

M_c = 6.21 kg

12/16/47

Experiment 52

8" Reactor

H/x = 60 67.60

Uncamped.

Cronin
Williams
Fox
Caellhan

Scales: 3 - 100

4 - 10

5 - 1

R.E. - 25 ms.

		I	II	M ⁻¹		
	"Zno" Count	I	II	I	II	
1:42 P		105.5	94.5			
		105.0	92.5			
48						Filling from #7
58	H = 10.2 cm	100.5	89.5	1.05	1.04	
2:07	= 18.2	166.5	151.0	0.632	0.620	#7 Empty. CS Control not in.
		169.5	152.0	0.620	0.616	" " " and
17	= 23.4	205.0	182.0	0.514	0.514	Filling from #3; #3 Empty.
26	= 30.1	234.5	211.0	0.445	0.443	Filling from #6 (#6 empty at 37.8)
37	= 40.0	255.5	235.5	0.412	0.397	Filling from #4
46	= 46.0	270.0	243.5	0.390	0.384	Empty #4.
55	= 58.5	285.0	255.5	0.370	0.366	Filling from #5; #5 Empty
3:08	= 70.0	286.5	258.0	0.368	0.363	Filling from #1
3:40	= 0.5 cm	111.5	99.5			

Conclusion: 8" reactor, uncamped, H/x = 65, apparently λ is not too critical at infinite length. DC.

Drain Back - data #1 - 12.9 cm in 8" reactor.

3 -	10.0	"	"	"
4 -	10.0	"	"	"
6 -	10.0	"	"	"
7 -	20.0	"	"	"
8 -	13.3	"	"	"
	18.5	"	"	"

11/30/48 DC

$H = 70.0 + 1.5 = 71.5 \text{ cm}$

$H/x = 67.7, \text{ app} = 1.50$

$\text{with } H/x = \frac{26.4}{24.6} = 0.396 \text{ ft/ft}$

$V = 23.18 R$

$M = 9.18 Rg$

Estimated - $V_c = H_c = M_c = \infty$

12/16/47

Experiment 53

8" Reactor

Tamped

H_{cr} = 60 - ~~62.6~~ 62.60

Williams

Cromi Seeds - 3 - 100
 In 4 - 10
 Cells RE - 50 mv - unstable

4:06 P "Zero Count"

	I	II
H = -0.5cm	12.5	14.0
	12.5	13.0
	12.5	13.5

4:11 Filling from #3.

			M ⁻¹			
			I	II		
4:14	H = 5.0	19.0	18.0	0.658	0.751	
4:26	= 10.5	34.5	33.0	0.363	0.409	#3 Empty
4:33	= 13.3	48.5	46.5	0.258	0.291	Filling from #1
4:40	= 16.0	71.5	68.0	0.175	0.199	
4:48	= 18.0	112.0	106.0	0.112	0.129	
4:55	= 19.7	182.0	174.0	0.069	0.078	
5:07	= 20.5	286.0	267.5	0.044	0.050	Filling from #4
5:13	= 21.7 (= 21.5 with source out)					critical with @a 10 cm @d below liquid surface
5:25	= 21.3 (source out)					slightly sub critical with @d control rod completely out.

Conclusion: 8" reactor tamped, H_{cr} = 60 - critical at 21.4 ± 0.05 cm -

De.

DRAIN BACK -

- #1 - $\frac{23.4}{20.5}$ cm in 8" reactor = 18.5 - cm in 9" reactor.
- #4 - 10.0 " " 8" " = 7.9 " "
- 6 - 10.0 " " 8" " = 7.9 " "
- 7 - 20.0 " " " " = 15.8 " "
- 8 - 13.3 " " " " = 10.5 " "
- 9 - Dead volume

11/17/48 21.4 + 1.45 = 22.9 cm - H_{cr} corrected for bottom.

H_{cr} = 62.6 62.7

8" Stainless Tamped.

sp gr = 1.50
 wt % = 26.4 = 0.396 g/cc

V_c = ~~9.40 L~~ 7.42 L

M_c = ~~5.06 Kg~~ 2.94 Kg

Exp 54. 9" Cylinder, Cadmium Tamped. $M/x \approx 60-67.60$ Dec. 17.

Beck
Mofette
Fox
Crown

#3 Chamber strips at 91, #4 at 95 on 100 scale

#4 on 10, #3 on 100, #5 on 2. Reel & Proc Monitor. OK.

	Solvent	Counters		C/pc		
		#1	#2	#1	#2	
10:00 AM.	"Background"	14	14			
	"	14	14			
10:12.	1.3 cm	13.5	12.5			
		12.	12.			
10:19	10.0	22	22.5	.568	.568	From # 8
						# 8 empty at 11.5.
	19.0	52	52.5	.24	.24	#6 empty.
10:26	23.0	88.5	93.2	.14	.135	
10:43	26.0	213	210.	.058	.056	
10:47	26.5	275	275	.045	.045	
10:52	27.1	461	459.	.027	.027	not critical with source in
10:59.	27.15	Critical with source out (level drops ≈ 2 mm when source is pulled)				

Conclusion: Critical at 27.15 with source out (level drops 400 mm when source pulled).

To
19
6
35
4
4
4
200
3
000

Down back.

#1	4	6	7	8	9
18.5	25	9.5	15.4	9.8	lead Vol

11.7/48 DC $27.15 + 1.15 = 28.3$ cm = He corrected for bottom -

$M/x = 62.7$

9" Stainless, Tamped + Cs shielded.

$dp/dx = 1.50$
with $Q_{1/2} = 26.4 \approx 0.396$ gm/cc

$V_c = 11.64$ R

$M_c = 4.61$ Kg.

Exp ~~#4~~ 55. 9" Unjamped. $H/x = 62.6 \text{ v. } 60$

Dec 17
18

27

Everything same as for previous experiment.

So	Solution Level	#1	#2	C _o /C _i	
11:30.	0.4 mm.	1025	95.5	#1	#2
		102.5	93.0.		
11:50	15.9.	212.	207.5	.475	.455
11:58	24.5	374	354	.27	.265
12:06	33.1	571.	542	.178	.174
12.	40.0	839	810	.12	.115
12:25	44.1	1136.	1096	.089	.086.

#1	#4	#6	#7	#8
16	7.5	10	16	10.

Conclusion: Does not go at 44 cm height, but probably would go at 55 cm or so.

$$H = 44.1 + 1.2 = 45.3 \text{ cm}$$

$$H/x = 62.7 \text{ (see previous page)}$$

$$V = 18.59 \text{ R}$$

$$m = 7.36 \text{ kg}$$

Estimated

$$H_c > 55 \text{ cm}$$

$$V_c > 22.6 \text{ L}$$

$$M_c > 8.9 \text{ kg}$$

Exp. 56 - 9" Tamped - H/x ~ 60.6 x .60

Dec 17.

Beck Merfitt Cronin Fox.

Same as in prev. experiment.
 Instruments all repaired satisfactorily.

	Solution level	Counting		Co/c	
		#1	#2	#1	#2
1:45	zero.	15	15		
	12.0	64.5	68.5	.23	.22
2:01	14.1	107	113	.14	.132
2:09	15.0	163	167.5	.092	.109
2:15	16.0	303	312	.05	.048
2:25	16.4	505	511	.0292	.0295
2:30	16.7	⁹²⁸ 940	940	.0162	.016
	16.8	Critical - some above.			

Conclusion: Critical at $16.75 \pm .05$

11/17/48 $16.75 + 1.15 = 17.9$ cm. = Hc corrected for bottom

H/x = ~~62.6~~ 62.7

9" Stainless Tamped.

$\rho_{app} = 6.50$
 $\text{with } H_c = 26.4 = 0.396 \text{ gm/cc}$

$V_f = 7.39 \text{ L}$

$M_c = 2.93 \text{ kg.}$

Drum Back.

	#1	#4	#6	#7	#8	#9
9" cyl.	16	25	10.	16	10.	Dead Vol. for 9"
10" cyl.	13	6.1	8.1	13.	8.1	"

483 508

Exp 57, # 10^{10"} - Cadmium Tamped. H/x 260^{62.60} - Dec 17.

Beck
Mofett
Fox
Cronin

Same as in prev. Exp.
Instruments all respond satisfactorily

	Solution Level	Counting Rate		Co/C.	
		#1	#2	#1	#2
3:36	0.3.	12.5	14		
		12.5	13.		
3:50	15.0	51.5	53.5	0.24	0.25
	18.2.	101.	105.5	0.124	0.128
	20.1	250	244.	0.050	0.55
		240	247.		
4:12	20.6	347	347	.036	.039
	21.0	644	642	.019	.019
	21.05	Critical			

Conclusion: Critical at 21.05.

Drain back.

#1	#4	#6	#7	#8	#9
13	6.1	7.1	14	8.1	Ready Volume.

#17/44 cc 21.05 + 0.93 = ^{22.0}21.98 cm - Hc Corrected for bottom.
H/c = ~~62.6~~ 62.7

10" Stainless, Tamped and Cd shielded.

Sp gr 1.50
wt % C = 26.4% or 0.396 g/cc

Vc = ~~7.39~~ ~~11.65~~ 11.15 L

Mc = ~~2.93~~ ~~4.61~~ Kg 4.42 kg

Exp 58 ^{67.60} $H/X = 60$ 10" Reactor Untamped

Murray
Morfill
Fox
Cromie

9:30 Equipment checked and starting
 9:32 Film badges & dosimeters issued personnel checked.
 Instruments: #3 #4 #5 Power Reed
 Scale 100 10 2 - 50
 Trip Point 94 94 - -

Selection

Cylinders: #1 #4 #6 #7 #8 #9
 Ht. in 10" reactor 13 cm 6.1 7.1 14 8.1 dead vol.

In previous exp. ($H/X = 44$) Untamped = 31.4 cm
 Shuddered - Tamped = 20.5 cm
 Tamped = 13.95 cm

($H/X = 60$) Cd Tamped = 21.05 cm
 Estimate of critical Ht = approx 32 cm.

	Cyl	Ht.	Counters	#1	#2	C_1/C_2	C_1/C_2	
9:53	#9							
10:00	#9	0.9	82	94				Cyl empty
			81	92.5				
10:08	#8	8.3						Cyl empty
10:11	#6	11.1	160	173.5	.509	.536		Cd Rod In.
			163.5	170.5	.498	.542		Cd Rod out
10:21	#6	15.8	271.5	290	.300	.320		Cyl empty
10:29	#4	22.1	534	572	.153	.163		Cyl empty Cd Rod out.
10:39	#1	26.0	920	1030	.0886	.092		
10:50	#1							
10:50	#1	27.0	-	-	-	-		Source pulled note a maximum at about 12 cm up.
10:55	#1	28.0						Source out to 20 cm with Cd Rod out
11:00	#1	28.6						Source at 23 cm Cd Rod out.
11:08	#1	29.1						Source at 25 cm Cd Rod out
11:13	#1	29.6						" "26" " " "
11:16	#1	30.1						" "30" " " "
11:21		30.4						" "38" " " "
11:26		30.9						" "40" " " "
		30.7						Source on front or possible Rod at 19 cm
								Source at 60 Rod out

Drain back to give

#1 #4 #6 #7 #8 #9
 13 cm 7.4 6.2 14 8.3 dead vol.

Conclusion. Exp 58. at $H/x = 60$, 10" reactor untamped goes critical at 30.8 ± 0.1 cm. On untamped experiments the ionization chambers should be quite far from the reactor, to allow multiplication measurements closer to criticality. Had to stop, today, almost 5 cm from critical height.

Note: Interchanged counters to try to find some temporary trouble. Cleared up of own accord, but left them reversed

11/17/48

$$30.8 + 0.9 = 31.7 = H_c \text{ corrected for bottom -}$$

$$H/x = 60 \text{ to } 62.7$$

10" stainless, untamped.

$$\rho_{p,gr} = 1.50$$

$$\text{wt} \% X = 26.4 = 0.396 \text{ g/cc}$$

$$V_c = 16.05 \text{ R}$$

$$M_c = 6.36 \text{ Kg.}$$

Exp 59

12/18/47

10" Reactor Tamped $\frac{4}{8}$ u606260

Murray
Worfill
Fox
Crown

1:16

Dead Volume full-tamper filled

	#1	#2
Background	16.0	16.0
	16	15.25
	15.25	16-3/4

Time	Cyl.	Ht.	#1	#2	C/C ₁	C/C ₂	Remarks
1:25	#8	7.0cm	32.5	32.0	.493	.500	
1:57	#8	8.8	43	50.5	.369	.314	cyl empty
			48.5		.327		
1:48	#1	11.0	83.0	89.0	.193	.180	} Reading taken with some in solution.
2:00		13.0	195.5	202.5	.081	.0791	
		13.5	307	335.5	.052	.0478	
2:20		14.0	461	476	.031	.030	
2:30		14.2	1018	1083	.0141	.0133	
		14.3	—	—	—	—	CRITICAL Cd in some out. Tamper down

Conclusion:

10" reactor tamped $\frac{4}{8}$ u60 critical at

14.25 cm \pm .05 cm. Very important:

Cd rod not worth much. Should not add more solution than Cd rod is worth when approaching critical.

Drainback:

giving

#1	#4	#6	#7	#8	#9
13	7.4	6.2	14	8.3	dead vol = 10"
30.	17.5	14.5	33	19.5	

11/17/48 de 14.25 + 0.93 = 15.2 cm the corrected for bottom -

H₁ = 6.76 62.7

10" Stainless Tamped.

ppm = 1.50

ml. 2.4; \pm 0.396 g/mlcc

V_c = 7.70R

M_c = 3.05Kg.

Exp 60 - 6 1/2 Tamped - $\pi/x \approx 62.60$ 12/19/47

Beck
Weckler
McLendon
Crown

8:20 Checking safety devices. Dump mechanism, trip points, instrument response.

3 trips at 90, # 4 on 94.

5, # 1, # 2, recd. & proc. monitors responds satisfactorily.

Solution level	Counting Rate		Co/C	
	# 1	# 2	# 1	# 2
Background:	12	15.5		
	13	13.5		

9:06 zero 0.4

12.0 13.0

8 empty at 21.5

9:12 34.8

72.0 78.5

.167 .166

6 empty at 34.8

9:17 40.1

110. 123.

.11 .105

9:24 43.5

184. 204.

.065 .063

9:30 45.7

312 358.

.038 .036

with source in

9:35 45.0

not critical

with source out (45.4 source in).

45.2

not critical

45.4

not critical

45.6

not critical

9:52

45.7

Critical

Conclusion: Critical at 45.7 ± 0.1 cm

Drain back:

# 1	# 4	# 6	# 7	# 8	# 9
30	17.5	15	33	20	Dead Vol.

11/7/48

$45.7 + 2.2 = 47.9$ cm Ac- counted for bottom -

$H/x = 62.6$ 62.7

6 1/2" Stainless Tamped.

$\rho_{sp} = 1.50$

with 90% = ~~0.34~~ 26.4 = 0.346 gm/cc

$V_c = 10.25$ R

$M_c = 4.06$ kg.

12/22/47

Project - dilution to $\frac{H_2}{H_1} \approx 80^{\pm 20}$

* Samples taken from #9 for $\frac{H_2}{H_1}$ measurement and density measured 1.501 @ 24°C. (1.507 @ 14°C.) from Cronin's $\frac{H_2}{H_1}$ vs d chart. $\frac{H_2}{H_1}$ estimated at 56 for dilution purposes. $\Delta = 0.3940$ V calculated by formula

Tank #	dia"	H ₂	H ₁	DH	V	Δ (H ₂ to add)
1	4	70.0	32.5	37.5	5921 5921	
2	4	51.5	49.3	2.2	200 347	
3	3	51.2 51.3	49.4	1.9	172	
4	3	71.6	30.9	40.7	3691	
5	3	51.8	48.9	2.9 3.1	281	
6	3	69.5	32.8	36.7	3329	
7	4	73.5	29.3	44.2	4009 6979	
8	3	73.6	29.3	44.3	4018	
9	3	69.2	33.4	35.8	<u>3247</u>	

Capacities 4" 7349 crit value $\frac{7349}{1.3940} = 5272$

3" 4223 $\frac{4223}{1.3940} = 3029$

∴ #s 1, 4, 6, 7, 8, 9 all too full to dilute

$\frac{30}{1.394} = 21.5$ liters, max needed (8" cyl) soln for next run

Decision to leave #8 at present dilution & dilute the rest. (pull each cyl to dilute below DH = 33.4 on manometer)

* 11/19/48 From Cronin notes

Dish L-3
Gross 7.0753 gm
Tare 6.4283
Net 0.6470 gm
from 1.7890 gm soln -
sp. gr. 1.501

Dish 40
Gross 9.8492 gm
Tare 8.7832
from 1.0660 gm oxide
3.1914 gm sol.
≅ 66% $\frac{H_2}{H_1}$ average.

Area 4" Cylinder = 80.4 cm² 80. ✓
 Area 3" Cylinder = 46.2 cm² 46.8 ✓

after adjusting heights in cylinders

		H ₂	H ₁	ΔH	Volume cc	Volume cc
1	4	68.9 64.1	39.5 38.0	29.4 26.1	4640	1824
2	4	68.6	38.8	28.8	4548	1792
3	3	69.0	39.5	29.5	2678	1034
4	3	66.1	36.3	29.8	2700	1064
5	3	emptied ~ (1.2)				
6	3	64.5	37.9	26.6	2411	951
7	4	66.1	36.2	29.9	4720	1860
9	3	65.9	36.2	29.7	2693	$\frac{1061}{9.6108}$

added water as per above schedule ↑ rough measuring d after mixing

#	1	2	3	4	5	6	7	8	9
d	1.35	1.34	1.35	1.35 (empty)	1.35	1.35	$(H/x \approx 60)$	1.35	1.35

Heights after dilution (manometric) { NB 11/30/48
 See pg 46 this book for data on concentration

#	dia	H ₂	H ₁	ΔH	Height in Storage Cylinder	6 1/2" Equiv
1	4	71.5	37.4	34.1	74.8	28.35
2	4	74.0	35.1	38.9	85.3	32.30
3	3	73.4	35.8	37.6	82.5	17.66
4	3	73.0	36.1	36.9	80.9	17.25 x
6	3	72.8	36.3	36.5	80.1	17.1 x
7	4	73.5	35.7	37.8	82.9	31.40
9	3	73.6	35.6	38.0	83.4	17.8 x

36 12/23/47

Experiment 61

6 1/2" Reactor.

Cronin
Foy
Williams
Callahan

Tamped.
HX = 86.30

Trip points #3 89 x 100
#4 89 x 100

Scale #3 - 100
#4 - 10
#5 - 2
R.E - 25 ms.

"Pseudocritical" I II
11.5 10.5
11.5 10.5

9:45 AM
9:50
10:00
10:07
10:20
10:30
40
55

H = 0.0 cm
H = 10.0
= 19.6
= 27.7
= 36.0
= 45.3
= 53.7

11.5 10.0
20.7 17.0
31.5 26.5
41.5 38.0
56.0 50.5
98.5 92.0

Filling from #6.
#6 Empty.
Filling from #9
#9 Empty.
Filling from #4
#4 Empty.
Filling from #3
Filling from #2

M⁻¹
I II
0.556 0.588
0.365 0.374
0.277 0.263
0.205 0.198
0.117 0.109

2 (= 53.4 come out) Critical with 21 cm control rod in lamp.

= 53.2 (come out) critical with " " " "
= 52.0 (" ") Critical " " " "
= 51.2 Subcritical.
= 51.4 " "

= 51.7 (come out) slightly super critical

12:05 PM

= 49.1 (come in) 160.5 150.0

0.072 0.067

Since solution #2 was slightly less dense than the other ones, we blew through sight glass.

= 49.4 161.0 151.5

Indicates slight inhomogeneity so above height at criticality may be low.

12:35

= 0 11.5 10.5 -

DRAW BACK.

# 1	Yes	28.3 cm in 6.5" reactor	= 33.2 cm in 6" reactor.
# 2		28.9 " " "	= 33.9 " " "
# 3		13.4 " " "	= 15.7 " " "
# 4		17.4 " " "	= 20.4 " " "
# 5		18.0 " " "	= 21.1 " " "
# 7		31.4 " " "	= 36.8 " " "
# 9		Dead volume.	

Conclusions

- 6 1/2", HX = 80 - Tamped Critical at Solution Height = ~~51.7 ± 0.0~~ 51.6 ± 0.1 cm -
- The multiplication curve dropped off very rapidly near critical; DC 1423

11/17/48 DC
11/14/48 DC

51.6 + 2.2 = 53.8 cm = Hc bottom corrected
HX = 86.3 86.4
6 1/2" Stainless, Tamped.
op pr = 1.35
with 90% = 21.3 = 0.288 g/cc

Vc = 11.5 l.
Mc = 3.31 kg.

11/23/47

Experiment 62

6" Reactor

Tamped
 $H/X = 86.3$

Fox
 Cronin
 Cascha

Trip points #3 89K100 Scales #3 - 100
 #4 89K100 #4 - 10
 #5 - 2

Background Count I II R.E. = 25 mV

Time	Sol'n.	I	II	%	%	Cyl.
15:12	0	12.0	12.5			#9
15:15	dead Vol. ^{1.6 cm}	13.5	11.0			#9 empty
		13.5	12.0			
15:32	5.7	16	13.5	.844	.890	#2
15:55	15.5 15.3	23.0	19.	.588	.632	
16:07	25.3	29.0	25.0	.466	.481	
16:16	38.1	32.0	30	.424	.417	#2 empty
16:25	50.2	35	32	.386	.391	#1
16:36	65.4 65.4	38.0	34.5	.356	.363	
16:46	70.3	37.0	33.5	.365	.373	
		36.5				

Drain back:

#1	has 35.4 cm in 6" Reactor = 26 in 7" reactor.
#2	34.8 " " "
#3	18.7
4	20.4
6	21.1
7	36.8
9	Dead Volume.

17:04 Recheck of background I II
 zero level 140 10.5

Conclusion: 6" Reactor, $H/X = 80$, Tamped, Not critical at 70.3 cm & probably would not be so at infinite length - DC.

11/30/48 DC $H/X = 86.4$ - see preceding page

$H = 70.3 + 2.6 = 72.9 \text{ cm}$

$V = 13.30 \text{ L}$

$M = \pm 3.83 \text{ L}$

Estimated: $H_c = V_c = M_c = \infty$

12/24/43.

Experiment 63.

7" Cadmium - Tamped.

HX = 86.3

Beck
Vernier
Joy
McLendon

8:30

Aligning cylinder, checking instruments.

Trip points # 3 - 88 # 4 - 92

4 on 50 scale # 3 on 100, # 5 on 2, Reed & Pw. Monitor OK.

	Solution Level	# 1	# 2		
10:30	Background	14.5	12.5		
		15.0	13.5		
		14.5	12.5		
	zero: 0.9	13.0	10.5		
		13.0	10.5		
10:52		26.3	25.0	2.2	152, .46 # 7 empty.
11:06		42.0	27.0	24.5	148 .43
11:13		56.3	26.5	25.5	.49 .41
11:25		70.0	26.0	24.5	

4 empty

"

6 empty

Drain back:

# 1	26
2	25
3	18.5
4	15
6	15
7	27
9	dead Vol.

Conclusion: Does not go. Curve is flat beyond 35 cm.

$$H = 70.0 + 1.9 = 71.9 \text{ cm}$$

$$HX = 86.4 \text{ (see next page)}$$

$$V = 17.85 \text{ L}$$

$$M = 5.14 \text{ kg}$$

$$\text{Estimated} - H_e = V_e = M_e = \infty$$

Experiment 64. 7" Temped. $H/x = 86.3$ 12/24/47.

11:30 removing cadmium, readjusting for Temped experiment.

Back et al

12:30 Instrument Check. — all OK.

	Solution	Counting rate			
		#1	#2		
12:44	zero: 0.0.	14.	12.0	13.5	12.
		13.	12.5		
12:56	25.1	68.5	61.5	.197 from 19.5	From # 2.
12:59	27.5	84.0	78.5	.16	.153
1:07	30.0	94.5	105.	.143	.114 error in counting
		113	105	.100	.114
1:16	32.5	210.	200	.064	.06
1:27	34.0	460.	427	.029	.028
1:37	34.4	Well above critical.			

Drain Back

#	Temp	For 7" reactor.	=	Temp	For 8" reactor.
1	26			20	
2	25			19	
3	11.5			8.8	
4	15.			11.5	
6	15			11.5	
7	27			20.5	
9	Dead vol				

Conclusion - Critical at 34.1 ± 0.1

$H_0/H_{sc} = 341 + 1.9 = 36.0 \text{ cm}$ He bottom covered

$H/x = 86.4$

7" Stainless Temped.

$\rho_{99} = 1.35$
 $\text{wet } \rho_{99} = 21.3 \approx 0.288 \text{ gm}^3/\text{cc}$

$V_c = 8.94 \text{ d.}$

$M_c = 2.57 \text{ kg.}$

Experiment 65. 8" Cadmium-Tamped. $\frac{1}{2}x = 80.86.3$

Beck
Vomer
Joy
McLendon

200 - Removing 7" cylinder; installing 8" - aligning, etc

Instrument check

4 frgs at 94; # 3 at 90.

Solution Level	Counting rate, C.		C/c	
	#1	#2	#1	#2
3:05 zero. 0.7 Co.	9.0	9.0		
	8.5	9.0		
3:22	32.4	37.5	0.24	.252
3:31	43.1	58	.155	.165
3:38	49.6	90.0	.103	.10
3:45.	53.1	159.	.056	.059
3:51.	54.0	223	.040	.041
	54.5	not critical		
	54.6	not critical		
	55.0	Critical		

Drumback #1	20	8" reactor
# 2	12.4	
# 3	10.5	
# 4	11.5	
6	11.5	
7	20.5	
9	Dead Vol.	

Conclusion 55.0 ± .1 Critical

11/7/48 DC 55.0 + 1.45 = 56.5 cr - He bottom corrected

11/20/48 DC He = 86.5 → 86.4

8" Stainless. Tamped + ed shielded

Opgr = 1.35

whl top = 21.3 = 0.248 g/cc.

Vc = 18.32 L

Mc = 5.28 kg.

Handwritten signature: McLendon

Handwritten signature: Beck

11/29/47 Experiment 66 - 8" Tamped; $H_V = 80$ 86.3

Mauldin
Fort
Vinson
Cecilham-

Trip points #3 90 x 100
#4 92 x 100

Scales #3 - 100
4 - 10
5 - 2
RE - 25mm

#1 Pulse recorder n.g.

HIDA Filling dead volume for #9.

	H	I	II	M ⁻¹		
11:20	H = 0.9cm.	12.0 11.5 10.0 14.0	12.0 11.5 12.0 11.8			#9 empty -
11:27	H = 5.2	19.5 16.5 18.0	16.5	0.72 19.5	0.72	Filling from #7.
40	H = 10.0	28.5	24.0	0.441	0.492	
52	H = 15.0	46.0	41.5	0.305	0.285	
12:02 P	17.9 18.0	72.5	63.5	0.193	0.186	Filling from #1
15	= 20.5	135.0	122.5	0.104	0.096	
25	= 21.9	314.5	286.0	0.045	0.044	
33	22.3 22.4	584.0	459.5	0.028	0.026	
45	.	509.0	464.0	0.028	0.025	
50	= 22.5	Critical with 15cm CD below level of solution. (Source out).				
11:00	22.7 22.5	148.5	132.5	0.094	0.089	Top temper raised 25cm above sol. level.

Conclusion - ① 8" reactor tamped $H_V = 80$ Critical with 22.3 ± 0.1 cm solution -
 ② Top temper, at criticality, ≈ 2 cm solution.
 ③ Cause of drop in curve (M⁻¹ vs H) does not seem to be due to lack of delayed neutron stabilization.

- Drum Pans -
- 1 20 cm in 8" reactor.
 - 2 12.4 cm
 - 3 10.5 cm
 - 4 11.5 "
 - 6 11.5 "
 - 7 20.5 "
 - 9 -

11/17/48 pc
 $22.3 + 1.5 = 23.8$ cm the bottom corrected
 $H_V = 86.3$ 86.4
 8" Stainless Tamped.
 $\rho_{sp} = 1.35$
 with 9.7 = 21.3 = 0.288 g/cc
 $V_C = 7.72$ L.
 $M_C = 2.22$ Kg.

Experiment #67

12/29/47

8" Reactor, Untamped, $H/x \approx 80$ 86.3

Fox
Machin
Vibro
Ceecha

Scales - 3 - 100
4 - 10
5 - 2
RE - 50

	$H = 0.32m$ $H = 0.4m$	I	II
2:10P		72.5	73.0
		72.0	73.0
		86.5	79.5
		86.0	76.5
2:25		86.3	78.0
31	$H = 11.9cm$	113.0	100.5
145	$H = 23.2$	163.0	152.0
3:00	= 34.8	194.0	181.0
.17	= 53.9	213.5	193.5
36	= 69.5	214.5	201.5
50	= 79.7	218.5	198.0

Filling from #3.

#3 Empty.

Filling from #4; #4 Empty.

Filling from #6; #6 Empty.

Filling from #2; #2 Empty.

Filling from #1;

Filling from #7

	M	I	II
		0.764	0.776
		0.530	0.513
		0.444	0.431
		0.404	0.403
		0.402	0.388
		0.395	0.394

Conclusion -

8", Untamped, $H/x = 80$ - Not critical at ∞ length -

DEAD BACK -	#	$H/x =$	Length	Equivalent Length
	1	80	16.4 in in 8" reactor	= 13 cm in 9" reactor
	2	" "	23.0 in in 8" reactor	18.2 " "
	3	" "	13.7 " " "	10.6 " " "
	4	" "	11.2 " " "	8.8 " " "
	5	$H/x = 60$	" Empty	
	6	$H/x = 80$	10 cm " 8" reactor.	7.9 " " "
	7	$H/x = 80$	20.3 in in 8" reactor	16 " " "
	8	$H/x = 60$	Ca 4 ft.	
	9		Dead volume -	

$H = 79.7 + 1.5 = 81.2 cm$
 $H/x = 86.4$ (see following page)
 $V = 26.33 L$
 $M = 7.58 kg.$

Estimated $H_c = V_c = M_c = \infty$

Experiment 68

$H/\lambda = 86.3$

9" Reactor Tamped with Cd. Shielding

12/30/47

Callahan
Fox
Williams
Cronin

TRIP Points - #3 - 89x10
#4 - 94x10

Scales 3 - 100
4 - 10
5 - 2
RE - 25mV

8:30 Changed Reactor - Installed 9" Cd shielded cylinder

Time	Soln Hts.	Counters		c/c		Cyl.	
		#1	#2	#1	#2		
12:45P	Background	12.5	11.0				Filling lead out. for #9 -
12:55P	H = 0.6 cm	10.0	9.5	Calculated with $C_0 = \text{Background}$			#9 empty
	"Zero"	9.5	10.0				Filling for #3
1:05	H = 5.1 cm	12.0	10.0	0.816	0.980		
17	= 11.2	20.0	17.0	0.490	0.574		#3 EMPTY.
30	= 17.7	35.0	30.0	0.357	0.367		Filling for #2
37	= 22.6	62.5	54.0	0.200	0.202		
52	= 25.1	93.5	87.5	0.134	0.126		#2 has 4cm left.
2:03	= 27.1	183.0	169.0	0.064	0.065		Filling for #1
18	= 28.0	335.0	309.5	0.037	0.036		
25	= 28.1 (Source out)	sub-critical (crit. with tamps up 5mm).					
	= 27.9 " "	sub-critical - (Source volume = 0.15 cm in 9" reactor).					

Drain back

#1	15.6 cm	(H/λ=80)	in 9" reactor.
#2	18 cm	"	"
#3	10 cm	"	"
X #4	8.8	"	"
5	Empty	(H/λ=60)	
6	7.9 cm	H/λ=80	"
7	16 cm	"	"
8	(4.2)	H/λ=60	
9	-		

Conclusion: 9" Reactor - water tamped plus Cd shielding - Critical at H = 28.0 ± 0.05 cm with source out.

11/17/48 DC 28.0 + 1.2 = 29.2 cm H₂O bottom connected
 11/18/48 DC. H/λ = 86.4
 9" Stainless, tamped with Cd shielding
 sp gr = 1.35
 water ρ₀ X = 21.3 = 0.288 gmf/cc.
 V_c = 11.48 L
 M_c = 3.45 kg.

12/30/47

EXPERIMENT 69

Fox

9" REACTOR, $H/X = 86.3$, TAMPED.

WILLIAMS
CROMBIE
CALLIHAN

TRIP POINTS UNCHANGED.

#3 - 100
#4 - 10
#5 - 2
RE - 25ms

	H = 1.5cm	I	II	M ⁻¹	
				I	II
3:20 P		12.5	11.5		
		12.5	11.0		
		12.5	11.3		
35	= 5.1	17.0	15.0	0.736	0.733
45	= 10.0	32.5	30.0	0.385	0.367
55	= 13.1	57.0	53.5	0.219	0.206
4:07	= 15.6	121.5	109.5	0.103	0.103
:20	= 17.0	243.5 229.	265.0	0.043	0.042

Filling from #7

(3cm left in #7)

Filling from #3.

= 17.5 (with source) slightly subcritical. (= 17.4 cm source out).

= 17.6 (source out) Critical with 6cm of control rod below solution.

Drawback - Same as previous exp. 1743.

Conclusion - 9" Reactor - $H/X = 80$, Tamped - Critical at $H = 17.5 \pm 0.05$ cm with source out of the solution -

11/17/48 DE

11/26/48 DE

17.5 + 1.2 = 18.7 cm = He bottom corrected

$H/X = 86.3$ 86.4

9" Stainless, Tamped.

OPPV = 1.35
wt % X = 213 = 0.288 g/1cc.

$V_c = 7.67$ L.

$M_c = 2.21$ kg.

Experiment 70 -
9" Reactor, $H/X \approx 86.3$, Untamped

Fox
Cromin
Williams
Callahan

Temp points unchanged

Scales # 3 - 100
4 - 10
5 - 1
RE. - 25 mv

		I	II	M ⁻¹		
				I	II	
5:15P	H = 0.1cm	88.0	86.5cm			
		87.5	83.5			
		87.8	82.5			
5:25	H = 10.1	110.5	101.5	0.794	0.813	Filling from #3
40	= 19.9	238.5	217.0	0.368	0.380	#3 Empty; Filling from #7
50	= 26.0	332.0	307.5	0.264	0.268	#7 Empty; Filling from #4
6:00	= 35.2	511.0	477.5	0.172	0.173	#4 Empty; Filling from #2
:15	= 45.1	900.0	857.5	0.098	0.096	
35	= -0.2cm	90.0	84.5			

DRAINAGE:

#1	H _X = 80	15.6 cm in 9" reactor	=	12.6 cm in 10" Reactor
#2	"	18 " " " "	=	14.5 " " " "
3	"	10 " " " "	=	8.1 " " " "
4	"	10 " " " "	=	8.1 " " " "
5	H _X = 60	" EMPTY "		
6	H _X = 80	7.9 cm in 9" reactor	=	6.4 " " " "
7	"	15.0 " " " "	=	12.1 " " " "
8	H _X = 60	ca 4h.		
9	H _X = 80	Dead Volume		

Conclusion - 9" Reactor - $H/X \approx 80$, Untamped - filled to $H = 45$ cm - was not critical - but probably would be critical at finite length - (ca 75cm). at 45 cm $M = 10$ -

$H = 45.1 + 1.2 = 46.3$ cm
 $H/X = 86.4$ (see preceding page).
 $V = 19.00$ L
 $M = 5.47$ kg

Estimated $H_c > 60$ cm
 $V_c > 24.6$ L.
 $M_c > 7.1$ kg

Experiment #71 10" Cadmium Tamped H/X = 86.3
88.

12/31/47

Beck
Fox
Crown
McFadon

until 2:00 used in installing and adjusting 10" cylinder — and in repairing #1 counter.

Suggpts. #3 91
#4 88

Instruments O.K.

11/19/48 Notes from Brown re H/X.

Dish 41 Gross 9.5614 gm
Tare 8.8251
Net 0.7363 gm oxide

Dish L-1 Gross 7.2442 gm oxide
Tare 6.8455
0.3987 gm

from sample Gross 102.9752
Tare 100.2404
Net 2.7351 gm

from sample Gross 100.2405 gm
Tare 98.7683
1.4802 gm

This gives H/X = 86.4 ave

	Solution Level	#1	#2		
1:59	Background	13	12.5		
	12.5	12.5	13.0		
	zero	11.5	12.0		
		11.5	12.0		
	14.6	38.5	41	.3	.29
2:28	19.8	143.5	151	.08	.08
	20.4	226.5	236	.051	.051
2:45	20.8	289.5	301	.04	.04
3:12	21.1	440	458	.026	
	21.1	Critical			Source in Source out

Conclusion: Critical at 21.05 ± .05

Handwritten signature

Drawback - Same as exp 70.

11/17/48 re. $21.05 + 0.93 = 21.98$ cm He bottom corrected
 $H/X = 86.3 \rightarrow 86.4$
 10" Stain less Tamped and Cd shielded.
 $DP = 1.35$
 $with H/X = 21.3 \approx 0.288$ qu/ce.
 $V_c = 11.15$ L.
 $M_c = 3.21$ Kg

HAPPY New Year
1949

Experiment # 72

10" Reactor, Tamped.

1/24/48 ⁴⁷

$H_x = 86.3$

Maxima

Crown

Max. H

Cellular

Trap points: #3 - ~~94~~⁸⁶ + 100
#4 - 94 + 100

Scale #3 - 100

#4 - 10

#5 - 2

RE - 25 ms.

I II
14.5 14.0

10:50 H = 0.2cm 13.5 13.5 #9 empty.
13.5 13.5 M⁻¹
13.5 13.5 I II

11:07 H = 5.0 21.0 20.5 0.643 0.659

Falling from #7

20 = 10.1 48.0 50.0 0.281 0.270

(2cm depth in #7)

26 = 12.5 100.0 104.5 0.135 0.129

Falling from #2

34 = 13.8 237.5 236.0 0.057 0.057

40 = 14.3 442.0 460.0 0.031 0.029

55 = 14.5 cm (same out) critical with C control and just above solution level.

DRAIN BACK - Same as #70 -

Conclusion 10" Reactor - $H_x = 80$, Tamped CRITICAL at $H = 14.5 \pm 0.05$ cm

11/17/48 DC 14.5 + 0.9 = 15.4 cm = He bottom connected.

11/16/48 DC $H_x = 86.3$ 86.4

10" Stainless Tamped.

Depth = 1.35

with $H_x = 21.3 = 0.288$ gm x/cc

$V_c = 7.80$ L.

$M_c = 2.25$ kg.

48
1/2/48

EXPERIMENT # 73.

Crown

10" Reactor. $H_{cr} = 86.3$ Untamped.

Macklin
Marfill
Callahan

Trip points - same as before

Scales 3 - 100

4 - 10

5 - 2

RE - 25m

	H	I	II	I	II
12:20P	H = 0.2cm	77.5	83.0		
		77.0	86.5		
12:30P	H = 0.2cm	80.5	81.0		
		80.5	81.0		
		80.5	81.0		
45	H = 7cm				
47	H = 12.2	151.5	155.0	0.531	0.522
52	= 15.0	207.0	212.0	0.389	0.382
57	= 16.1				
1:00	= 19.1	313.5	323.5	0.258	0.251
07	= 21.8	423.0	436.0	0.190	0.186
20	= 25.9	745.5	778.0	0.108 0.080	0.104
30	= 28.7	1391	1436	0.058	0.056
30	= 31.0	Critical with Cd control and gub in solution -			

Filling form #7 - H 7cm

Stop Filling form #1 to 15.0cm

Filling #6 to 16.1cm

Filling #4 to 19.1cm

Filling #3 to 21.8cm

Filling form #2.

Conclusion - 10" Reactor. $H_{cr} = 86$, Untamped. Critical at $30.31.0 \pm 0.05$ cm

11/17/48 31.0 + 0.9 = 31.9cm H_{cr} bottom corrected

11/20/48 H_{cr} = 86.3 → 86.4

10" Stainless Untamped.

sp gr = 1.35

with % X = 21.3 = 0.288 gm/cc.

V_c = 16.16 L.

M_c = 4.65 kg.

1/3/48

Area 3" storage cylinder = 46.8 cm²
 " 4" " " = 80.2 cm²

Measurement of Solution Height Prior to Dilution to H/x = 125.

Cross-section	4"	4"	3"	3"	3"	3"	4"	3"	3"
Manometer	1	2	3	4	5	6	7	8	9
h ₁	67.8	70.3	67.1	67.6	Full	67.7	Full	H/x=60	Full.
h ₂	40.3	38.1	40.9	40.6		40.4			
Manometer Δh	27.5	32.2	26.2	27.0		27.3			
Cylinder h _{cm}	60.3	70.6	57.4	59.2		59.5			
Volume cc	4835	5660	3455	2710		2800			

Present H/x = 86.3

Proposed H/x = 125

Present density = 1.35 g/cc.

It is required to add water to the present solution in the amount of 31.7% of present solution by weight or 42.9% by volume.

Estimated density at H/x = 125 is 1.244 g/cc.

Capacity 3" storage cylinder 294223 cc.
 4" " " 7349 cc

In order to effect dilution a 3" cylinder must contain $\frac{4223}{1.424} = 2958$ cc
 = 63.2 cm solution height.
 = 28.8 cm manometer "

" " " 4" " " " $\frac{7349}{1.424} = 5145$ cc
 = 64.2 cm solution height.
 = 29.3 cm manometer "

3" Cylinder #8 was isolated (H/x 62% full) and set aside (in the pit) a 4" cylinder was employed in position #8 and excess solution from #2 and #9 put in it.

The manometer readings on #2, 8, & 9 just before dilution were

	2	8 (4")	9
h ₁	66.7	62.4	66.6
h ₂	-41.3	-41.0	-41.4
Δh	25.4	17.4	25.2
cc in cyl.	55.6	38.2	55.1

Cylinders #5 (3") and #7 (4") were left undiluted and full of H/x = 86.3 solution.

Computed cylinder heights after dilution are:

		(equivalent 10" reactor height)		8" reactor
1	86.2 cm	(4)	13.8 cm	21.6 cm
2	79.5	(4)	12.7	19.8
3	82.0	(3)	7.4	11.6
4	84.6	(3)	7.6	11.8
6	85.5	(3)	7.7	12.0
8	54.6	(4)	8.7	13.6
9	78.8	(3)	7.1	11.4

* 11/26/48 From Cronin's notes - Re - ^{Corresponding} ~~near~~ H/X -

Sample L6 - 0.6009 gm U_3O_8 from
2.9675 gm solution.

Sample 26 - 0.5844 gm U_3O_8 from
2.8758 gm solution

gives ave. H/X = 123.2

Specific gravity = 1.250.

Wt % X = 16.4 = 0.205 gm X / cc of solution -

1/3/48

EXPERIMENT 74

Macklin
Mayer
Cronin
Calkin

10" REACTOR, UNTAMPED, $H/V = 125 = 127.4$

TRIP points #3 95x100 Scales 3 - 100
#4 91x100 4 - 10
5 - 1

I II Backgrounds @ .1 cm. R.E. - 25 mV
92.0 93.5 #1 77.0 #2 78.5

Cl	Time	Height	#1	#2	% #1	% #2	Remarks
#9	2 ⁴⁵	0.1 cm	76.5, 77.5	78.0, 79.0	—	—	#9 Empty @ 2 ⁵⁰
#8	3 ⁰⁸	9.0	106.	106.5	.727	.738	#8 Empty @ 3 ¹⁰
#6	3 ¹²	16.3	211	219.5	.367	.358	#6 Empty @ 3 ¹²
#4	3 ²⁹	23.9	422.5	439.5	.182	.179	#4 Empty @ 3 ²²
#3	3 ⁴¹	28.8	(682.5)	(712.)	(.113)	(.110)	ROD IN
			821.5	855.5	.094	.092	4.9 cm taken from #3
#2	3 ⁵¹	31.0	1343.5	1394.	.057	.056	
			Source Pulled				
"	4 ²⁶	31.9	with source out		NOT critical but close		S=32
"	4 ¹⁴	32.2	"	"	"	"	S=44
"	4 ¹²	32.5	"	"	"	"	S=44
"	4 ²²	32.9	"	"	"	"	S=53
"	4 ²⁴	33.1	"	"	"	"	S=60
"	4 ²⁷	33.6	Critical with 11 cm Cd in soln.		S=∞		
DRAIN TO							
"	4 ²⁹	33.4	CRITICAL WITH ROD OUT.				

Conclusion → Est. criticality $33.4 \pm .05$ cm. 10" Reactor Untamped, $H/V = 125$

1/17/48 de $33.4 + 0.9 = 34.3$ He bottom cancelled

1/18/48 de. $H/V = 127 = 123.2$

10" Stainless Untamped.

$\rho_p \rho_v = 1.250$

with $\rho_X = 16.4 \equiv 0.205$ gm/cc.

$V_c = 17.38$ L.

$M_c = 3.56$ Kg.

EXPERIMENT 25

1/5/48

10" Reactor Tamped

H/x ~ 127.4
125

Fox
Macklin
Visner
Callahan

Trip points

3 90 x 100
4 90 x 100

Scales 3 - 10
4 - 10
5 - 10
RE - 50

Backgrounds.

no sol. # 1 - 12.5 # 2 - 14.0
Cm. # 1 # 2
H: 0.2. 15.0 16.0
15.0 15.0

	H =			M ⁻¹	I	II
10:40 P	5.0	18.0	17.0	0.834	0.982	
48	10.1	37.0	38.0	0.406	0.408	
55	12.6	64.5	64.5	0.232	0.237	Filling for #2
11:00	14.0	106.5	111.0	0.141	0.140	
1:09	14.9	193.0	200.0	0.078	0.078	
20	15.6 (room in)	399.0	419.0	0.038	0.037	

= 16.0 (room out) Critical not fully tamped.
= 15.9 " " tamped, 8cm of Cd control rod below insertion level.
At 15.9 point Cd control rod appeared to have little effect - i.e. 16.0
Cm solution was critical with rod in + not completely tamped; 15.9 was critical. - then began to withdraw rod.
= 15.6 396.0 413.5 0.038 0.037 Rod out.
142 = 15.4 321.5 333.0 0.047 0.047 Rod in.

- Conclusion -
- 10" Reactor, Untamped, H/x = 125 critical at 15.9 ± 0.05 cm.
 - at M = 25 - Cd control rod = 1.5 mm of solution in 10" reactor.
 - It is apparent, from some observations here, that with a 10" reactor the imprecision of eight glass readings (ca 0.05 cm) represents a the condition between critical & non-critical. For example:
Sight-glass = 15.9 cm - Condition: Sub-critical, tamped, control rod out -
= 15.9 " - " Critical, tamped, control rod 8cm below surface -
 - At this solution concentration the density and viscosity are sufficiently low to use 6 psig air pressure. A higher pressure, 10 psig, appeared to cause liquid level to increase 3 or 5 mm after clearing value. This needs to be reflected! =

Solution drained base as before -
11/17/48 15.9 + 0.9 = 16.8 cm Hc bottom covered
11/20/48 H/x = 123.2
10" Stainless, tamped.

well % x = 16.4 ± 0.205 g/cc
ρ_{gr} = 1.25
V_c = 8.5 L
M_c = 1.74 kg

EXPERIMENT 7b

1/5/48

8" REACTOR TAMPED

$H/X \approx 125$ 127.45

		I	II	M^{-1}		
0	Fry					#3 - 100
2	Viamu					#4 - 10
3	Maxlin	11.0	12.0			#5 - 2
2	Callihan					RE - 25
	3:05P H=0.-G.	12.0	11.0			Filling for #2.
		11.5	11.0			
		11.2	11.0	I	II	
	=5.0	15.0	14.5	0.787	0.758	
	=11.0	24.0	23.5	0.492	0.468	#1 - Empty. Filling for #2.
	=16.0	36.0	37.0	0.328	0.297	
3.45	=19.0	52.5	53.5	0.225	0.206	
50	=21.9	95.0	96.0	0.125	0.115	
4:00	=24.0	233.5	243.5	0.051	0.045	
12	=24.7	421.0	435.0	0.028	0.025	(Source in).
	24.9	Critical	Rod in, not completely tamped			(Source out).
	24.7	"	9cm Control rod in -			(" ")
	24.6	"	9" " " "			(" ")
	24.4	Slightly sub critical				(" ")
	24.1					Source out.
	24.25					Source in -

Conclusion - ① In 8" reactor source ≈ 1.5 mm.
 ② 8" Reactor - $H/X \approx 125$ - Tamped - Critical at 24.5 ± 0.1 cm.
 ③ at 4:12P - H = 24.7 source in ≈ 24.55 source out $M = 40$ - (sub critical).
 later H = 24.6 " " Super critical -
 This indicates again, as did Exp. 75, a severely rapid drop to the $M^{-1} - H$ curve - or a large inaccuracy + irreproducibility in the pipet glass readings - D.C.

Drain back - see pg. 50.

11/17/48 24.5 + 1.5 = 26.0 cm = Hc bottom cancelled

11/20/48 $H/X = 127.2$
 8" Stainless, Tamped.
 $\rho_{sp} = 1.25$
 with $\rho_{ox} = 16.4 \approx 0.205$ gm/cc.
 $V_C = 8.43$ L
 $M_C = 1.73$ kg

EXPERIMENT 77

1/6/48

8" Reactor - UNTAMPED - $H/X = 125.127$ WILLIAMS
FOX
CALLAHAN.TRIP POINTS - 3 - 89 x 100
4 - 91 x 100Scales 3-10
4-100
5-2
RE-25ml1:50P
:58

H=0.2 cm

	I	II	Filling from #9	
	77.5	77.0		
	78.0	76.0		
	<u>77.8</u>	<u>76.5</u>		

= 1.0

2:15

= 14.5

110.0

109.0

	I	II
	0.707	0.707
	0.512	0.505
	0.454	0.445
	0.436	0.427
	0.428	0.409
	0.427	0.411

#9 Empty - Filling from #8

#8 Empty - Filling from #6

Empty #6 - Filling from #4

#4 Empty - " " #3

#3 " ; " " #2

#2 " " " #1

30

= 26.1

152.0

151.5

40

= 37.8

172.0

172.0

53

= 49.4

178.5

179.0

3:10

= 67.8

181.5

187.0

25

= 80.2

182.0

186.0

30

= 0

79.5

79.0

DRAIN BACK

#1	20	cm in 8" reactor = 15.8	cm in 9" reactor.
#2	20		15.8
#3			
#4	10		7.9
#6	10		7.9
#8	20		15.8
#9	Dead Volume -		Dead vol.

Conclusion - 8" Reactor, Untamped, $H/X = 125$ - Not critical at ∞ length etc.
 $H = 80.2 + 1.5 = 81.7$ cm
 $H/X = 123.2$ as preceding page.
 $V = 26.49$ L
 $M = 5.43$ kg.

Estimated $H_c = V_c = M_c = \infty$

Experiment 78

9" reactor - Cadmium Tamped.

$k_{eff} = 1.25$ 127.4

1/7/48.

Back
for
cross
reference.

Trip points #3 and #4 both on 90.
All instruments respond properly.

	Solution Level.	Counting Rate.		Cp/c.		
		#1	#2	#1	#2	
9:10.	Background	13.5	14			
9:15	Zero - 0.5.	11.5	11.0			
		11.5	12.0			
9:28	16.4					# 2 empty. (15.9)
9:34	24.4	51.5	53.5	.22	.22	From # 4. (8 cm)
9:43	28.0	91.	92.	.124	.13	
9:49	30.0	188	196	.061	.061	
9:55	30.7	285	299	.04	.04	
10:01	31.0	381	415	.029	.029	Source in.
	30.8	Super-critical with source out.				

There were curious and anomalous effects here. The solution with source removed was quite super-critical - the cadmium rod had to be inserted several centimeters. With the source inside the solution the assembly was definitely below critical.

Another effect noted here: the assembly was definitely less critical with the top tamper in contact, than when 1 mm and more away, thus, raising the top tamper made the assembly more critical.

The effect of source position was investigated: Solution level 31.0 cm.

Source Position	Rod Position	Meter (100 scale)	
Touching bottom	out	40.	} Lowest level of activity is with source holder 6 cm from bottom. Touching bottom and 12 cm up gives same reactivity.
6 cm from bottom	out	35.	
12 " "	out	40	
From this point on, source was raised and Cad. Saf. Rod inserted to maintain level at 40 on #4 (100 scale).			
14	36 (3 cm in soln)	40	} Position of greatest activity = Source 24 cm from ^{"touching"} bottom. Here 7.5 cm of safety rod required to hold level at 40 on #4.
16	34 (5 cm in soln)	"	
18	32.7		
20	32		
22	31.5 (7.5 cm in soln)	40	
24	31.5		
26	31.5	40	

Source position	Rod position	Meter Level (#4)	
28 (from bottom)	32.2	40	Here actual source is 1cm inside top tamper.
30	32.5		
34	34.0		
36	34.	40	Here actual source is at top of top tamper.
40	34.7		
45	35.		
65	35.2 (3.8cm in pole)	40	} Thus, with source completely removed, 3.8 cm of rod is required to hold level at the activity with source at bottom and rod <u>out</u> .
100 (ie removed)	No change.		

with source out, rod withdrawn to note effect:

out	36 (3cm in pole)	Level rose from 40 to 75 in 110 seconds.
out	35 (4cm in pole)	" fell from 75 to 50 in 400 seconds. rod could not be withdrawn.

with rod 3cm in pole and source out, assembly behaved exactly as ~~is~~ super-critical
with rod out and source at bottom, assembly was definitely not critical.
In all cases top tamper was kept in contact, though level of pole rose or fell 1-1.5 cm as source & rod were moved in or out.

Conclusion:

The assembly, with source out is critical at 30.8 ± 0.1 cm. } some amount of
The assembly, with source in is definitely sub critical at 31.0 cm } resolution involved.

11/17/48 DC $30.8 + 1.2 = 32.0$ cm = the bottom centered.

11/26/48 DC 4" Stainless Tamped ~~with~~ C shield

$$HX = 127.4, 123.2$$

$$p_{gr} = 1.25$$

$$\text{well } \rho_{ox} = 16.4 = 0.205 \text{ gm/cc.}$$

$$V_c = 16.4 = 13.13 \text{ L}$$

$$M_c = 2.69 \text{ kg.}$$

Experiment 79. 9" 1/7/48 Tamped - $\frac{11}{4} = 127.4$

Beck
Fox
Crom
Metelson

All instruments check. OK.

It is intended to count each level with the source in two positions:
(a) touching bottom and (b) a position of highest activity.

with source moved to position to give highest level.

Time	Selection level	Source holder Position	1		C - C ₀		C ₀ /C	
			#1	#2	#1	#2	#1	#2
	Background	0 (touching bottom)	14.5	14.5				
1:24	0.3	0	13.5	13.5				
1:32	10.1	0	29.5	30.0	.606	.606	.455	.450 From #4, (8) & #2
		0.8	27.5	29.0			.272	.272
1:48	14.0	0	49.5	49.5	.278	.278	.272	.272
		1.7	46.0	49.5				
2:05	16.1	0	46.0	49.5				
		0	72.5	80.0	.17	.15	.186	.170
		2.0	72.	83.				
2:30	18.0	0	170.5	179.5	.062	.062	.079	.075
		8.5	191.0	206.5	.056	.051	.07	.065
2:38	18.5	0	268	292.	.039	.036	.05	.046
		10.	346.5	385	.03	.027	.039	.035
3:00	18.7	0	324	361.	.032	.029	.042	.037
		14.5	544	606	.0186	.0169	.025	.022

18.8 ^{Above} Critical with source out.

Conclusion: Critical at $18.7 \pm .1$ with source out.

New Technique in handling measurements and manipulating data give better approach to critical point. See Graph Exp 79.

11/17/48 $18.7 + 1.2 = 19.9$ cm = He with bottom corrected

11/20/48 $H_v = +27.4$ 123.2

9" Striker, tamped.

$A_{gr} = 1.25$

with % $X = 16.4 \approx 0.205$ gm x / cc.

$V_c = 8.16$ L.

$M_c = 1.67$ Kg.

Exp. 80. 9" Un-Tamped - $H/x = 125$ 127.4 1/7/48.Back
Jap.
Crown
McLendon

Eveninging O.K. —

	Solution Level	Source Level	#1	#2	C ₀ /C		C - C ₀	
					#1	#2	#1	#2
	Zero. 0.5	0	68.5	77.5				
3:40		0	68.0	77.0				
3:50	25.0	0	224.	257.	.34	.36		
		9.5	235.	260			.6	.55
4:05	40.	0	402	442	.17	.174		
		13.5	544	605			.174	.19
	44.8		478	529.	.142	.147		
			689	771			.16	.144

Conclusion: does not go critical, but data indicate that the 9" un-tamped might go if a longer cylinder were available.

Drain back:

	Ht. in 9" Reactor	C ₀ CKB	in 7" reactor
1	13.2 cm	15.8	26.1
2	15.8 "	15.8	26.1
3		—	
4		7.9	13.0
6		7.9	13.0
8	15.8	15.8	26.1
9	Dead Volume	d.v.	d.v.

11/30/48 DC

$$H = 44.8 + 1.2 = 46.0 \text{ cm}$$

$$H/x = 123.2 \text{ (see following page)}$$

$$V = 18.88 \text{ L}$$

$$M = 3.87 \text{ kg}$$

Estimated: $H_c = 770 \text{ cm}$
 $V_c = 28.7 \text{ L}$
 $M_c = 5.9$

Exp. 81 7" tamped $N_H/N_X = +25127.4$ 1/8/48

Crown
Fox
Moffitt
Midway

8²⁰ Counts 8,8⁻
792,8⁺

Trips: #388 #4,90 on 100 scale.

In this experiment, counts will be made in two positions @ With true source 8cm off bottom & ⑥ With source at point of highest activity. Ion chambers moved back to 3ft from original position to reduce power level at near critical assembly.

Instrument positions: #3 - 100 scale, #4 on 10 scale #5 on 2 scale. Read on 50 scale

Background Readings

#1	#2	Ave #1	
9.25	9.75	9.50	
9.75	9.75	Ave #2	9.75
9.50	5@8cm 9.75		5@Max

Time	Solu Level	#1	#2	%/c ₁	%/c ₂	#1	#2	%/c ₁	%/c ₂
From #6		#1	#2	%/c ₁	%/c ₂	#1	#2	%/c ₁	%/c ₂
10:25	10.0	15.5	15.75	.613	.618	(Probably above max)			
10:48	#6 Empty Filling from #4	H = 13.0 cm							
10:52	17.7	25.75	27.0	.369	.361	(Probably @ max)			
11:07	22.7	33.5	36.5	.284	.267	(None detectable flat minimum)			
11:20	27.5	44.0	30.0	.216	.195	44.5	49.5	5@ 3cm above orig	
	#4 Empty Filling from #2								
11:28	32.5	64.0	72.0	.149	.136	65.0	74.0		
11:45	37.5	122.5	141.5	.0776	.0671	130	150.5	Source 8cm above orig.	
		Source 13cm up from original.		%/c ₁ = .073	%/c ₂ = .065				
11:04	40.1	262.5	302.	.0362	.0323	683.5	7.58.	.0137	.0123

Critical @ 40.4 ± 0.05 cm.
with Control Rod @ 30 cm.

Multiplication with rod @ 10 cm. 152.0

Drainage Same as previously.

11/17/48 DC 40.4 + 1.9 = 42.3 cm - No bottom corrected.
11/17/48 DC $N_H/N_X = +25127.2$
7" stainless tamped.

with $\rho_{0X} = 16.4 \approx 0.205$ g/cc
AP gr. = 1.25
Vc = 10.502
Mc = 2.15 kg.

Exp #82 6 1/2" Tamp. $N_{14}/N_x \approx 127.4$
 ≈ 125 1/8/58

Cronin
 Fox
 Morlitt
 Murray

Ready to go. @ 3:17 P.M.

All counts taken with source as shown.

Time	Soln.	Source 8 cm (<u>true</u>)	#1	#2	B/c ₁	B/c ₂	Remarks	
3:17	1.2 cm.	8 cm	8.75 9.0	9.25 9.12	} Use #1 #2	9.0 9.25	Dr From 9.	
Solution Levels H for 6 1/2" cyl		#1	#2	#4		#6	#8	#9
			30.5	30.5	15.2	15.2	30.5	du.
3:22	Filling from #8.							
3:37	15.0	8 cm	18.0	18.5	0.500	0.500		
3:45	30.8	"	28.5	32.0	.316	.289	#2 Empty	
<p>NB → At a height of approximately 38 cm, the tamper motor jammed & could not be operated with the switches from the control room. Upon drainback, we tried again & the thermal cut-out opened. No fuses were blown. The top of the cylinder was tightened up with no success. The main coupling was loosened & the top two split bearing loosened. The motor then gave satisfactory operation. The tamper was not jammed in the cylinder. The trouble appeared to be due to a tight bearing at the top but this is by no means certain.</p> <p>The dead volume was then filled from #9, & #2 reemptied to fill the cylinder to a height of</p>								
4:45	31.1	"	27.5	29.0	.327	.319		
<p>Since check on counting was satisfactory the experiment was continued, filling from #6</p>								
4:51	44.0	8 cm	38.5	39.0	.233	.237		
<p>#6 Empty - @ 44.0 Filling from #7</p>								
4:58	55.3	"	51.25	54.5	.175	.170		
5:04	50.4	"	56.5	59.0	.159	.157		
<p>39 - 17 above original position</p>								
5:24	70.0	8 cm	97	105	.083	.084		
<p>39 cm above original.</p>								
5:40	75.0	8 cm	107	113	.084	.082		
<p>6 cm above original</p>								
			194	212	.076	.077		
			253	279	.035	.033		

→ Not critical at max height available. Probably critical @ 78.0 cm.
 Drainback into original container as above. (See next page)

Note: In taking #4 base, drained base too much into #4
 Solution heights need to be remeasured before
 starting next experiment. ←

6 1/2" Stainless - Tamped -
 $H = 75.0 + 2.2 = 77.2 \text{ cm}$
 $H_T = 123.2$; $\text{spgr} = 1.25$
 $\text{wt} \% X = 16.4 = 0.205 \text{ gm} / \text{cc}$
 $V = 16.52 \text{ L}$
 $M = 3.39 \text{ kg}$

Estimated $H_c = 78 \text{ cm}$ $78 + 2.2 = 80 \text{ cm}$
 $V_c = 16.7 \text{ L}$ 17.1 L
 $M_c = 3.42 \text{ kg}$ 3.50 kg

Project - Dilute to $H/x \approx 175$ *

$$\Delta = (.377) \left(\frac{1}{17.281} \right) d \cdot V$$

$$= 0.294 d \cdot V$$

$$= 0.368 V$$

Starting $\%x = 127.4$ $d = 1.25$

Cylinders adjusted so that full height at next dilution shall be < 88 cm (91 cm max cap.)

manometer shld be $< 88 \left(\frac{1.25}{2.96} \right) \left(\frac{1}{1.368} \right) = 27.2$ cm $> \Delta H$

(11) 46.9 cm^2 3' cap
(193) 80.4 cm^2 4' cap

Cyl. No.	Solution #	Solution Heights After Redistribution					Vol $H_2 O$ Padd	Total Vol.
		H_1	H_2	ΔH	Vol	$\Delta H \left(\frac{2.96}{1.25} \right)^2 \text{ area}$		
4	# 1	66.8	41.2	25.6	4940		1818	6758
4	# 2	66.8 66.5	41.2 41.4	25.6 25.1	4840		1781	6621
3	3	67.5	40.5	27.0	2995		1102	4097
3	4	66.8	41.4	25.4	2820		1037	3857
4	5	67.1 67.1	41.4 41.4	25.7	4960		1825	6785
3	6	67.1	41.4	25.7	Full of $\%x = 127.4$ (Storage)			
4	8	67.5	40.5	27.0	5210		1917	7127
3	9	67.3	40.9	26.4	2930		1078	4008

- ① Arranged to pull source into attic - Installed new stainless steel cable.
- ② Summarized data in new notebook "Summary of Solution Experiments" - plotted data.

* 11/26/48 From 1954 Book #22 - entry dated 11/21/48.
 Solution specific gravity $1.1864 = 1.19$
 average $H/x = 174.1$ 174.
 ~~≈ 12.4 wt %~~
 Wt % $x = 12.4\%$
 ≈ 0.148 gm/cc solution.

Williams

$M/\bar{x} \approx 175$

Crossin
Mc
Callahan

Trip points # 3 - 84x100
4 - 81x100

Scales # 3 - 100
4 - 10
5 - 2
RE - 25ms.

1:20P	Filling for #9				
1:22P	H = 0.7cm	I	II	I	II
		10.5	11.0		
		11.0	11.5		

} Source 4cm from bottom

H in 6 1/2 reactor	#
32.7cm	21.5
32.1	21.1
19.8	13.0
19.0	12.5
33.4	22.0
35.0	23.0
19.6	12.9

		2.5	3.5		
		10.0	12.0		
		10.5	11.5		
	= 3.4	14.5	14.5		
	= 10.1	14.5	16.5	0.724	0.649
	= 21.7	17.5	20.5	0.600	0.561
	= 31.7	20.0	22.5	0.525	0.511
	= 41.7	21.5	25.0	0.488	0.460
	= 52.0	22.5	27.0	0.467	
	= 59.9	21.5	27.0	0.488	0.426
	= 70.1	24.0	26.5	0.437	0.434

Source in attic.

Source 4cm from bottom -

#9 empty; filling from #4.

#4 empty; filling from #8.

Filling from #2

Conclusions
11/30/48 DC

6 1/2" - $M/\bar{x} \approx 175$, Tamped - Not critical at ∞ length - $M_i \approx 2.5$ at 70cm.
 $H = 70.1 + 2.2 = 72.3$ cm
 $M/\bar{x} = 174$; $R_{pg} = 1.19$
 $M/\bar{x} \% \bar{x} = 12.4 \approx 0.148$ ft x / cc
 $V = 15.47$ L
 $M = 2.29$ kg.

Estimated - $H_c = M_c = V_c = \infty$

64
1/13/48

EXPERIMENT 84

Fry

8" Reactor, Untamped, $M/x = 175$

Williams
Gross
Callahan

Trip points same as before

Scales # 3 - 100

4 - 10

5 - 2

R.E. 25 mil.

Time	Filling from #9	I	II	M-1	II
3:35P	H = 0.6 cm	86.0	83.0		
		84.0	84.5	I	II
	= 2.0	85.0	83.8		
4:05	= 20.6	145.5	155.5	0.584	0.538
4:16	= 39.9	171.5	186.0	0.495	0.450
4:20	= 42.7				
4:26	= 55.1	169.0	187.0	0.503	0.468
4:34	= 67.5	174.5	186.5	0.487	0.450
4:44	= 84.3	171.0	180.5	0.497	0.465
5:07P	= 0	87.5	84.0		

9 Empty, Filling from # 8

8 Empty, Filling from 5

5 Empty, Filling from # 4

4 Empty, Filling from # 3

3 Empty, Filling from # 1

11/30/48

$H = 84.3 + 1.5 = 85.8$ cm

2c

$M/x = 174$ (see following page)

$V = 27.82$ L.

$M = 4.12$ kg.

Estimated $H_c = V_c = M_c = \infty$

Conclusion: 8", Untamped, $M/x = 175$ - Not critical at ∞ length.

Drain Bank

1	21.5 cm in 8" reactor.	= 17 cm in 9" reactor
2	21.1 " " " "	= 16.6 " " "
3	12.5 " " " "	= 9.8
4	22.6 " " " "	= 9.9
5	22.4 " " " "	= 17.7 " " "
6	Full $H_c = 127$.	
7	" " = 86.3	
8	20 cm in 8" reactor.	= 15.8 " " "
9	Dead volume.	

EXPERIMENT 85

1/13/48

Cross

8" Reactor, Tamped, $H/X = 175$

Mullins
37x
Collins

Trip point same as 28.3

Seals - #3 - +0.50

#4 - 10

#5 - 2

RE - 25mm

		I	II		
J:24P	H = 0.1cm (-)	9.5	11.0		
		9.0	10.5	M	
		9.3	10.8	I	II
J:32	H = 5.1cm	12.0	13.5	0.775	0.800
38	= 9.9cm	16.5	18.5	0.564	0.584
50	= 15.0	22.0	26.0	0.422	0.415
56	= 22.0	40.0	47.5	0.232	0.228
6:04	= 26.0	76.5	90.5	0.124	0.119
12	= 28.0	166.0	200.5	0.057	0.053
22	= 29.0	437.5	532.0	0.021	0.020
50	= 29.2	766.5	956.5	0.012	0.011

Filling jar #1.

#1 Empty Filling jar #2.

Source in

SOURCE
4cm
from
bottom
of
col.

Removed source, ^{float} level went through minimum, then maximum level started to increase necessitating putting control rod in 14cm. At this control position, level continued to increase C_c linearly with time for 4¹/₃ min. Level of solution during this time is 29.0 - same quantity as at 6:50P.

Drain back to 28.8cm, source out, with ^{control} rod at 8cm in solution - level rose linearly but at less rate than above.

Drain back to 28.7, source out, with 3cm control rod in, level rose linearly but at still less rate -

Drain back to 28.6cm source out, level still slowly rising - with 3cm control rod
Drain back to 28.5 " " control rod out, level fell slowly.

Replaced source (to 4cm) raising tamped correspondingly level in sight glass = 28.7

7:30 = 28.7 327.5 399.5 0.028 0.027 source in -

Removed source - solution level dropped to 28.5 - re-tamped - control rod out - level fell slowly as above

DRAINBACK - see pg 64.

Conclusion ① 8", Tamped, $H/X = 175$ Critical at 28.6cm source out -

② " " 29.3 " " in, from source - extrapolated value

11/17/48 28.6 + 1.5 = 30.1 cm - He bottom corrected

11/20/48 $H/X = 174.5$

8" Stainless Tamped.

$\rho_{90} = 1.19$

$\rho_{175} X = 12.4 \approx 0.148 \text{ gm} / \text{cc}$

$V_c = 9.76 \text{ L}$

$M_c = 1.44 \text{ kg}$

66 1/19/48

Experiment 86

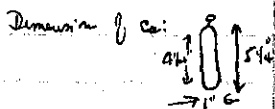
Visner
Joy
Maddin
Callihan

To examine effect of moving the displaced solution ("hole") which occurs, in the usual experiment as the source is moved in and removed from the solution.

Method - 8" Reactor, HK=175, tamped except top - Similar to #85 except absence of top tamped. A replica of the source holder - stainless steel ca 5" long, 1" diameter, has been prepared and can be moved in the reactor in a manner analogous with the source. Replica is 4.5 cm from reactor ^{axis} center (radially) and source bob is 9.5 cm from ^{axis} center.

With replica out of solution the experiment will be started in the usual manner -

Volume of source - 60cc
" " source replica - 65cc.



TRIP points #3-92x100, #4-92x100
Scals #3-100; #2-10, #5-2, 2E-50 mo.
Source 4 cm from reactor bottom.
#9 Empty.

Time	Filling level volume from #9	I	II	I	II
11:25 A					
11:30 A	H=0.7cm	13.0	14.5		
	(Level)	13.0	14.5		
12:05	H=10.0	13.0	14.0		
20	=20.3	26.0	30.0	0.500	0.485
30	=25.2	43.0	44.0	0.305	0.296
35	=29.0	100.0	110.0	0.130	0.132
40	=30.5	223.0	254.0	0.061	0.057
50	=31.3	810.0	913.0	0.016	0.016

Filling from #8
#8 Empty - Filling from #5

(Control rod = 7mm)

Time	Source out	Control rod height	Power level
1:15	31.1	15 cm from bottom	38 on #4
1:16	31.0	20 cm	45 on #4
		19 cm	38 on #4
1:25	30.8	Not critical	
1:28	31.1	Critical	13.5 from botto. (Power level 38)
1:38	30.9	Critical	21.5 " " (Power level 38 on #4)
1:45	31.25	Critical	"

Dummy inserted, subcritical, Source inserted in effort to raise level, rod also taken out.

Time	Source out	Control rod in	Power level
2:05	32.0	Both bobs in, control rod in	Not critical
2:10	32.5	Dummy in, source and c. r. out	Not critical
2:25	32.7	" " " "	Not critical
2:28	33.1	both bobs in, Source out Cd Rd at 24 cm from botto	CRITICAL

Not meas. with both bobs in

Here length of Bob = 13.4 cm

2:35 H = 33.1 ^{Dummy in} Source out. Critical source out Cd Rod at 17.5 from bottom power level at 38 on #4. Bot of Dummy at (11-1) cm from bot of reactor.
 { Also critical will bot of bob (7.5-1) cm from bottom having gone thru a minimum Cd Rod plane.
 { Bottom of bob is (9.2-1) from bottom of reactor.
 { Cd Rod 18.5 cm from botto. Critical.

Bot of bob from bot of reactor cm.	Cd Rod from bottom cm.
------------------------------------	------------------------

	10	16.7	17.5	32.70cm	
	6.5	13.2	17.5	32.70	
	8.2	14.9	18.5	32.73	
	3.5-1 = 2.5	9.2	4.5	32.38	
	15.5-1 = 14.5	21.2	5.0	32.39	
	13.0-1 = 12.0	18.7	15.0	32.64	
3:00	6.0-1 = 5.0	11.7	14.5	32.63	
3:03	6.0-1 = 5.0	11.7	19.2	32.65	H = 33.0 ^{Dummy in} Source out.
3:07	1-1 = 0.0	6.7	7.5	32.13	H = 32.8 ^{Dummy in} Source out.
	18.0-1 = 17.0	23.7	4.0	32.04	$\frac{17.4}{1.94}$
	18.0-1 = 17.0	23.7	13.0	31.98	H = 32.5 ^{Dummy in} Source out.
3:15	20.4-1 = 19.4	26.1	18.0	31.64	H = 32.0 ^{Dummy in} Source out.
3:30	28.1-1 = 27.1	33.8	9.5 (Dummy bot)	31.20	H = 31.5 ^{Dummy in} Source out.
					H = 30.9 ^{Dummy in} Source out.
					30.8 ^{Dummy out} Source out.
3:35	33.8-1 = 32.8	39.5	15.8	30.83	H = 31.1 ^{Dummy out} Source out.
	57.5-1 = 56.5	63.2	16.5	30.86	H = 31.05 ^{Dummy out} Source out.
	34.5-1 = 33.5	40.7	15.8	30.83	H = 31.05 "

Height of center of bob above bottom of reactor (cm)

Equivalent critical height with source, rods, reflector and control rods completely removed.

Exp. 86 (Cont)

Conclusions:

- ① A plot was made of the position of the source holder replica vs. effective solution height at criticality (i.e. a sight glass reading at criticality was corrected for the displacement of the replica, and for the amount of central rod required at that condition). This plot shows a minimum of solution required when the center of the replica is at center of solution (axially). (This solution height = 32.73 cm). With the center of replica at 6 cm from bottom of reactor (usual source position - bottom of replica touching bottom of reactor) $H_s = 32.13$ cm. With replica raised so distance $H_s = 30.86$. The maximum effect of this void corresponds to 1.87 cm of solution, with the void at this ~~out~~ radial position from the reactor axis (4.5 cm). The effect due to motion of void within solution is greater than its removal from the solution, i.e. displacement (position) effect vs. density of active material effect.
- ② Reference to the multiplication curve for this experiment, after its correction for source holder displacement, shows the above ① to overcorrect the "drop" in the extrapolation. This is probably due to the replica being nearer the reactor axis (during the ^{evaluation} ~~construction~~ of the displacement effect at criticality) than was the source (in its holder) during the multiplication measurements.
- ③ Critical height in this experiment = 30.9 cm - without top tamper
 " " Exp. 85 = 28.6 " - with top tamper.
 Top tamper is equivalent to 2.3 cm of solution under these conditions.

For 8" Reactor, Tamped - except top, $H/X \approx 175$

Cromin
William
Leather-

Purpose - To re-run Exp. 86 using the same π source (ca 1/2 curie) as usual but with it removed from the (60cc) stainless steel case. The source was heavily coated with paraffin & attached to directly to the cable. The source diameter is ca 7/8" (= 2.1cc). The source is 9.5 cm (radially) from the axis reactor; (this quantity is guess & to be uncertain because of the source cable is not taut due to buoyance of solution, etc). This experiment ~~is~~ shown) distinguish between the effect, at the high multiplication end of the curve, of a void and of source displacement. Source is 4cm from bottom of reactor.

TRIP Points - #3 - 85 x 100

#4 - 86 x 100

Scale #3 - 100

#4 - 10

#5 - 2

RE - 50 ms.

10:55 A Filling dead volume for #9

11:00 H = 0.6 cm I 16.5 II 15.5 #9 empty.

15.5 16.0

16.0 15.8 I M II

Filling from #8

11:16 H = 10.5 cm 12.0 12.5

12.0 12.5 1.33 1.26

This indicates source may have moved since in #86, at 10cm C-Co.

:30 = 15.1 17.5 18.0 0.914 0.878

= 20.3 28.0 29.0 0.572 0.545 #8 empty; Filling from #5.

:50 = 25.4 44.5 51.5 0.323 0.307

12:01 P = 28.0 89.0 96.0 0.180 0.165

:07 = 29.0 139.0 145.5 0.115 0.108

:18 = 30.1 248.5 328.5 0.054 0.048

:27 = 30.5 601.0 648.5 0.027 0.024

:50 = 30.8

Critical with ^{1cm} #8 control rod below solution surface. {Source raised to above max. point now 2.4 cm from bottom, after this pt.

With reactor critical the large source holder replica was lowered into the solution - The reactivity increased, due probably to the tamping effect noted in #86, then as the slug entered the liquid, the level dropped rapidly & went through a minimum as the slug passed the ^(vertical) center of the solution.

Replaced source at 4cm from bottom of reactor. Drained back to 30.5cm.

2:30 P H = 30.5 535.0 578.5 0.030 0.027

542.0 584.0

= 30.5 134.5 142.0 0.119 0.111

With 65cc stainless steel source holder replica at the center of reactor - giving minimum multiplication. These values of M^{-1} , compared with above $M^{-1} - k$ curve shows the stainless slug to be worth about 1.5 cm solution at this reactivity. This checks yesterday's value of 1.87 cm at criticality.

- Conclusions:
- ① Using source of small volume ($\approx 2\text{cc}$) inside solution (4cm from bottom of reactor) the usual multiplication curve extrapolates to a critical mass value 1mm greater than that actually observed (30.8cm vs 30.9). Today's values check the value obtained yesterday with both source and replica completely removed.
 - ② As source is raised from the 4cm position when reactor is near critical there is a small rise in activity, followed by the usual decrease. There is no initial fall.
 - ③ With reactor near critical the ^{rod} source replica was submerged with a great repressing effect. At $M \approx 10$, 65 cc of void is equivalent to removing about 1.5 cm of solution. Checks yesterday's value of 1.87 cm at criticality.
 - ④ Source was suspended on end of 15 mil stranded stainless cable. About 50 cm above it was a counterweight to take up slack. Cable between source and counterweight tended to kink and source probably moved as solution was being added. No serious effect was noted in the data. It seems possible that this sized source can be used satisfactorily if "void" effect is so undesirable.

Job

Experiment 88.

1/20/48 71

William
Crosby

8" Reactor. $H/X \approx 175$, Tamped West Top.

Cellular

Source mounted outside reactor in tamper

Purpose: To reexamine the effect of mounting the source, ^(Ca²⁵²Curio) outside of the reactor in ^{the} tamper, on the shape of the multiplication curve.

Method: Source is mounted in its usual stainless steel holder - (5 1/4" x 1") (60cc) outside reactor, in water tamper, 1 cm ~~out~~ away from outside reactor, 13 cm above bottom of reactor.



	I	II			Temp PTS	Scales
3:36 P	$k=0.1$	7.5	8.0		3	-85 x 100
		7.5	8.0	M^{-1}	4	-86 x 100
				I	5	2
4:45	=10.1	6.0	5.5		RE	25ms.
50	=15.4					
50	=18.1	7.5	7.0	1.00		1.14
55	=20.6	13.0	12.5	0.576		0.640
4:03	=26.5	33.5	38.0	0.224		0.210
1:10	=28.1	53.0	55.5	0.142		0.144
2:25	=29.2	90.0	98.5	0.083		0.081
3:0	=30.1	210.0	233.0	0.036		0.034
4:0	=30.5	330.5	363.0	0.023		0.022

These data are following, now those of Exp. 87 & extrapolated to the same critical point. It is unnecessary to carry the activity further. Raising the source from this position lowers the activity, lowering it decreases the activity slightly.

Source lowered to level of reactor bottom.

5:00	$k=146$	14.5	13.0	0.690	0.692
	= 20.5	16.5	15.0	0.606	0.600
				0.489	
1:10	= 25.9	22.0	22.0	0.397	0.409
	30.1				
15	= 30.0	108.0	114.0	0.093	0.079
23	= 10.3	12.0	12.5	0.933	0.720
28	= -0.2	10.0	9.0	-	-
32	= -0.2	9.0	7.5	with source returned to 13 cm above reactor bottom - see 3:36 P values -	

Experiment 88 (Cont).

Conclusions:

- ① With source in taper at level of bottom of reactor, a (multiplication)⁻¹ curve which is initially flat & then falls rapidly is obtained.
- ② With source at about the midpoint of the final critical cylinder the (multiplication)⁻¹ curve is ~~linear~~ practically linear and extrapolates to the previously determined value.

Draw back - See pg 64.

Experiment 89

73
1/21/48

Fox

9" Reactor - Tamped plus Cd shielding, $k_{eff} \approx 175$

Mikendorf
Callahan

Source: $1/2$ curie in 2 cc holder placed in reactor 4 cm from bottom. Stainless Steel counter weight ($3" \times 2"$ dia) at end of stainless steel cable - source suspended from wire by string.

(12 cm on scale = source at bottom)

Trip points - #3 - 91 x 100
#4 - 86

Scales #3 - 100
#4 - 10
#5 - 2
RE - 100

Time	Filling dead volume from #9 H = 0.8 cm	Volume from #9		M ⁻¹		
		I	II	I	II	
1:25 P						
1:30		11.5	10.0			#9 - Empty
		9.5	11.0			
		10.0	10.5			
		10.3	10.5			
1:48	= 5.1			(Blow out right glass + set tamps zero)		Filling from #8
	= 10.0	14.0	13.0	0.736	0.808	
1:58	16.9 = 16.8	20.5	22.0	0.502	0.478	#8 Empty -
2:06	= 22.0	29.0	30.5	0.355	0.344	Filling from #5
2:14	= 27.9	48.0	52.0	0.215	0.204	
2:30	= 32.6	105.5	116.5	0.098	0.090	#5 Empty - Filling from #3
2:35	= 34.5	203.0	227.0	0.051	0.046	
2:43	= 35.2	336.0	368.0	0.031	0.029	
3:10		Critical at 36.1 ± 0.1 cm.				

Drainback - See pg 64.

Conclusions:

- 9" reactor with Cd shielding and H₂O tamping, critical at 36.1 ± 0.1 cm $k_{eff} \approx 175$.
- Source in position + conditions described gave very satisfactory results. Multiplication curve is quite linear and extrapolates to critical condition to within 1 mm.
- This observation was made: System near, ^(slightly below) critical with top tamps about 5 mm above surface. lowering tamps ^{first} raises the reactivity, tamps effect, lowering it still further, to contact, makes system subcritical again, probably Cd shielding effect. etc.

1/17/48 de 36.1 + 1.2 = 37.3 cm - H₂O bottom corrected.

1/21/48 de $k_{eff} = 174.4$

9" Stainless Tamped and Cd shielded

$k_{eff} = 1.19$
wt % Cd = 12.4 = 0.148 gm/cc

$V_c = 15.30 L$

$M_c = 2.26 kg.$

74

1/21/48

Experiment 90

Joy

9" Reactor, Untamped, $H/x = 175$ McKendrew
Callahan

Same - Same as in # 89 -

Trip point " "

Seals # 3-100; #4-10; #5-2, RE-100 ms.

		I	II			
3:42 P	H=0.6cm	71.0	71.0			
		71.5	69.5			
3:48				I	M ⁻¹ II	Filling from #8.
4:01	H=17.2	138.0	144.0	0.516	0.484	#8 Empty, Filling from #3.
:11	=27.1	206.0	222.5	0.346	0.316	#3 Empty, Filling from #4
:19	=32.4	246.0	261.0	0.290	0.269	
:26	=37.1	273.5	297.0	0.260	0.237	#4 Empty, Filling from #2
37	245.0	325.5	352.0	0.219	0.200	

Conclusion:

9" Reactor Untamped, $H/x = 175$ - probably not ke
 critical at ∞ extension - $M^+ = 5$ at 45 cm -

DRAIN BACK:

- #1 ~ 17 cm in 9" reactor.
- #2 16.1 " " 9" "
- #3 10 " " 9" "
- 4 10 " " 9" "
- 5 ~ 17.7 " " 9" "
- 6 Full - $H/x = 127$
- 7 " - $H/x = 86.3$
- 8 18 cm in 9" reactor.
- 9 Dead volume.

$$H = 45.0 + 1.2 = 46.2 \text{ cm}$$

$$H/x = 174 \text{ (see following page)}$$

$$V = 18.96 \text{ L}$$

$$M = 2.81 \text{ kg}$$

$$\text{Estimated } H_c = V_c = M_c = \infty$$

1/22/48

Experiment # 91

9" Reactor Tamped $H/x = 175$

Cronin
Fox
Mortitt
Murray

Trip points #3 - 92 #4 - 91

#3 100 Scale #4 - 10 Scale #5 - 25 scale
Source 10 cm from bottom. In reactor. Wax covering only.
Source + counter check #1 6 1/2 #2 7.

Background 7.0, 7.0; 7.0, 7.0

Time	H	C ₁	C ₂	C ₀ /C ₁	C ₀ /C ₂	
9:40	5.0	7.0	8.0	1.0	.875	Filling from 5.
9:44	10.2	13.0	13.0	.538	.538	#5
9:52	15.8	39.5	42.5	.177	.165	#5 Virtually Empty.
10:04	17.6	63.5	70.0	.110	.100	Filling from #1
10:17	19.0	121	131	.058	.053	
10:22	20.0	243	270.5	.029	.026	Source Moved - Replaced. Flat Maximum.
10:31	20.5	414	458	.0169	.0153	
10:42	20.8	Not Critical				Feeding from 3 for better control.
10:53	21.0	Critical with Rod @ 19 cm.				
		Est. Criticality H = 21.0 cm.				
		Source back				

Conclusion: The 9" cylinder Tamped is critical @ 21.0 cm @ $N_0/A_0 = 175$.

After Drainback:

#	Height in 9" reactor
#1	15.8
#2	16.1
3	10
4	10
5	15.8
6	Full $H/x = 127$
7	$H/x = 86.3$
8	18.0
9	Dead Volume

Height in 12" reactor

8.9 cm
9.0
5.6
5.6
8.9
10.1
Dead Volume.

11/17/48 de
11/20/48

21.0 + 1.2 = 22.2 cm the bottom covered

$H/x = 174$

9" Stainless, Tamped.

$k_{eff} = 1.19$

with $\rho_{0x} = 12.4 = 0.148 \text{ gm x/cc}$

$V_c = 9.11 \text{ L}$

$M_c = 1.35 \text{ kg}$

76

1/22/48

Experiment #92

Cronin
Fox
Morlett
MurrayBackground (K) 12" Reactor, Cd Shielding Tamped
N₂/N₂ = 175

S @ 6.0 cm from bottom

#	Time	H	C ₁	C ₂	C ₁ /C ₂	C ₂ /C ₁		
	12:42	0.2	5.0, 5.5	3.5, 5.5	—	—	Use 5.5 @ background	
	12:51	5.1	4.5	4.75	—	—	Filling from #2 empty @ 8.7	
	1:00	10.1	15.0	14.5	.367	.378	Filling from #8	
	1:10	13.0	25.5	25.5	.216	.216		
	1:16	16.3	72.0	76.0	.076	.072	Stopped Filling from #8	
	1:25	17.4	153.0	159.0	.036	.035	Filling from 5.	
	1:38	18.0	300.5	326.	.018	.017		
	1:52	18.3	670	731	.008	.008		
	1:59	18.5	Not critical S = 28 cm. (14 cm off bottom)					
	2:08	18.75	Just barely subcritical. Period of dropping less than one division per 2 minutes					

Conclusion: Criticality of 12" Reactor, Tamped & Cd Shielded occurs at a height of 18.8 cm with N₂/N₂ = 175.

Drainback: per exp #92.

11/27/48 DC 18.8 + 0.7 = 19.5 cm = He bottom corrected.
 11/26/48 DC H₁₈ = 174.8
 12" Stainless, Tamped & Cd shielded
 ρ_{sp} = 1.19
 wt% X = 12.4 = 0.148 gwt/cc
 V_c = 14.22 L
 M_c = 2.10 Kg.

1/22/48

Experiment #93

Crowin
Fox
Murphy
Murry

12" Reactor Untamped

$N_H/N_X \approx 175$

Background Counts #1 - 74
75

*2,76
75
ave. 75

source at 6 cm from bottom.

Time	H	C ₁	C ₂	C ₁ /C ₀	C ₂ /C ₀
2:43	0	75	75	1.00	1.00
2:46	10.0	70 $\frac{1}{2}$	72 $\frac{1}{2}$	1.06	1.04
2:45	14.9	182	190 $\frac{1}{2}$	2.42 1.06	2.54 1.04
3:02	16.3 17.1	296	311	2.53	2.1
3:08	19.0	435 $\frac{1}{2}$	468 $\frac{1}{2}$.172	.160
3:15	21.0	787	857	.095	.0875
3:28	22.3	1421	1454	.053	.052
3:35	23.2	1502	1598	.050	.048
3:50	23.7	counters haywire, maybe because level too high.			
4:00	27.0	not critical.			
		critical.			

notes
Filling from # 2
Filling from #8 #2 Empty at 8.5
Stopped filling from #8
Filling from #5.

2:23 Stopped filling from #5
Filling from #4

Conclusion: Criticality of 12" reactor, ^{un}tamped = 29 cm. $N_H/N_X \approx 175$

Drain back. as per exp 92.

pm

11/17/48
11/20/48

24 + 0.7 = 24.7 cm = H_c bottom connected.
H_X = 174.2
12" Stainless, Tamped. Untamped.
K_{eff} = 1.19
M_X = 17.4 = 0.148 gm/cc
V_c = 18.02 L
M_c = 2.67 kg

$MIX = 175$

Beck
Macklin
Fax
Kewer

12" reactor in position. Instruments checks.

3 & #4 slip at 92 on 100 scale.

1 & 2 counters OK.

5 OK

Reel & Process monitor OK.

Sample 3cm from bottom.

Time	Level	Counting Rate		Cp/C.	
		#1	#2	#1	#2
12:20.	Background	27.5	28.0		
	zero 0.5 cm.	10.0	14.0		
	5.4	16.0	17.0	.62	.82
	8.7	26.0	32.0	.382	.44
	11.0	43.0	52.	.23	.27
	13.0	130.	164.	.077	.085
	13.4	189.5	246.	.053	.057
	13.7	259.0	332.	.034	.042
1:31	14.0	806.	985.	.012	.014
	14.1	did not go - but close.			
	14.2	well above critical			

Conclusion: Critical at 14.15.

^{117m}Sb DC $\frac{14.2 \times 0.7}{14.15 + 0.65} = 14.9$ cm
-He bottom cancelled.

^{120}I HW = 174.0
12" Stainless Tamped.

app = 1.19

WHL $\rho_{w/c} = 17.4 \approx 0.148$ gm/cc

$V_c = 10.87$ R

$MIC = 1.61$ kg.

Drainback	For 12" Reactor	For 10" Reactor
1 8.9	8.9	12.8
2 9.0	9.	12.9
3 5.6	5.4	7.8
4 5.6	5.6	8.0
5 8.9	8.9	12.8
8 10.1	10.1	19.5
9 Dead vol.	Dead Vol.	

Experiment 95 10" Reactor.

$H/X = 175$

Tamped

10" reactor installed and checked.
 Trip point #4-85, #3, 92.

Wacke
 Vism
 Top
 Back

Time	Level	Sediment		c/c	
		#1	#2	#1	#2
4:00	Background				
4:09	zero 0.5	8.0	10.0		
4:20	15.2	84.0		.095	.098
	15.7	112.5	143.5	.071	.070
4:40	16.3	166.5	206.5	.048	.047
	16.8	429.0	519.	.019	.019
	17.0	not critical. But close			
	17.15	slightly below critical			
	17.2	critical			

Conclusion - Critical at $17.2 \pm .05$.

Valve on #4 Storage cylinder found leaking - 100cc of Soln. Found
 in pit.

Drainback

# 1	14.8
2	14.9
3	9.
4	none - leak
5	14.8
8	14.5
9	Dead Vol.

11/17/44 DE 17.2 + 0.9 = 18.1 cm - Hc bottom covered.
 11/20/48 DC H/X = 174.8
 10" Stainless, tamped.
 $\theta_{pr} = 1.19$
 $w_{pr} = 12.4 \approx 0.148 \text{ gm/cc}$
 $V_c = 9.17 \text{ L}$
 $M_c = 1.36 \text{ Kg}$

1/27/48 - Fox & Cronin repairing leakage valve on #4 storage cylinder. Replaced #3 and #4 3" storage cylinders with 4" cylinders.

1/28/48. Experiment 96. 10" untempered Hx = 175.

Beek
McFendon
Fox
Cronin.

9:00 AM Check pit - Instruments OK.
Trip Points #4 at 84, #3 at 88.
Source at 13 cm (7 cm scale reading)

		#1	#2	#1	#2
	Solution Level	Counting Rate		C ₀ /C _c	
	Background	72	94		
9:20		73	101		
9:28	zero 0.0.	73	113		
9:47	25.0.	353.	436	.203	.23.
9:54	30.	710.	833.	.102	.12
10:01	32.9	1206	1375.	.06	.72
10:07	34.0	1488	1345	.049	
	34.5	not critical - repeated additions of 2 mm each and test for critical			
10:29.	37.8	Final reading at critical			

Conclusion: (1) Critical at 37.8.

(2) Detectors on vented equipment should be moved back to reduce levels.

11/17/48 de 37.8 + 0.9 = 38.7 cm - He bottom connected

11/26/48 de Hx = 174.8

10" stainless untempered.

appx = 1.19

weight of Hx = 12.4 = 0.146 gm/cc.

V_c = 19.61 L

M_c = 2.90 kg

Measurement of Sol'n Hts. -

	#1	#2	#3	#4	#5	#6	#7	#8	#9
	70.5	71.5	70.2	33.6	71.0	NK 127	H/ X	70.9	71.5
	37.2	36.4	37.7	32.7	37.0		86.3	37.4	36.7
Δh	33.3	35.1	32.5	0.9	34.0	—	—	33.5	34.8
	83.1	87.5	81.1	2.25	84.9			83.6	86.9
	26.1	27.5	25.5	.706	26.6			4.075	in 7" Reactor
Volume	6.665	7.018	6.504	.180	6.809			6.705	6.967 Total Volume 37.775 Liters

Suggest: #8 be filled and used for storage and put 3.5 liters in #5 for storage and adjust #1, 2, 3, 4 so that approx 5.2 liters in each cylinder or 20 cm in a 7" Reactor. In #9 should have approx 2.5 liters.

This would give on dilution a total volume of 30 liters and require 12 liters of DD water for dilution to an $\frac{1}{4}$ of 250

Exp. 97 7" tamped, $N_H/N_X \approx 175$ 1-29-48

Cronin

Fox

Marfitt

Murray

Tripps #3 86

#4 92

#2 Counter making erroneous counts - input voltage changed from dial setting of 8.5 to 10.

9:10 Filling dead volumes

	Cylinders	Soln Ht.	C_1	C_2	C_0/C_1	C_0/C_2
9:17	#9	0.2 cm.	6.5	6.25		
	#9	2.0 cm	6.25	6.0		used as C_0
9:30	#5	15.0 cm	13.5	12.5	.463	.480
9:38		25.0 cm	25.5	24.5	.245	.245
		28.5	—	—		#5 empty
9:48	#3	32.3	37.5	37	.167	.162
10:00		40.0	54.5	54.5	.110	.115
10:06		50.0	143.5	146.0	.044	.041
10:15	#3	53.3	—	—		#3 empty
10:17	#2	55.0	not critical but very high power level.			
10:45	#2	54.85	1113	1138	.0055	.005
10:51		55.15	not critical with source out.			
11:10		56.45	Critical with rod 2.5 cm for soln			

Conclusions: 7" tamped reactor at $N_H/N_X \approx 175$
critical at ≈ 55.4 cm. (Probably will not go at $N_H/N_X \approx 250$)

11/17/48 DC 55.4 + 1.9 = 57.3 cm - He bottom counted

11/20/48 DC

$N_H = 174.8$

7" Stainless, tamped.

$K_{eff} = 1.19$

wt % = 12.4, $\rho = 0.148$ gm/cc

$V_C = 14.22$ L

$M_C = 2.10$ kg.

Dilution to H/X = 250*

	#1	#2	#3	#4	#5	Storage			#9
Drain back	20.0cm	20.0cm	20.0cm	20.0cm	H/X 175	N/H X	H/X 36.3	H/X 174.0	10cm
Volume	5.14	5.14	5.14	5.14					2.57
Water to Add =	2.198	2.198	2.198	2.198		127			1.099

Total Volume = 33.029 Liters after dilution

$$92 \times \frac{3.7}{99}$$

Notes from page 55, Note book 22. Re measuring H/X - Entry dated 7/4/48 -

Specific gravity 1.15

Average H/X = 226

Wt % X = ~~0.0~~ 9.95 = 0.114 gm/cc of solution.

Exp. 98 7" Reactor Tamped - $H/X \approx 250$ ^{225.76} ~~250~~ 1/29/48

Beck
Kastler
Crown

Solution diluted to $H/X \approx 150$.

1:20 P. Instruments checked.
Trip points: #3, 80; #4, 83.

Time	Solution Level.	Counting Rate		C./c.	
		#1	#2	#1	#2
1:45		4.5	5.0		
2:00	zero . 0.5	5	4.5		
2:10	30.0	19	18.5	.26	.27
2:25	48.	38.5	39	.13	.13
2:40	60.	53.5	52.5	.085	.085
2:45	68.	62.5	61.5	.18	

Conclusion: Does not go critical ^{at 68cm height.} and probably would not at indefinite height. $N_0/\lambda \approx 225.76$, 7" reactor tamped

Drain back 7"
#1 - 28 cm
#2 - 28 cm
#3 - 28
#4 - 28
#9 - Dead volume, plus some extra.

8"
21 cm

11/20/48 DC
 $H = 68.0 + 1.9 = 69.9 \text{ cm}$
 $H/X = 226$; $\rho_{sp} = 1.15$
 $W_{ht} 0.705 = 9.95 \approx 0.114 \text{ gm/cc}$
 $V = 17.35 \text{ L}$
 $M = 1.98 \text{ kg}$

Estimated - $H_c > 100 \text{ cm}$
 $V_c > 24.8 \text{ L}$
 $M_c > 2.8 \text{ kg}$

Note: Specific Gravity of a well mixed sample from # 1, 2, 3, & 9, = 1.149.

Experiment 99

8" Reactor Untamped

H/x = 250 ^{225.76}

2/2/48 85

Martin
Fox
Visnes
Callahan

(Probably not be critical but will give opportunity to mix solution).

Source: 12 cm from bottom; 578" brass sphere, paraffin enclosed

Trip points:	3	4	5	RE
	83x100	83x100		
Scales	100	10	2	25

10:20 A

Filling from #9

	I	II
H = 0.3 cm	73.5	78.0
	<u>73.0</u>	<u>77.0</u>
	73.3	77.5

OK Sight glass zone + for leaks.

H = 1 cm

			M ⁻¹	
			I	II
10:40	= 22.3 cm	85.0	86.0	0.863 0.902
52	= 34.8	115.0	127.0	0.638 0.635
11:05	= 44.2	120.0	127.0	0.610 0.610
15	= 65.4	121.0	133.5	0.606 0.580
30	= 84.3	122.0	135.0	0.601 0.574

#9 Empty; Filling from #4

#4 Empty; Filling from #3

#3 Empty; Filling from #2

#2 Empty; Filling from #1

Mixed solution -

Drain 10 cm into #2; Empty #1 - (ca 2.5 cm) Mixed solution.

Conclusion - 8" reactor, untamped, H/x = ^{225.76}/~~250~~ will not be critical at ∞ extension -

DRAINTSACK: #1 - 22 cm in 8" reactor

#2 - 22 "

#3 - 22 "

#4 - 22 "

#9 - Dead Volume

11/30/48

$H = 84.3 + 1.5 = 85.8 \text{ cm}$

$H/x = 226$ (see preceding page).

$V = 27.82 \text{ L}$

$M = 3.17 \text{ kg}$

Estimated $H_c = K_c = M_c = \infty$

7/1/48

Experiment # 100

Vigney

8" Reactor, Tamped, $H/x = 225.76$
 $H/x = 250$

Macklin

Trip pt - 40 in #99; Source - 10 in #99

Fox

Scales 3-100, 4-10 5-2 RE-25mv

Callahan

		I	II		
1:15P	H = -0.7cm	4.5	5.5		
		5.0	5.0		
		4.8	5.3		
1:25P	= 4.9cm	4.0	5.0	I	M ⁻ II
1:35P	= 15.0	10.0	13.0	0.440	0.408
40	= 20.1	18.0	23.0	0.267	0.230
50	= 23.2	27.0	32.0	0.178	0.166
55	= 27.5	46.0	55.5	0.104	0.096
2:07P	= 31.0	93.0	112.0	0.052	0.047
15	= 33.0	207.5	243.0	0.023	0.022
20	= 34.0	510.0	601.0	0.009	0.009
30	= 34.3				Sub critical
32	= 34.6				Sub critical.
35	= 34.9				Critical with control rod 3cm below surface of solution -

Filling from #4.

(1.9cm left in #4).

Filling from #3

DRAIN-BACK - SAME AS EXP #99

Conclusion: 8" Reactor, tamped, $H/x = 225.76$ Critical at 34.8 ± 0.1 cm -11/17/48 DC $34.8 + 1.5 = 36.3$ cm = Hc at bottom corrected.11/20/48 DC $H/x = 225.8$ 226

8" Stainless, tamped.

opw = 1.15

wt % x = 9.95 = 0.114 gm x/cc.

 $V_c = 11.77$ L. $M_c = 1.34$ kg.

EXPERIMENT # 101

87
2/3/48

904
Cronin
Callahan

9" Reactor, H₂O tamped, Cd shielded, $M/k = 225.76$
Source: ¹³⁷Cs curie, paraffin enclosed, (2cc) 12 cm from reactor bottom -

	3	4	5	RE
TRIP POINTS	83	82	-	-
Scales (start)	100	10	2	25

Time	Cyl.	Sol'n Ht.	Counters		C ₀ /C ₁	C ₀ /C ₂	Remarks
			I	II			
10:30	9	6mm	5.5	6.0			#9 empty
			6.0	6.5			
			6.0	6.0			
			5.5	6.5			
		avg.	5.8	6.3			
10:50	4	5.2	4.5	5.0			
11:00	4	17.9	10.5	12.5	.552	.504	#4 Empty
11:15	3	25.1	20.0	23.5	.290	.268	
	3	32.5	35.5	42.0	.164	.150	#3 Empty
11:35	3	35.2	47.5	57.	.122	.110	
11:45	2	40.0	91.5	114.5	.064	.055	

Drain Back

- #2 - 4.8cm ?
- #3 - ~~18.2~~ 18.2
- #4 - 17.0 = 17.0
- #9 Dead Vol. plus.

Conclusion:

9" reactor, H₂O tamped and Cd shielded, $M/k = 225.76$ was not critical at maximum possible height - 40.0 cm - where $M = 16$. Extrapolation of the multiplication curve indicates criticality at $H = 45$ cm.

$H = 40.0 + 1.2 = 41.2$ cm -
 $M/k = 226$ (see preceding page).
 $V = 16.96$ l.
 $M = 1.93$ kg

Estimated: $H_c = 45 + 1.2 = 46.2$ cm
 $V_c = 18.96$
 $M_c = 2.16$ kg.

EXPERIMENT # 102

2/3/48

9" REACTOR, TAMPED, $H/X = \frac{225.76}{250}$

Cromin
Zn
Calibration

Trip points and source same as in #101.
Scales - 3 - 100 5 - 2
4 - 10 RE - 2.5

Time	Sol'n Ht.	Cyl	# I	# II	C_0/C_1	C_0/C_2
1:15	0		5.5	5.5		
			5.0	5.5		
			6.0	5.5		
			5.0	6.0		
			9.5			
		aveg	= 5.2	5.5		
1:35	11.9	3	10.5	11.5	.495	.478
	18.5	3	32.5	40	.160	.137 # 3
1:50	20.1	4	50.0	60	.104	.092
1:55	21.9	4	105.0	123 124.5	.452	.0448
2:05	23.2	4	251.0	297.5	.021	.0186
2:16	23.7		423.0	499.5	.0123	.0111
2:25	24.0		not critical			
2:31	24.2		slightly supercritical with Rod all out.			

Conclusion

Critical at 24.1 ± 0.17 cm
9" Reactor. Tamped, $H/X = \frac{225.76}{250}$

Draw back:

1 - 17.5 cm	$H/X = 250$	in 9" reactor	= 9.8 cm in 12" reactor
2 - 17.5 "	"	" " "	= 9.8
3 - 18.5 "	"	" " "	(overly free) = 10.4
4 - 17.0 "	"	" " "	= 9.5
5 - ?	$H/X = 175$		
6 - ?	≈ 125		
7 - ?	≈ 86		
8 - ?	≈ 175		
9 - Dead volume	$H/X = 250$		

11/17/48 DC
11/24/48 DC

24.1 + 1.2 = 25.3 cm = Hc bottom covered
 $H/X = \frac{225.76}{226}$
9" Stainless, tamped.
 $sp. g. = 1.15$

with $\rho_0 X = 9.95 \approx 0.114 \text{ gmX/cc}$.
 $V_c = 10.38 \text{ L}$
 $M_c = 1.18 \text{ kg}$

304
Cromin
McLendon
Celliker

12" Reactor, $H/X = 250$, Cd shielded H-2 Tamped
Source - ^{252}Cf , $z_{\text{eff}} = 12$ cm from bottom - (paraffin enclosed only).

Trip points: #3 - 92 x 100
#14 - 86 + 100

Scales 3 - 100
4 - 10
5 - 2
RE - 25 mV

		I	II	M ⁻¹		
	H=0.7	4.0	5.0	I	II	
2:21		<u>4.0</u>	<u>4.5</u>			
		3.5	4.0			
2:36	4.9	3.5	4.0	.615		Adding from #4
2:43	9.5	6.5	7.0	.615	.643	#4 - M.T.
2:58	15.1	17.5	22.0	.228	.205	Adding from #3
3:04	16.6	31.0	39.0	.129	.115	
3:10	17.7	50.5	62.0	.080	.073	
3:18	18.9	104.5	129.5	.038	.035	To 18.9 from #3
3:26	19.6	222	266.0	.017	.018	Adding from #2
3:46	20.0	613	745	.0060	.0065	
4:00	20.2	Critical —		Top Tamper on; Source out!		

Conclusion: Critical at 20.2 cm. — 12" Reactor, $H/X = 226$ - H-2 tamped & Cd shielded.

Brain back: Same as # 102.

11/7/48 $z_{\text{eff}} = 20.2 + 0.7 = 20.9$ cm Hc bottom corrected.

11/20/48 $H/X = 226$

12" Stainless, Tamped, Cd shield

$\rho_{\text{Pu}} = 1.15$

wtd % $X = 9.95\% = 0.114$ gm/cc.

$V_c = 15.10 \pm 15.25$ L

$M_c = 1.72$ kg. 1.74 kg

7/4/48

Exp. 104

Cronin
Fox
Callahan

12" Reactor UnTamped $H/x = 225.76$

Trip points (same as Ex 103)
Scales - #3 #4 #5 RE
100 10 2 25

		Cylinder	I	II		
4:50 P	H = 0.6cm		63	71.5		
			63.5	69.5		
			62.0	71.0		
			62.8	70.6	I	II
5:05 P	H = 10.5cm	empty	38.0	42.2		
12	= 15.0	2	83.5	97.5	0.752	0.724
1:22	= 20.1	2 empty	314.5	370.0	0.200	0.191
1:32	= 21.6	3	500.5	591.0	0.126	0.119
1:40	= 23.2	3	955.5	1119.5	0.066	0.063
1:50	= 24.4	3	Not critical -			
1:53	= 25.0	3	"	"		
1:55	= 25.4	3	"	"		
6:00	= 25.7	3	Critical with 10cm (d) control rod in solution.			
6:05	= 25.6	3	"	"	8"	" " " "
10	= 25.55	3	"	"	5"	" " " "
12	= 25.5		"	"	Cd control rod out.	

DRAIN BACK :

- 1 - 10.0 cm in 12" reactor $H/x = 225$
- 2 - 10.1 " " " "
- 3 - ~ 10.4 " " " "
- 4 - 9.5 " " " "
- 5 - ? $H/x = 175$
- 6 - ? $= 127$
- 7 - ? $= 86$
- 8 - ? $= 175$
- 9 - Dead volume -

Conclusion 12" Reactor - untamped - $H/x = 226$ - Critical at 25.5cm -

11/7/48 de 25.5 + 0.7 = 26.2 cm - He bottom tamped cancelled.
11/20/48 de $H/x = 225 + 226$
12" Stainless untamped.

net $H/x = 9.95 = 0.114$ gwt/cc
appx = 1.15
 $V_c = 19.11$ L
 $M_c = 2.18$ kg.

2/5/48

Exp. 105

Cronin
Fox
Murray

12" Tamped $H/\lambda = 225.76$

trip pts 95 each

Scales #5-2, #4-10, #3-100, Reed-25.

Source 6 cm from bottom.

Tamper ran off bottom, took off a few threads.

10^{AM} ready to go.

Time	H	Cylinder	#1	#2	(M) ₁	(M) ₂	Comments
10 ⁰⁰			4.0	4.5			
			4.0	5.0	Source moved		
			5 ³ / ₄ (6)	7.0 (6 ¹ / ₂)			
			6 ¹ / ₄	6 ¹ / ₄			
Collar on tamper screw at top slipped. By <u>error</u> , had left off bottom bearing. Replaced and readjusted.							
11 ³⁰	H = 5.3	4	8.0	9.0	.75	.72	
11 ³⁵	H = 7.1	4	10.0	12.0	.60	.54	Stopped falling from 4
11 ⁴⁵	H = 10.1	3	19.0	23.0	.32	.28	
11 ⁵⁰	H = 12.0	3	31.0	38.0	.19+	.17	
11 ⁵⁵	H = 14.0	3	84	99.5	.071	.065	Stopped falling from 3
12 ⁰⁰	H = 14.6	2	137	163.5	.044	.040	
12 ¹⁰	H = 15.3	2	367	441	.016	.015	
12 ³⁵	H = 15.8	2	critical.				

Conclusion: 12" tamped cylinder critical at 15.8 cm with $NH/\lambda = 225.76$.

Draw back. Same as in Exp 104.

12

11/7/48 15.8 + 0.7 = 16.5 cm - the bottom cemented

11/26/48 $N/\lambda = 226$

12" Stainless tamped.

Open = 1.15

wt % X = 9.95 = 0.114 gm X / (cc)

V_c = 12.04 L

M_c = 1.37 kg.

2/5/48

Exp 106

10" untamped, $N_H/N_X \approx 225.76$

Cronin
Fox
Murray

- Soln. heights:
- 1 14.4
 - 2 14.5
 - 3 15.0
 - 4 13.7
 - 5 } of the
 - 6 } concentrations
 - 7 }
 - 8 }
 - 9 D.V.

Time	Cylindr.	H.	#1	#2	RM, RM ₂	Comments
2:35	dead vol. #9	0	67 66	70.5 69.5		
	#4	12.8				empty
2:45	#3	15.0	54	55.5		
		18.9	93.75	105.5	.71 .66	
3:00	#3	27.4	248	279.5	.27 .25	empty
	#2	33.0	422	477	.16 .15	
	#2	40.0	1061	1241	.063 .056	
	drain back to sum above Moved counters back.					
3:50	dead vol.	0	20 19.5	17 17.5		
4:05	#4	13.3			.43	#4 empty
	#3	20.6	455	40	.43 .57	
4:15	#3	28	90	70.5	.22 .245	#3 empty
	#2	35.2	194	158	.10 .11	
4:30	#2	38.0	271	229	.073 .075	Stopped filling #2
	#1	40.0	379.5	325	.052 .053	
4:40	#1	42.1	623	549.5	.032 .031	
	#1	43.9	1217	1109	.016 .0155	
		46.1	critical with rod post way in. (8cm)			
		45.7	critical exactly			

Conclusion: 10" untamped critical at 45.7 cm. $N_H/N_X \approx 225.76$

N_H/N_X de $45.7 + 0.9 = 46.6$ cm bottom corrected, $N_H = 225.8$, $N_X = 10$ " stainless untamped; $q_{cr} = 1.15$; $\rho_{wt} \% X = 9.45$; $\rho = 0.114$ g/cc. $V_C = 23.61$ & $M_C = 2.69$ kg.

2/9/48

Exp 107

10" Reactor, Tamped. $H/X = 225.76$

Flushed air header line with water from ~~explos~~ union just within cylinder storage pit, ^{back} to tee + block valve where vacuum is normally applied; also drained same through vent valve. This was necessary since in the draining back on 2/5 a cylinder was overfilled + solution was collected in the vacuum pump trap (flock).

Vision
Joy
Maudlin
Caution

H/C source, peroffin enclosed, 12 cm feed reactor bottom.

		3	4	5	RC
	Trip points	88.100	83.100		
	Scales	100	10	2	50 mv.
10:30A	H = 0.0 cm	5.0	6.0		
		5.0	6.0		
	0.7 = 4.0			I	M ⁻¹ II
1:57	= 14.4	24.0	26.0	0.208	0.231
11:06	= 16.5	55.0	60.0	0.091	0.100
15	= 17.5	89.0	98.0	0.057	0.061
19	= 18.5	274.0	296.5	0.018 0.020	0.020
27	= 18.9	631.0	688.0	0.004	0.004
38	= 19.0	Sub critical.			
42	= 19.2	Critical with 10 cm CD rod below solution level.			
44	= 19.1	Critical with CD control rod bottom at solution level.			

#9 Empty; Filling from #4.
#4 " ; Filling " #3

11/17/48 DC 19.1 + 0.9 = 20.0 cm the bottom corrected

H/C = 475.8, 226
10" Stainless, Tamped.
Ap_g = 1.15
wt 70g = 9.95 = 0.114 gm x 100.
V_c = 10.13 L.
M_c = 1.15 Kg.

Conclusion 10" Reactor. H/C = 225, Critical at 19.1 cm.

10.2 cm into #1, 2, 3, 4
5.8 cm into #9

old (3") #6 removed to storage new (4") #6 filled full of H/C 225.76
extra few liters to re-evaporation apparatus for eventual storage

added D.D. water to #1, 2, 3, 4 & 9 { 0.436 by volume }
2270cc ↑ Calc. by FCrossin 2/6/48
1282cc

The above procedure was calculated to give a dilution to H/C = 325

EXPERIMENT 10B

2/10/48

10" REACTOR ^{Stainless} UNTAMPED

H/X = 325

Joy
Cromin
Callahan

TRIP POINTS #3 91K100 #4 83X100.
Seals #3-100, #4-⁵10, #5-2, R-E-25ms.
Cylinders 1, 2, 3 & 4 have solution = 14.5 cm in 10" reactor
" 9 has lead volume
Source - 12 cm from bottom, paraffin enclosed.
Counter set away from reactor 130 cm

	H = 0.0 cm	I	II		
10:25A		15.5	25.5(?)		
		15.0	20.0		
		16.0	20.5		
"		15.5	20.3		
35	H = 1.4	I	I	I	II
50	= 16.3	18.0	36.0(?)		
		17.5	26.0	0.886	0.776
		18.0	26.5		
11:05	= 25.1	43.0	88.0(?)		
		42.0	77.0		
		42.0	71.0		
		41.5	58.0		
		41.5	54.0	0.374	0.376
11:27	= 30.7	60.0	77.0?	0.258	0.264
		60.0	106.5?		
		60.0	136.0?		
11:40	= 37.4	86.0	124.0		
		87.0	169.0?	0.178	
:52	= 42.3	105.0	163.5		
		107.5	129.5	0.144	
12:02	= 45.8	124.5	255.0?		
		126.0	251.0	0.123	

#9 Empty, Filling from #4
#4 Empty - mixed sol - reduced H 3mm.
Filling from #3 (mixed)
#3 Empty - MIXED -
Filling from #2
Mixed - no chg in reading. Filling from #1

Conclusions: ① #2 counter erratic
② 10" Reactor Untamped H/X = 325 - not critical at maximum attainable height -
H = 45.8 cm M = 8; No safety at ∞ length is doubtful -

Inventory	#	H/X	cm in 10" reactor (etc)	
	1	325	~ 14.7 cm	18.3
	2	325	~ 14.7 cm	18.3
	3	325	14.7 cm	18.3
	4	325	14.5 cm	18.2
	5	175	?	
	6	226	(free)	
	7	86	?	
	8	175	?	
	9		3W+	

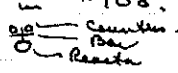
11/30/48 DC
H = 45.8 + 0.9 = 46.7 cm
H/X = 320 (see following page)
V = 23.66 L
M = 1.90 kg
Estimated:
Hc > 75 cm
Vc > 38 L
Mc > 3.0 kg

EXPERIMENT 109

For
Cromi
Catcher.

10" REACTOR, TAMPED, $H/x \approx 325$

2/10/48

Trap, ports, scales, same as in #108.
Counters: Top view \leftarrow 

	H = 0.7 cm	I	II	
		4.0	83.0	
		4.0	84.0	
		4.0	89.0	
		4.0	82.5	
		4.0	85.1?	
1:35 P		4.5	74.0	M^{-1}
45	= 5.2	5.5	65	0.889
50	= 9.7			0.728
2:00	= 15.5	12.5		0.320
2:07	= 18.1	20.5		0.195
2:12	= 20.5	40.5		0.099
2:18	= 24.8	64.0		0.063
2:25	= 22.8,	120.0		0.033
2:30	= 23.6	389.5		0.010
39	= 24.0	Slightly subcritical.		
44	= 24.2	Critical with 20cm Cd control rod below solution level.		

Filling from #4.

#3 EMPTY, FILLING FROM #1.

Conclusion - 10" Reactor, Tamped, $H/x \approx 325$ - Critical at 24.1 cm.

Inventory: Same as pg 94, Exp 108.

NOTE: EACH CYLINDER IN PIT IS UNCOMFORTABLY FULL SO BE CAREFUL TO PREVENT OVERFILLING ON DRAIN BACK, DO

11/17/48 DE
 $24.1 + 0.9 = 25.0 = H_c$ bottom corrected.
 $H/x = 319.9$ $W = 7.32$
 10" Stainless, Tamped.
 Sp Gr 110 $g_m \times / cc \text{ sol.} = 0.0805$
 $V_c 12.67 \text{ l.}$ $M_c 1.02 \text{ Kg}$

Stainless

Experiment 110 - 9" Reactor, Cadmium Tamped H/x-325 - 2/11/48

Beck
for
Cromin

8:30 - Drain, clean readjusting counter #2.

9:30 - Beginning check lists.

Trip points #3 tripped at 92, #4 at 83.

All instruments O.K. The two counters located 130 cm from assembly.

	Solution Level	Counting rate		C./C.	
		C ₁	C ₂	#1	#2
	Background	2	2		
10:30	10.00	2	2		
10:35	0.2. Zeros.	2	2		
10:50	30.0	6	6	.33	.33
10:56	35.1	7	7.5	.288	.269
11:00	39.3	8.5	8	.235	.25

No more reactor height available.

Conclusion: does not go critical; - multiplication about 3.5 - and leveling off.

Drawback

9" reactor

#1 - 18.3 cm

#2 - 16.

#3 - 16

#4 - 15.5

#9 7.5 cm + dead volume.

11/30/48

$$H = 39.3 + 1.2 = 40.5 \text{ cm}$$

$$Mx = 370 \text{ (see following page.)}$$

$$V = 16.62 \text{ L}$$

$$M = 1.34 \text{ kg}$$

Estimated:

$$H_c = V_c = M_c = \infty$$

11:45 Instrument check - all OK.

Solution Level	Counting		C/P	
	#1	#2	#1	#2
0.2 g ₁₀	4	4		
"	4	4		
20.	15.5	16.5	.258	.242
	25.8			
23.9	28.5	30.	.135	.133
26.1	43.5	45	.092	.089
28.27.9	69.5	71.	.575	.56
29.5	120.	121.5	.033	.033
30.4	180	191	.022	.021
31.6	not critical; but close.			
31.95	above critical.			
31.8.	Critical.			

Conclusion: Critical at 31.8.

Drainback	9" reactor	8" reactor
#1	18.3	23
#2	16. +?	20.2 +?
#3	16.3	20.3
#4	16.	20.2
#9	7 + dead volume 8.8 + dead vol.	

11/7/48 DC 31.8 + 1.2 = 33.0 cm = H_c bottom corrected.

H₂X - 319.9

W₈ % X = 7.32

9" Stainless tamped.

Sp Gr. 1.10 $\frac{g \times X}{g \times \rho_{\text{water}}} = 0.0805$

V_c = 13.54 L

M_c = 1.09 Kg

Exp 112 8" Tamped $\frac{1}{4} = 325$

2/11/48.

Back
Top
Crown

1:30 changed reactor.

2:35 Instruments checked. All OK.

	Solution Level	Rate		c. / c	
		#1	#2	#1	#2
2:38	0.5 340	3.5	30		
3:00	30.3	15.5	15.5	.233	.1935
3:11	41.1	29.1	31.5	.120	.095
3:32	47.4	47.5	47.5	.079	.063
3:45	54.3	116	121	.03	.025
	56.6				
	57.2	not crit.			
	57.9	" "			
	58.6	Critical			

Conclusion: Critical at 58.6.

Drawback:

#1 23
#2 22
#3 22
#4 22 ✓

Solu.

10.2
9.8
9.8
9.8

#9 Dead vol + 4 cm.

2/17/48 DC

58.6 + 1.5 = 60.1 cm = He bottom corrected.

HV = 319.9 Sp Gr. 1.10

8" Stainless tamped.

Wt % X = 7.32 gm X / cc = 0.0805

Vc = 19.48 l. Mc = 1.57 Kg

Experiment 113 - 12" untamped, $N_H/N_X \approx 325$ 2/12/48

Cronin
Fox
Murray
9: changed reactor

Time	Solution level - Cylinder		Counts		(Multiplication) ⁻¹		Comments
			#1	#2	#1	#2	
10 ³⁰	0.0	#9	18.5	17.5	1.0	1.0	
10 ⁴⁰	1.5	#9 dry					
10 ⁴⁵	11.4	#1 dry					
10 ⁵⁰	15.0	#2	30.5	22	.60	.80	
			30.0	22			
11 ⁰⁰	20.0	#2	61	51	.30	.34	
11 ¹⁵	22.0	#2 dry	81	66	.23	.265	
11 ²⁰	27.1	#3 stopped fill.	271	241	.068	.073	
11 ²⁵	28.1	#4	409.5	378.5	.045	.046	
11 ³⁰	29.2	#4	1024	971	.018	.018	Rod out
			335		.055		Rod in
	30.0	#4 above critical					
	29.9	#4 below critical					

Conclusion: A height of ^{reading} 4mm corresponds to zero level in the reactor, thus should subtract 0.9 cm from above. (PLEASE NOTE FOR OTHER 12" EXPERIMENTS)
 $H = 29.6$ for 12" untamped $N_H/N_X \approx 325$.

Drain back:

- 1 10.2
- 2 9.8
- 3 9.8
- 4 9.2

- 9 D.V. + 7.5cm.

11/17/48 $20 \times 79.6 + 0.7 = 30.3$ cm = He bottom covered
 $N_H = 319.9$ $S/G_2 = 1.10$
 12" stainless untamped.
 $wt\ \% X = 7.32$ $gm\ X/cc = 0.0805$
 $V_c = 22.10$ l. $M_c = 1.78$

Exp 114 12" tamped $N_H/N_x \approx 325$ 2/12/47

Cronin
Fox
Murray

Source at 7cm

Background $5\frac{1}{4}$ $5\frac{1}{2}$

Constructed broad flat Cd sheet for control rod →
Zero position = 7cm on control scale.



6" x 32"

Time	Level	Cylinder	Counts		Recip. mult.		Comments
			#1	#2	#1	#2	
2 ¹⁵	0	dead vol.	$5\frac{1}{4}$	$5\frac{1}{2}$	1.00	1.00	
2 ²⁵	8.1	4	$8\frac{1}{2}$	10	.62	.55	
2 ²⁵	10.1	4 new M.T.	$11\frac{1}{2}$	$13\frac{1}{2}$.46	.41	
2 ⁴⁵	12.6	3	18	$17\frac{1}{2}$.29	.31	
2 ²⁰	14.9	3	31	32	.17	.17	
2 ⁵⁶	16.2	3 stopped wiring	49.5	53	.11	10^+	
2 ⁰⁵	17.4	2	124	133	.042	.041	
3 ¹⁰	18.0	2	1216	1300	.0043	.0042	Multiplication of 230
3 ²⁰	18.2	superint. - Rod not out.					

Conclusion: ^{error in level} Citrat 18.2 - 0.4 = 17.8 cm
 $N_H/N_x \approx 325$, 12" tamped

drop back

# 1	10.2	≈	9.0
# 2	9.8	≈	9.0
# 3	9.8	≈	9.0
# 4	9.8	≈	9.0
# 9	d.v. + 1cm		

11/17/48 $V_{Cd} = 17.8 + 0.7 = 18.5$ cm He bottom corrected
 $M = 319.9$ Sp G = 1.10
 12" stainless tamped.
 $Wt\ of\ X = 7.32$ $g^m/cc = 0.0805$
 $V_c = 13.50$ l. $M_c = 1.09$ Kg.

2-16-48 Emptied sol. from #5 & #6 for evaporation.
 Put about 2 liters back into #6 at a sp. gr. of approx. 1.34

2/19/48

Preparation of Salin H/Xⁿ 86 for experiment

Cyl No:	6	7	8	
Ht. =	48.2	90	61.0	in Storage cylinder (4")
Vol =	3.91 liters	7.30	4.95	Sp. Gr. approx 1.310
Ht in 8" cyl	12.0 cm	25 cm	15.2 cm	
dead Vol. =	3.4 liters =	42 cm in 4" cyl =	10.5 cm in 8" cyl.	

7/23/48

Exp 115*

To examine effect on critical conditions of increasing

the thickness of stainless steel reactor wall.

Cronin
Fox
Visnov
Callahan

A sheet of 302 stainless $\frac{1}{16}$ " thick was rolled to ca $7\frac{3}{4}$ " radius with an overlap and fit snugly over the ~~35"~~ long (35") 8" reactor.

In order to measure this effect at two concentrations sufficient solution of $H/k = 85$ was prepared (see pg 101) In addition we also have $H/k = 320$.

Further, in order to mix with the $H/k = 85$ an untamped experiment was done.

$H/k = 85$, 8" Reactor, Untamped.

Trip points # 3 - 87x100 # 4 - 90x100

Seals # 3 - 100; # 4 - 5, # 5 = 2, P.E. = 25ms.

Source (^{137}Cs) - ~~on bottom at 45cm on scale~~ placed at 15cm from bottom (around paraffin coated glass) Top tamper in, but all way to top.

I	II
47.5	42.5
46.5	40.0
47.0	41.5

Control rod outside reactor

11:10 A

Filling from #6.

:15	H = 0.5cm	46.0	43.5
		45.0	42.0
		45.5	42.3

M⁻¹

11:30 A

= 3.0

I

II

#6 Empty, Filling from #8

40

= 16.2

50.0	44.0
49.0	44.0

0.910

0.97

(B) Rod in space outside reactor (normal tamped exp. position)

(C) Rod with drum - #8, empty, filling from #7

57

= 24.1

43.0	84.0
------	------

0.485

0.509

12:12 P

= 34.6

133.0	118.0
-------	-------

0.342

0.363

:18

= 36.8

139.0	123.0
-------	-------

0.327

0.343

#7 Empty, out of solution

Conclusion:

Insufficient solution made it impossible to go beyond H = 36.8cm. at this height the reactivity is somewhat greater (M = 3 vs. M = 2.3) than in Exp 67 - where conditions were about the same except for additional $\frac{1}{16}$ " wall thickness of reactor. This difference may be due to ① Somewhat different H/k ; ② Tamping by additional $\frac{1}{16}$ " wall ③ change in source position giving differently shaped M⁻¹ curves.

Drain back - 18.8 cm in 8" reactor into #8

18 " " 8" " " #7.

* Experiments 115-120 inclusive are considered in to give suspect results because, upon changing from one concentration to the next, a buildup of solution would ~~also~~ change the H/k values.

Exp. 116 $M/K = 85$, 8" Reactor Tamped.

103
2/23/48

Doubles Reactor Wall Thickness

Visner

Trip points as before.

Same (1/4") $\frac{1}{8}$ cm above reactor bottom.

Scale - #3-100, #4-5, #5-2. Read-out of order.

Fox
Cronin
Callahan

	$H = -0.3$ cm	I	II			
		5.0	5.0			
		4.5	5.5			
2:00 P	$H = 4.9$	6.0	6.0	0.800	0.883	Feeling for #7
:10	=10.0	9.5	9.0	0.505	0.589	
:16	=15.0	21.5	19.0	0.223	0.279	3cm left in #7 - Now beginning to fill for #8
:25	=17.9	38.5	36.0	0.125	0.147	
:31	=20.3	71.5	67.0	0.067	0.079	
:38	=21.5 =26.5	110.0	103.5	0.044	0.051	
:46	=22.5	209.0	189.0	0.023	0.028	
:55	=23.0					Not critical
:59	=23.4					" "
3:05	=23.5					" "
07	=23.7					Critical with 6.7 cm Cd control rod below solution surface.

Conclusion: ① 8" Reactor, tamped, $M/K = 85$ with additional $\frac{1}{16}$ " stainless steel around reactor (i.e. reactor wall thickness doubled) critical at 23.6 ± 0.1 cm —

② If this M/K is the same as that used in Exp 66 ($= 86.3$) the height now at criticality is 1.3 cm ($23.6 - 22.3$) greater than previously, without the extra reactor wall.

Inventory:		M/K	
1	320	-	9 cm in 12" Reactor = 20 cm in 8" Reactor.
2	320		9 " " " " " "
3	320		9 " " " " " "
4	320		9 " " " " " "
5			Empty
6	86		Dead volume
7	$M/K = 86$	-	18 cm in 8" Reactor.
8	86		18.8 cm in 8" Reactor
9	320		Dead volume

2/23/48

Exp 117 8" Reactor, HV=320, Tamped

JF
Cronin
Vivner
Callahan

Reactor wall thickness increased by 1/16" Stainless Steel.

Trip points as before.

Scales #3-100 #4-10 #5-2 RE out of order.

Source - 1/2" C - brass + paraffin - 12cm from bottom of reactor.

Dead volume filled from #9.

	H=0.2cm	I	II	M ⁻¹		
3:40P		4.0	4.0			
		5.0	4.0			
4:10	=21.8cm	15.0	13.5	0.300	0.296	Filling from #4. #4 Empty; Filling from #3
20	=32.4	25.0	24.0	0.180	0.167	
26	=41.4	37.0	36.5	0.122	0.110	#3 Empty; Filling from #2.
35	=50.1	46.0	55.0	0.080	0.073	
43	=57.0	99.0	96.0	0.045	0.042	#2 not empty; Filling from #1
50	=62.6	394.0	402.0	0.011	0.010	
5:03	=64.6	Critical with 12 cm of Cd control rod below solution level				
:08	=64.3	" " " " " " " " " " " "				
:11	=63.8					
:11	=63.7	Slightly subcritical				
:14	=63.9	Very " " " " " " " " " " " "				
:16	=64.1	" " " " " " " " " " " "				
:19	=64.3	Critical with 9 cm of Cd control rod below solution level.				

Conclusion: ① 8" Reactor, Tamped, HV=320, 1/16" additional to reactor wall thickness - critical at 64.2 ± 0.1 cm
 ② Compared with Exp. 112, the extra 1/16" of stainless steel wall increased the critical height by (64.2 - 58.6) = 5.6 cm or ca 9.5%

Inventory	HV	cm in 8" reactor
1	320	~20
2	320	~20
3	320	=20.0
4	320	=21.4
5	empty	
6	86	Dead volume
7	86	19.0
8	86	18.8
9	320	Dead vol +

Experiment 118 8" Reactor - Normal wall

H/x = 85, Tamped

24, 105
2/24/48
Fox
Cronin

Purpose: to evaluate effect of increasing wall thickness
of reactor by #116 stainless steel by
comparing this experiment with #116.
*116 has been compared with #66 but
without analysis there is no assurance
that the H/x values are the same

Callahan

Continued on next page

2/24/48

EXPT 118

8" Reactor $H/X \approx 86$

Tamped

Callahan
Cronin
Fox

Reactor wall thickness = $1/16$ "

Trip points: #3 = 88 #9 = 85

scales: #3 - 100 #4 - 5 #5 - 2

Source at 12 cm from bottom
started pulling D.V. from #6

2:30 PM

HT.	I	II		
2:35	1.2cm	5.0	5.0	M ⁻¹ from #6
		4.5	6.0	
		5.0	5.0	I II

2:55	10.4cm	10.0	9.5	500	.526	
3:01	15.0	20.5	20.0	244	.250	
3:14	19.2	50.5	50.0	.099	.100	#7 empty
3:22	21.0	100.0	89.0	.056	.056	pulling #8
3:42	22.1	188.0	171.5	.026	.029	
3:54	22.8	352.5	327.0	.014	.015	
3:58	23.2	not crit.				
4:05	23.4	"				
4:10	23.6	critical with 8cm control Rod in 2al.				

Conclusion: ① Critical at $23.5 \pm .1$ cm.

② This agrees, within the experimental precision, with the value obtained with this solution when the reactor had a $1/16$ " sheet of stainless steel wrapped around it. The difference observed between exp 116 & 66 probably due to difference in H/X . This to be checked by sampling.

Drain back	#	cm for 8" Reactor
	# 8	18.8
	# 7	18.0
	# 6	D.V + 1 cm

Other as on previous page (104)

3/25/48

Experiment 119 8" Reactor #4 = 320 Tamped. (Repeat of 112).

Best
for
cym
studies
method

Repeating #112 because of diff in height between crit. in 8" reactor with and without extra steel around reactor, it was thought advisable to check the experiment performed earlier.

12:15 - checking instruments. all OK except Reed, which is out for repairs.
Trip Points #4, 94 #3, 88.

	Solution Level	Counting Rate		C/c		
		#1	#2	#1	#2	
12:40	Background	5	6			
		5	6			
12:45	Zero 0.0	A	4.5			lead val from #9.
12:50	31.0	31.0	29.0	.129	.155	from #4
1:30	44.9	114.	99.5	.035	.045	
1:40	50.0	above critical (crit with 6 cm rod left ").				
1:45	49.5	below critical.				
1:50	49.7	Barely below critical.				
2:00	49.8	Critical				

Conclusion: Critical at 49.8 — obviously the discrepancy between this and the previous value of 58.6 is due to inadvertent mixing of #8 = 86 stuff.

2/25/48

Experiment 120 8" reactor Tanged + 1/16" steel, $H/x = 320$.

Reck

Repeating exp 117 with stainless steel.

For
crossin

Effect of stainless steel on previous experiment.

McLendon

all instruments OK except need out for repair
and #5 drifts badly - needs new battery.

	Solution level	Counting Rate		C/p	
		#1	#2	#1	#2
2:13	Zero.	0.5	5.5	7.0	
2:30	35.4	31	26.0	.178	.25
2:35		31.5	27.0	"	"
2:45	45.1	50.0	46.0	.11	.14
2:55	54.2	122.0	109.0	0.045	0.064
3:00	58.3	374.0	333	0.015	0.021
3:12	59.9	Slightly sub critical			
3:15	60.0	"			
3:20	60.2	With pump down & critical rod all way out, removal of source to its maximum height causes n level to drop sharply and then become constant.			
3:5	60.3*	Critical with 15 cm control rod below solution level.			

Reck out
level in In.

(filling for #2.)

Conclusions:

8" Reactor, with approx 1/16" stainless steel wall - $H/x = 320$ -
critical at 60.3 cm -

Inventory

#	H/x	Length	Notes
1	~320	20 cm	8" Reactor
2	~320	220	
3	~320	20.5	"
4	~320	20.5	"
5		empty	
6	~86		Dead wt.
7		18.0 cm	8" Reactor
8		18.8	"
9	~320		D.V.

2/26/48 Two samples of the solution used in the above exp were taken during "drain back". These gave $H/x = 293$
 $= 300$
Sppt measured at time of drain back $H/x = 1,110$

From back. 20.5 cm (8") were put into #4 (60.7 - 40.2).
 18.2 cm (8") " " " #3 (40.2 - 18.2 = 22.0).
 However #3 contained 7.3 cm giving total of 20.5 cm

When $H = 22.0$ cm; free surface, ~~the~~ the tamping, at contact reduced liquid level in sight glass to 21.9 cm + tamping indicator was at 21.45 cm. Mixing by blowing back through sight glass did not change these values.

It was decided to re-admit the solution from #3 + 4 at this time to determine reproducibility. (However, tamping had been drained so it was refilled)

	H = 22.0 cm	I		II		
2:45 P	H = 22.0 cm					Started filling from #3.
:50	H = 43.2	44.0	42.5	0.091	0.125	#3 empty. Filling from #4
3:07	H = 49.1	65.5	61.0	0.061	0.087	
3:15	= 56.0	140.0	129.0	0.029	0.041	
23	= 58.5	275.5	254.0	0.015	0.021	
32	= 60.1	Not Critical.				
37	= 60.3	" "				
45	= 60.6	Slightly below critical.				
58	= 60.8	Critical with 20 cm (D) central rod below solution level.				

Drain back - 17.6 cm (8") into #4 making its content 20.5 cm
 into #3 20.5 "

- Conclusions:
- ① With $H/x = 281.8$ (to be determined), 8" Reactor, tamped double wall thickness - critical height = 60.7 cm.
 - ② It was possible to check this value to ± 0.1 cm by draining about $\frac{2}{3}$ of the solution and re-admitting it.
 - ③ These values to be compared with 60.3 obtained under supposedly same conditions in Exp 120. Difference may be due to slight variations in H/x .

Sample taken on drain back for sp. gr = 1.108
 + for $H/x = 300$ } ^{obtained} at F.05 by straight
 288 } ignition
 281.8 from Run 8 DLB based on one sample from wet. burette and FOS's value of the sp. gr. (Sample electrolytically purified).

Tabulated Data on Wall Effects. 8" Reactors, Tamped

Exp #	Reactor Wall	H/x	Hc (corr.)
121	1/8" SS	281.8	60.7 ^{62.2}
122	1/16" SS	302.5	52.3
123	1/16" SS	99.5	24.2
124	1/8" SS	91.2	25.5
125	1/16" Al	98.2	22.4
126	1/16" Al + 1/16" SS.	~98 (?)	23.8
127	1/16" Al + 1/16" SS	289.8	47.5
128	1/16" Al	289.8	40.1
129	1/16" Al	58.8	20.5
130	1/16" Al + 1/16" SS.	58.4	21.9
131	1/16" SS	58.4	20.8
134	1/16" Al + 1/16" SS.	192.	30.8
135	1/16" Al	192	28.1
136	1/16" SS.	192	29.4

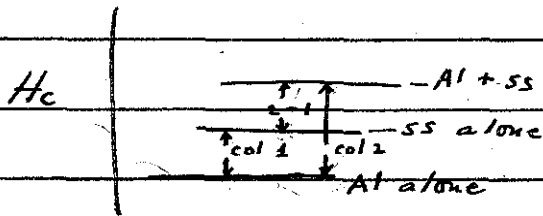
The above may be grouped as follows:

H/x Range	Al	SS	Al + SS.	SS + SS
58.6 ± 0.2	20.5	20.8	21.9	—
95.4 ± 4.2	22.4	24.2	23.8	25.5
192	28.1	29.4	30.8	—
292.1 ± 10.4	40.1	52.3	47.5	60.7 ^{62.2}

from which we see.

	Col. 1	Col. 2	Col. 2 - Col. 1	
H/x - Range	ΔH_c on substituting SS for Al	ΔH_c on adding SS to Al		
2.	58.6 ± 0.2	0.3	1.4	+ 1.1
6.	95.4 ± 4.2	1.8	1.4	- 0.4
	192.	1.3	2.7	+ 1.4
	292 ± 10.4	11.8	7.4	- 4.4

The simplest way of showing the data to be inconsistent is to obtain the value: Col 2 - Col 1 & note what this value represents.



So Col 2 - Col 1 is a

measure of effect of adding Al to stainless. Each value is expected to be positive & less than its corresponding value in column 1. This condition is not fulfilled anywhere.

There are other inconsistencies. The value C-1^(1.3), for instance, ~~which~~ should lie between 1.8 & 11.8.

For these reasons, the data were not reported in "Critical Mass Steels, Part III"

Experiment #122.

8" Reactor $H/X = 302.5$ (~300)

Cronin

Tamped - Normal reactor wall thickness, using same solution as used in #121.

Medlin
Thompson
Caelton

Starting with $H \approx 22$ cm - as at end of #121

Assume "zero" count $f = I = 4.0$ $II = 5.3$

	H	I	II	I	II	
				M^{-1}	M^{-1}	
A: 46P	H = 21.6 cm	15.5	16.0	0.258	0.331	Filling from #4.
52	= 30.0 "	27.5	26.5	0.145	0.200	
49	= 37.5	46.5	43.0	0.086	0.123	
	= 41.8					#4 empty, filling from #3.
5: 09	= 45.2	101.5	97.0	0.039	0.055	
115	= 48.5	214.0	201.0	0.019	0.026	
22	= 50.1					Not CRITICAL.
25	= 50.5					
37	= 50.9					Critical with 12 cm Cd control rod below surface of solution.
35	= 50.75					Not CRITICAL.

During drain back - when $H \approx 20$ cm - sample taken for $k_{eff} = 1.108$

$k_{eff} = \begin{matrix} 2.41 \\ 2.46 \\ 2.80 \end{matrix}$ } obtained at $F=0.5$ by direct ignition
as on pg 110.

Conclusion: 8" Reactor $H/X = 302.5$ (~300) Tamped, Normal wall thickness - Critical at 50.8 cm.

Inventory	H/X	cm in 8" Reactor.
1	? (~320)	~ 20 cm.
2	~ 300	20.5 + cm
3	~ 300	20.5
4	~ 300	20.5 cm.
5	empty	
6	? ~ 86	Dead end.
7	"	18.0
8	"	18.8
9	~ 300	Dead volume +

$\% U = 9.136$

11/7/48 DC
50.8 + 1.5 = 52.3 cm - He bottom corrected
 $H/X = 302.5$
8" Stainless, Tamped.

$H/X = 302.5$

112

3/1/48

EXPERIMENT 123 - 8" Reactor, Tamped, normal reactor wall thickness.

*
 $H/x = 98.2 (\approx 85)$

Maxlin

Visner
 Crown
 Caution.

Purpose: To examine effect of increasing wall thickness of reactor by adding a 1/16 stainless steel sheet, with a higher concentration of active material than used in #121 & #122. This repeats #116 & #118 but with better care & sampling for H/x ratios.

Trip points #3 - 85+100 #4 - 84+100
 Scales #3 - 100 #4 - 10 #5 - ~ RE - 50 ms.
 Source 1/2 C, brass - paraffin endrod - 12cm from bottom.

1:50 Filling dead volume from #6
 c/c.

		#1	#2
1:55	H: 0.1cm	4.5	6.0
		4.5	5.5
	→	4.5	5.7

Filling from #8. (Checked for cylinder valve leak; NG).
 First ht indication was ~ 10 cm; blew back manometer 4 times, each time the level ^{appeared} lowered, to a final value of 7.8 cm.

2:30 H = 7.8 7.5 8.0 0.60 0.71

Filling from #7.

2:45 H = 14.7 22.0 23.0 0.205 0.248

2:55 H = 17.5 33.0 40.5 0.105 0.141

H = 19.5 76.5 68.5 .083
 .059 0.083

3:20 H = 21.0 144.0 128.0 .031 0.045

3:25 H = 22.2 456.0 405.0 .000 0.014

3:38 H = 22.6 Not Critical.

3:42 H = 22.9 Critical. C.R. 8 cm below solution level.
 Call 22.7 cm critical

Drawback

#7 - 18 cm

Density measured: 1.311

$H/x = 92.4$ from H/D analysis, $F=0.5$ sp. gr. -

* Ave of analyses Exp 123-126 use.
 gives $Wt\% = 19.24$
 $H/x = 99.5$
 Sp gr = 1.32

Box 22
 #157

11/26/48 DC 22.7 + 1.5 = 24.2 cm, corrected for bottom -

8" 5 grain brass tamped
 $D/H = 1.32$
 $H/x = 99.5$
 $Wt\% = 19.24 = 0.254 \text{ gm}^3/\text{cc}$
 $V_C = 7.85 \text{ L}$
 $M_C = 1.94 \text{ Kg}$

of pipetted sample.
 Sample purified electrolytically.

%U = 20.73

3/1/47

Experiment 124

8" st. st. reactor lamped

H/x ~ 85

additional 1/16" stainless steel wall added.

Note: The 1/16" stainless cover does not fit snugly on reactor as previously.

Scales # 3 - 100 # 4 - 10 # 5 - 2 Reed - 25 mv.

Use background counts from Exp 123.

Same as in exp 123

4:20	H = 8.0	7.5	7.5	0.60	0.76	
4:30	H = 15.9	25.5	24.0	0.18	0.24	
4:35	H = 18.6	18.5	45.0	39.5	0.10	0.14
4:40	H = 21.3	98.0	89.0	0.046	0.064	
4:50	H = 23.0	271.0	249.0	0.017	0.023	

5:00 H = 23.9 Not Critical. No 7 is dry.

Filling from # 8

5:08 H = 24.1 CRITICAL C.R. 10 1/2 cm below sol. level

Coll 24.0 cm critical

Drawbacks:

- # 7 - 16 cm in 8" reactor.
- # 8 - 18 cm
- # 6 - Dead volume.

Samples taken for $\rho_{app} = 1.137$ (This value is obviously in error).
 $H/x = 91.2$ Lab D analysis with ρ_{app} assumed 1.317.

Conclusion: Comparison of 123 & 124 & assumption that H/x = same in both - the extra thickness of stainless increases critical height by 1.3 cm

$$H/x = 98.2$$

$$\% U = 20.78$$

Experiment 125

~~Marklin~~
3/8/48
Marklin
Joy
Callahan
~~W. W.~~
Cronin

8" Aluminium Reactor

Tamped
~~H_{cr} = 85~~

~~To determine the effect of removing the stainless steel~~

Aluminium reactor (wall 40 mil al, base 1/2" 24ST al) substituted for stainless steel in order to evaluate poisoning effect of stainless - al reactor sprayed with tygon paint inside and out - due to poor alignment of top tapers + reactor some paint has been scraped off.

Trip points - 92x100 on 3; 87x100 on 4.

Scales - #3-10; #4-10, #5-2; R.E. 25 m.v.

In order to examine bottom of reactor, at well to base plate weld, for leaks some solution will be put in before the tamper water.

Source (1/4c in brass sphere) 12 cm from reactor bottom = 45 on scale

→ Zero of sight glass - with this reactor - reads 2mm low.

→ Values of H listed below are those read, need to be corrected.

	H = 0.1 cm	I	II	#6 empty. Filling from #7.	
12:30 P	H = 1.6	5.5	5.5		
		<u>45</u>	<u>60</u>		
		5.0	8.0	I	II
	= 5.0	5.5	8.0	0.910	0.726
	= 10.0	11.5	11.0	0.435	0.528
4:53	= 14.0	22.5	23.5	0.222	0.247
1:00	= 16.0	36.0	38.0	0.139	0.153
1:06	= 18.0	76.5	75.5	0.065	0.077
1:12	= 19.5	219.0	221.0	0.023	0.026
1:23	= 19.8	248.0	247.5	0.020	0.023
1:31	= 20.1	NOT CRITICAL.			
1:36	= 20.3	' "			
1:39	= 20.5	' "			
4:2	= 20.7	Critical with Cd control rod out.			

Ca 2cm left in #7; now filling from #8

$\%U = 20.80$

Drain back to 14cm into #8; to 8.5 cm into #7.

Conclusion: critical with height (corrected) = 20.9 cm - al reactor H_{cr} = 85, Tamped. This value is 1.8 cm lower than the corresponding experiment with a stainless steel reactor of normal wall thickness.

Sample taken on drain-back gone:
(d = 1.319; H_{cr} = 98.2)

11/17/48 DE 20.9 + 1.5 = 22.4 cm
11/26/48 DC H_{cr} = 98.2 = 99.5
8" Aluminium, Tamped
d_{top} = 1.32, d_{bot} = 1.24 = 0.25 in
k_{eff} = 1.26; M_{eff} = 1.84 kg

2/8/48

Experiment 126

8" Aluminium Reactor with 1/16" Stainless Steel Encasing Al.

Tamped.

$k_{eff} = 85 - 98.2$

Macklin
Fox
Gronin
Caehlan

Repetition of #125 with addition of 1/16" stainless steel around al. - Trip points as in #125

Scale #3-10, #4-10, #5-2, R.E. 50mw.

		I	II	I	II	
2:25P	H = 8.5 cm	8.0	89.0	0.625	0.644	
38	= 14.1 cm	20.0	21.0	0.250	0.275	Beginning to fill for #7
44	= 18.3	52.0	57.5	0.096	0.110	#7 not empty - filling from #8.
50	= 20.3	109.5	112.0	0.046	0.052	
57	= 21.6	386.5	397.0	0.013	0.015	
3:05	= 21.9	NOT CRITICAL.				
3:09	= 22.1	Critical with 5 cm Cd control rod below solution surface.				

DRAINBACK: #8 - 18 cm in 8" Reactor
#7 - 16" " 8" "
#6 = Dead volume -

Conclusion - 8" al reactor enclosed in 1/16" stainless sheet - critical at 22.3 cm (corrected for zero).

$k_{eff} \sim 100$

Summary #	Description	H_c	Δ	Effect of 1/16" stainless shell.
#123	Normal wall thickness stainless reactor	= 22.7 cm	} $\Delta = 1.3$	
#124	Stainless reactor plus 1/16" stainless sheet.	= 24.0 "		
#125	al reactor	= 20.9 "	} $\Delta = 1.4$	
#126	al reactor plus 1/16" stainless sheet	= 22.3 "		

= 26.2%

From #123 + 125 al vs stainless, bare $\Delta = 1.8$ cm - however there is included effect of changes in k_{eff} over period of a week. Final conclusions should be drawn after k_{eff} determinations have been made.

$\% U = 20.88$

116
8/9/48

Experiment 127

Fox
Gronin
Callahan

8" Aluminum Reactor encased in 1/16" Stainless Steel Shell.
Tamped. $k/x = 300$ (289.8)

Purpose: To examine effect of stainless steel on critical conditions at this $k/x = 300$.

Solution lines redrained, with vacuum pump to get ^{out} all $k/x = 85$ possible
Trip points: #3 86 x 100, #4 94 x 100
Seals #3 - 100, #4 - 5, #5 - 2, R.E - 25 ms.

Source - 1/2c, bus others - 12 cm from bottom of reactor.
Zero on sight glass = 2 mm solution.

		I	II	M		
2:25P						Filling dead volume from #9.
30	H = 1.0cm	4.0	5.0			#9 empty; start filling from #4
		3.5	5.0			
36	= 8.4cm	5.5	8.0	0.682	0.625	Sight glass = 8.3, Tamps 9.0 indicating some inhomogeneity
	= 15.0					" = 14.9 " 15.8 " "
	= 15.6	10.0	12.0	0.375	0.446	" = 15.75 " 15.75 after blow back.
3:15	= 23.0	18.0	20.0	0.208	0.250	#4 empty; now filling from #3
3:30	= 30.3	30.0	30.0	0.125	0.166	
36	= 40.0	74.5	75.0	0.050	0.067	#3 Not empty - but now filling from #2.
3:55	= 45.2	443.5	448.0	0.064	0.019	
4:05	= 45.7	NOT CRITICAL				
4:09	= 45.9	NOT QUITE CRITICAL				
4:16	= 46.1	Critical with 12cm CD control rod below solution level.				

Draw back into 2 to 40cm
" " " 3 " 22cm

Removed stainless steel shell -

Took sample for Sp gr = 1.103; $k/x =$ _____

Conclusion: Critical at 46.2 cm - corrected for zero -

8.6% U 8.57
8.03% X

Fox $k/x = 290$ data
See Lab data Report # A-1626
3/22/48

2/9/48

8" Aluminium Reactor - Tamped, $H/x \approx 300$. (289.8)

Joy

Cromin
Callahan

Purpose - see #127. also see #125 for description of reactor.
Scales & trip results as before, also same.
"Background" count taken as in #127

	H	I	II	M ⁻¹		
5:18P	H = 21.9 cm	19.0	21.0	0.197	0.238	Beginning to fill from # 3
27	= 32.5	58.0	59.5	0.065	0.084	
36	= 35.7	127.5	127.0	0.029	0.041	
43	= 37.5	379.5	382.5	0.010	0.013	
54	= 37.9	NOT CRITICAL				
6:02	= 38.2	"	"			
6:06	= 38.5	CRITICAL WITH 3cm Cd control rod below solution surface.				

	H/x	8" centimeters
1	? (~320)	~ 20cm.
2	~300	20.5+
3	~300	20.5
4	~300	21
5	empty	
6	~85	Dead volume
7	~85	16 cu
8	~85	18 cu
9	~300	Dead volume + 1cm.

Conclusion ① 8" Al reactor - $H/x \approx 300$ - Tamped Critical 38.6 cm (corrected for zero).

H/x ≈ 300 - Al reactor	H _c	Exp	Δ	
" " + 1/16" stainless steel	= 38.6 cm	128	} $\Delta = 7.6$ cm = 18%	} Effect of Stainless Steel Sheet
" " normal wall	= 46.2	127		
" " + 1/16" stainless steel	= 50.8	122	} $\Delta = 9.9$ cm = 18%	
" " + 1/16" stainless steel	= 60.7	121		

Comparison of Al + Stainless reactors	Exp	H _c	Δ
Al + S.S.	128	H _c = 38.6	} $\Delta = 12.2$ cm = 31.5% of Al val.
Al + S.S.	122	H _c = 50.8	
Al + S.S.	127	= 46.2	} $\Delta = 14.5 \approx 31.5\%$
Al + S.S.	121	= 60.7	

④ above assumes constancy of H/x values in two instances - respectively.

During drain back sample taken for sp. gr = 1.101
 $H/x = 289.8$

11/2/48
38.6 + 1.5 = 40.1 cm bottom corrected
 $H/x = 290$; sp.gr = 1.10; wgt % X = 8.01 ≈ 0.088 gm/cc.
8" Al tamped.
 $V_c = 13.00$ L
 $M_c = 1.15$ kg.

March 31, 1948 -

Beck
McFadden
Crown

8:30 AM. Removed cylinders #3, 4, and 7 - resoldered at leaking points.

3:07 PM. Purpose: mixing solutions in cylinders 1, 2, 5, 9 - (nominally 25-100 μ X.)

3:15 PM - adding from #1. filling dead volume
Counter

	#1	#2	
zero.	48(?)	56.	
2.7.	37	51	#1 empty.
	34	52.	

3:25 adding from #2.

7.9	47.	68.	#2 empty.
	46	67.	

adding from #5.

12.0	71	90	#5 empty.
------	----	----	-----------

adding from #9

16.0	73	95	#9 empty.
------	----	----	-----------

mixed by bubbling air -

Net reading 21. cm -

73 - 95

Drain back - into #1 and #2 and 9

10cm drained of liquid, then sample taken.

remainder drained back. Sp. $A_1 = 1.6514$ $N_H/N_L = \sim 41$

drain back into 1, 2, & 9.

#1 + 2 values very slow on drainbacks, even with vacuum.

4/2/48

Solution Inventory:

	#1	#2	#3	#4	#5	#6	#7	#8	#9
μ X	~40	~40	300	~100	~40	100	-	300	~40
h_1	66.5	34.0	68.6	59.3	72.7	62.4		69.0	MT
h_2	36.8	48.0	35.0	34.3	31.1	40.0		34.7	
Δh in manometer	29.7	6.0	33.6	25.0	41.6	22.4		34.3	
4" cyl	53.4	10.75	90.5	57.0	74.6	51		92.1	
8" " "		2.7w		14.2	18.5	12.7			

During the period 3/9-31

- ① The building wiring was renovated
- ② The laboratory rooms were decontaminated after it was found that there were accumulations of active dust on most all surfaces.
- ③ Preparations were made to improve recovery procedures by:
 - a) Construction of a new extraction column
 - b) Since burning of the waste paper, etc. containing active material in the open distributed activity in the atmosphere - a oven was designed and constructed.
- ④ a 6" al reactor was constructed.
- ⑤ It was proposed to investigate activity of 6" reactor in al at optimum H/X (for cylinder) for this purpose solution of $H/X \approx 24$ (which had been in storage) was mixed with ^{some} $H/X = 100$ to give the solution described on page 118.
- ⑥ Replaced P-18 pipet glasses.

4/7/48

Measurements of cylinder contents show ~ 11 L of $H/X = 40$ which is insufficient to fill a 6" reactor plus dead volume, 17 L being required. To increase the H/X and the volume additional $H/X = 100$ is to be added to the $H/X = 40$ -

4/1/48

Marf H
Maxler
Crown
Callison

To mix $HX = 40$ with $HX = 100$ - ~~to~~ solution
to be mixed in 8" reactor untemped.

Trip points # 3 = 88 + 100
4 = 94 + 100
Scales # 3 - 100
4 - 5
5 - 2
RE - 25 ms.

	I	II	M ⁻¹	
12:40 P	57.5	54.0		
	57.5	54.0	I	II
12:58 P	H=2.2 cm H=3.0	33.5	30.0	
1:15	=19.8	97.5	84.0	0.59 0.64
25	=29.0	110.5	97.5	0.52 0.55
55	=40.8			

1 empty. Filling from # 2

2 empty. Filling from # 4.

4 empty* (Mixed sol). Filling from # 5

5 empty - well mixed.

Drain back:

- 1 Empty
- 2 Empty
- 3 $HX \approx 300$ 90.5 cm in 4" cylinder
- 4 Empty
- 5 $HX \approx 60$ 70 cm in 8" cylinder
- 6 $HX \approx 100$ 12.7 cm in 8" cylinder
- 7 $HX \approx 60$ 10 cm in 8" cylinder
- 8 $HX \approx 300$ 92 cm in 4" cylinder
- 9 - $HX \approx 60$ 11.4 cm in 8" Reactor

(Dead volume in system).

Specific gravity of mixed solution = 1.51 $\approx HX = 60$

~~From the results~~

The quantity of solution mixed (20.8 cm in 8" reactor) corresponds to about 73 cm in a 6" reactor. It would be desirable to be able to put 80-85 cm in 6" reactor requiring about 2L additional solution.

* During the filling from # 4:

- a) a number of air bubbles were carried along by the stream -
- b) long before # 4 was empty, there was a persistent "feel" through the water handle of a "bubbling" it was not possible to determine the source. Possibly due to constriction in line since flow was low. This prob. was not observed when filling from # 5 -

Experiment 129. 8" al ~~Al~~ Reactor.

121
4/2/48

$H/X \approx 60$ (amped)

Crown
Moffatt
Mullin
Lalihan

#5 chamber out of order.

Scales - #3 - 100 #4 - 10.5 RE 25 ms.

Source - (1c) on bottom of reactor.

	I	II		
$H = -0.2$	12.0	13.0		
	12.5	13.0		
	17.3	17.3		
3:02 P	= 9.3 24.5	21.5	I m ⁻¹	II
11 P	= 15.3 58.5	53.0	0.50	0.60
			0.210	0.245
17	= 17.2 127	110.5	0.101	0.117
25	= 17.9 212.5	186.0	0.058	0.071
33	= 18.3 484.0	428.0	0.0254	0.0304
48	= 18.7			
55	= 18.9			

Filling from #7.

#7 empty. Filling from #5.

Not critical.

Critical with 8 cm cd rod below solution level.

Conclusion - 8" al Reactor. $H/X \approx 60$, critical at 18.8 cm solution -
(= 19.0 cm corrected for sight glass zero)

Inventory: (see also pg 120).

#5 - $H/X \approx 60$

20 cm in 8" reactor.

#7 $H/X = 60$

9.3 cm in 8" reactor plus dead volume.

Specific gravity = 1.51

Sample taken for H/X determination -

$H/X = 58.70 = 29.35\%$ by wgt of U.

11/17/48

19.0 + 1.5 = 20.5 cm - Hc bottom corrected

$H/X = 58.7 \rightarrow 58.8$

8" al, (amped)

$\rho_{sp} = 1.51$

wgt % X = 27.45 = 0.415 gm/cc

$V_c = 6.65 \text{ L}$

$M_c = 2.76 \text{ kg}$

11/17/48 H/X from Lab D - Report A1714

Exp 129 29.35% U

130 29.46

ave 29.40% U

$H/X = 58.8$

4/16/48

122
4/5/48

EXPERIMENT 130

Crown

8" Al. Reactor with 1/16" Stainless Steel (Shape)

Jrx

Extra wall added -

Vision

$H/x = 60$

Callahan

Trap points - #3 85x100, #4 85x100.

Pressey

Scale - #3-100; #4-10; #5-2, R.E. - 25ms.

Source - 100 in brass sphere - 12 cm from bottom of reactor.

1:25

Filling dead volume from #7

1:40

H: -0.2 cm	#1	#2	C ₁	C ₂
	5.5	4.5	Background.	
	6.0	4.5		
	5.7	4.5	← C ₀	

1:50

H = 9.7 cm

12.0

11.0

0.48

0.41

Cyl #7 dry from #5

2:05

14.1

27.0

25.0

0.21

0.18

2:15

16.5

52.5

46.0

0.11

0.098

2:20

17.5

81.0

72.0

0.070

0.063

2:25

18.4

126.0

114.0

0.045

0.390

2:35

19.2

240.0

209.5

0.024

0.022

2:45

19.6

400.0

350.0

0.014

0.013

2:55

~~19.8~~ 19.9

Not Critical.

3:00

20.1

Not Critical

3:10

20.3

Critical with rod 10.3 cm below solution level
Call 20.2 cm critical (uncorrected)

Drawbock

#5 - 20 cm (8")

#7 dead volume + 9.5 cm (8")

Conclusion

8" al. reactor with 1/16" stainless steel extra wall is critical at { 20.2 cm with $H/x \sim 60$
= 20.4 corrected for sight glass 3ms

Specific gravity (measured) = 1.52
this corresponds to $H/x \sim 57, 58$

$$H/x = 58.38 \approx 29.46\%$$

EXPERIMENT 131

123

4/15/46

Crown
Pressing

Carlson

8" Stainless Steel Reactor - Normal Wall

H/X \approx 60; Tamped.
(58.38)

TRIP POINTS #3 86x100 #4 94x100.
Scales RE-25mm, #3-100 #4-5 #5-2.
Source 12cm from reactor bottom.

10.50 A

Filling dead volume from #7.

11:00 A $\frac{I}{6.5}$ $\frac{II}{6.0}$

11:10 A H=0 6.5 6.0
6.0 5.0
6.5 5.5

		I	II	I	II	
20	H=9.2cm	11.5	10.5	0.55	0.525	#7 Empty. Filling from #5
11:30	=14.1cm	31.5	29.0	0.20	0.19	
45	=16.0	56.0	50.0	0.113	0.110	
54	=17.3	100.5	87.0	0.063	0.063	
12:00	=18.0	164.0	151.5	0.039	0.036	
05P	=18.5	268	234.5	0.024	0.024	
15	=19.2	1007	982	0.006	0.006	
35	=19.4	Critical with 6cm of Co control rod below solution level.				

Conclusion 8" Stainless Reactor, same solution as used in #129 & 130, H/X \approx 60
Critical at 19.3 cm - (~~19.5 cm corrected for sight glass error~~).

Draw back: #5 - 20cm in 8" reactor = 35.6 cm in 6" reactor
#7 - 9.5cm " " + dead volume = 16.9 " " + 11cm
#9 " " " " = 19.6 " " = 0.5

11/17/46 19.3 + 1.5 = 20.8 cm - He - bottom corrected.

11/14/46 H/X = ~~58.4~~ 58.8

8" Stainless, tapered

wt % K = 27.45 = 0.415 gmK/cc

ptg = 1.51

Vc = 6.74L

Mc = 2.80 kg.

Experiment 132

4/6/48

6" Aluminium Reactor - Tamped

Cronin
Pressey
Joy
Callahan

H/X = 60 - (58.38)

Trip points same as before

Scales #3-100, #4-5, #5-2, RE-25ms.

Scum - 12 cm from bottom of reactor

3:20 Filling dead volume from #9.

3:27	H = 1 cm	I 6.5	II 5.0
		<u>6.0</u>	<u>4.5</u>
		6.3	4.8

3:30 H = 1.8 cm #9 empty, filling from #7.

3:34	H = 5.1	#9 empty, filling from #7.			
4:1	= 15.1	I	II	M ⁻¹	II
4:5	= 15.1	15.5	11.5	0.41	0.42
5:5	= 20.0	19.5	15.5	0.32	0.31
4:05	= 25.0	27.0	21.0	0.233	0.23
7:0	= 35.0	37.0	30.0	0.17	0.16
25	= 36.5				
30	= 45.0	54.5	45.0	0.116	0.107
38	= 55.2	88.0	73.0	0.072	0.66
50	= 67.1	124.5	128.0	0.041	0.038
5:00	= 66.0	316.0	259 238.0	0.020	0.019
10	= 68.0	768	624	0.008	0.008

(Solution mixed - no dip in sight glass valve).

#7 empty, filling from #5

30	= 68.5	NOT CRITICAL			
37	= 69.0	NOT CRITICAL			
45	= 69.9	Critical with 13cm CD control rod below sol. surface #5 empty.			
50	= 69.5	" " 8 1/2 " " " " " " " " " " " "			
55	= 69.2	" " CD rod at surface of solution			

Conclusion 6" Aluminium Reactor - H/X = 60, Tamped Critical at H = 69.2 cm.

Inventory	#	H/X	Description
	1	-	Empty
	2	-	Empty
	3	≈ 300	90.5 cm in 4" cylinder
	4	-	Empty
	5	≈ 60	35 cm in 6" cylinder 25.7
	6	≈ 100	12.7 cm in 8" cylinder
	7	≈ 60	35 cm in 6" cylinder
	8	≈ 300	92 cm in 4" cylinder
	9	≈ 60	Dead volume

Sp gr taken on drain box = 1.51

11/17/48 DC 69.2 + 2.6 = 71.8 cm
= He bottom corrected
H/X = 58.4 58.8
6" at 4cm pad
Wtd % K = 27.45, = 0.415 g/lcc
Opt = 1.51
VC = 13.102
Mc = 5.44 g.

Experiment #133. 7" stainless steel, $H/x = 60$ (58.38) (Repetition of #6 & #7).

Back
Pressure
for
Crown
McLendon.

To measure effect of Top Tampering.

A - With Normal Tampering

Trips points # 3,83 #4,95.
all instruments OK.

Time	Solution Level	Counter Reading		M ⁻¹		REMARKS
		#1	#2	#1	#2	
10:52.		#1	#2			Adding from #5
	Behind.	4.5	5.5			
11:04	0.3	5.5	4.5			
		6.0	4.5			
11:13	20.0	30.0	25.5	.183	.177	#5 MT - (H=25.0)
11:24	25.0	66.0	53.0	.083	.085	Start adding from #7
11:33	28.5	178.	147.5	.031	.031	
11:43	30.5	Not Critical - Close -		Rod out -		
11:46	30.7	Critical; Rod out;		Source removed.		

Conclusion: 7" S.S. Reactor Tampered - $H/x \approx 60$ Critical at 30.7 cm.
This duplicates results of Exp. #6 within 1mm.

Drain back part way; remove top tamper, and continue.
~~Drain back~~

B. With No Top Tamper - otherwise Normal.

Time	Level	Counter Reading		M ⁻¹		REMARKS
		#1	#2	#1	#2	
12:06	27.5	67	54	.082	.083	#5 MT @ 31.0 cm
12:18	30.0	131	109	.042	.041	
12:23	32.1	447	373	.012	.012	
12:28	32.6	NOT CRITICAL -		ROD OUT -		
12:35	32.8	CRITICAL!		ROD OUT, SOURCE REMOVED.		

Drainback

#5	32.8	#7	9.7	#9	dead vol.
	9.7		0.0		
7" cyl	23.1cm		9.7		
4" cyl	7.5		5.16		
	70.17		29.7		

Dilution to $\frac{1}{x}$ in 200

Solution Inventory:

	#1	#2	#3	#4	#5	#6	#7	#8	#9
H in 4" cyl.	—	—	90.5 cm	57.6	70.7	70.7	29.7	92.1	dead Vol
$\frac{1}{x}$			300	60	100	60	300	60	
				empty		5.5 liter			

From calc. using all $\frac{1}{x}$ 300 (ca 14 liters) and adding 6 liters $\frac{1}{x}$ 100 should reach $\frac{1}{x}$ in 200 or 18.5 additional in 8" reactor.

20 liters = 49.5 cm in 8" reactor (to dead Vol. subtracted)

Drawback of mixed $\frac{1}{x}$ 200

#3	20 cm in 8" R
#6	20 " " "
#8	$7\frac{1}{2}$ + Dead Vol \approx 17.3 cm Total

4/8/48

Experiment #134 H/x ²²⁰⁰ "8" M - Reactor

Crown
Fox
~~...~~
Murray
Prelay

Tamped with 1/16" starter

#3 - 100 scale 4 - 10 scale 5 - 25 scale Reed - 25 Scale

Time	Sol Level	Counter Reading		H'		Remarks	
		#1	#2	#1	#2		
9:20	-0.1	4.0 ✓	7.0	9.0, 8.0, 6.5	Use 7.0	Adding from 8	
9:23	7.1	6.5	6.0	.63	—	8 empty adding from 6	
9:30	15.1	14.8	14.5	.27	.48		
10:00	18.0	20.5	18.2	.195	.384		
10:12	22.0	39.0	32.0	.103	.22		
10:22	26.0	76.0	58.0	.053		Left 6 adding from 3	
10:33	27.0	168.3	139				
10:40	28.5	354	287				
10:48	29.4	Critical with 7 cm of control still in					
11:05	29.2	Sub critical with Rod all out					

Critical at 29.3 cm ± 0.1 -

Drawbar as per Exp #133 opp. Page

H/x = 174.53

11/17/48 29.3 + 1.5 = 30.8 cm = the bottom corrected
H/x = ~~174.5~~

for H/x see p 128 this book

128 4/6/48

Experiment #135

$H/x \approx 200$ 8" Al Reactor

Cromin
Fox
Meritt
Murray
Presby

Tamped (*134 with Stanks Removed)

#3-100X #4-20X 5-2X Reed 50X

	Liquid Level.	COUNT #1	#2	RECP. #1	#2	soln.
12:25 p	0	4.5 (4.5)	4.5 (EST)			from #8
12:30 p	7.1					8 empty 7cm + 10X
12:35 p	15.0	15.3	14.5	.295	0.31	adding from #6
12:40 p	20.0	35.0	30	.13	.15	
12:47 p	23.1	78.0	66	.058	.068	
12:53 p	25.0	177.0	149.0	.025	.030	stopped #6
1:00 p	26.0	470	381	.0096 .030	.0005	from #3
1:10 p	26.5	NOT CRIT.				
1:17 p	26.8	super crit. at 17 cm rad in soln.				Draw back same as

Est. Critical height 26.6 cm.

Exp. 134

Measured ρ_p 1.167 approx H/x 182

This cannot be checked } $H/x = 174.53 \approx 12.26\%$ α by weight }
See Lab D report # A1774 4/16/48 }

11/17/48 DC 26.6 + 1.5 = 28.1 = H_c bottom corrected
 $H_c = 174.5$ 192
 8" Al Tamped.
 $\rho_p = 1.17$

$H/x = 192$
 $wb \rho_p = 11.45$
 $= 0.134$ gwt/cc.

$V_c = 9.11$ R
 $M_c = 1.22$ Rg.

11/17/48 DC

4/8/48

Experiment #136, $HX \approx 200$ (174.53) 8" SS. Reactor 129

~~6/11/48~~
Morrill
Pressey
Murray
Fox

#3 10.0 #4 - 5 #5 - 2 Reed 25-

Background 4.5 on both #1 & #2

Time	Liq. Level	Counts		Recip.		#2
		#1	#2	#1	#2	
2:25-	6.5	-	-	-	-	-
2:35-	15.3	15.5	13.5	.29	.33	#5 empty start
2:42	20.2	33.0	29.0	.136	15.5	#3 at 11cm*
2:50	25.0	92.0	80.6	.049	.056	
3:02	27.5	824	686	.0055	.0065	
3:10	27.9	824	critical	with rod	out	

Drumback:

20 cm m #8
? #6
7 cm + d. Vol. #3

11/17/48
u/w/08
 $27.9 + 1.5 = 29.4$ cm the bottom (corrected)
 $HX = 174.5$ 192
 8" Stainless stamped (?) probably
 $\rho_{sp} = 1.17$
 $w \times \rho_{sp} = 11.45 = 0.134 \text{ gm/cc}$
 $Vc = 9.53 \text{ L}$
 $Mc = 1.28 \text{ kg}$

* Evidently some sol. was added from #6 by mistake

4/9/48 | Filtered HX ~~at~~ = 200 solution with glass wool -
Flashed out right glass + main liquid line
with distilled water - Found Kleenex, profoant & etc.

130 4/13/48
7.343/48

Ex. 137

CALLIHAN

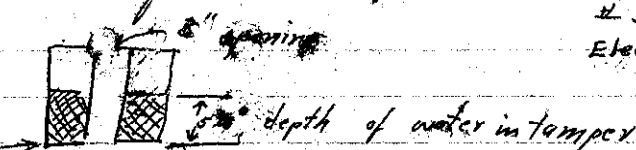
CRANIN

PRESSEY

FOX (P.M.)

7" Reactor #4 #60 with Modified Tamper

#3 - 100X
#4 - 5X
#5 - 2X
Electrometer 25



Source moves through 3" opening.
The 5 1/4" depth of water in tamper simulates the amount of 3" pipe at bottom of Reactor which is tamped.

#5 cyl 7" 23.4 cm #7 29.7 #9 lead Vol.

Control at zero (on scale) is actually 3 cm above bottom of Reactor.
Source 12 cm from bottom of reactor.

137a

Time	Soln LEVEL	Back Ground Count.				#1. 7.0				#2. 6.0		Soln level 0.2 cm #9 MT @ 2.5cm filling from #7
		TAMPER AT TOP OF SOLN LEVEL		1/m ₁ 1/m ₂		SOLN IN HOLE IN TOP TAMPER		1/m ₁ 1/m ₂				
10:00 am												
10:27A	3.6	7.0	5.5			4.5	4.0					
10:57A	6.5	7.0	6.0			7.0	5.5					
11:15A	12.6	10.0	8.0	0.7	0.75							
11:25A	16.7 16.7	16.5	14.5	0.44	0.41	11.5	9.5	0.61	0.63			
1:07p	19.7	26.5	22.0	.26	.27	17.5	14.0	.40	.43			
1:27p	22.8	40.5	33.5	.173	.179	25	22	.28	.27			
1:43p	25.7	70.5	59	.10	.10	38.5	31	.18	.194			
2:01p	27.3	103	87	.068	.069	50	42	.14	.143	STOPPED USING #7		
2:17p	28.9	180	151	.039	.040	65	56	.11	.11	Filling from #5		
2:35p	29.9	350	293	.020	.020	80	67	.088	.089			
2:52p	30.65	*TAMPER POSITION INDICATOR SHOWED 1cm DISCREPANCY. INDICATOR RESET to liquid level.				114	98	.061	.061			
		615	524	.011	.011	110	90					
3:10	31.3	Critical with only 27cm of liquid				108(109)	89(88)	.065	.068			
						122	96.5	.057	.062			
3:18	31.0	Not quite critical.				177	143	.039	.042			
						256	212	.027	.028			
						681	556	.0103	.0108			

CRITICAL HEIGHT 31.1 cm

Not Critical
Super-Critical
CRITICAL Height. 28.8 cm in 7" dia
+ 30 cm in 3" dia

The soln. was Drained while critical from 57.7cm to 42 cm before activity was noticeably reduced.

NOTE: ① Voltage surges made #4 inoperative on 5 SCALE. Put #4 on 100 SCALE + #3 on 10 SCALE.
② Approx 3:30 pm. It was noticed that water was on floor UNDER REACTOR. TAMPER WATER INLET valve had leaked and overflow hose had fallen off. Mopping up operations followed.

Spec. GRAVITY = 1.498
 (H/x = 60.85)

Conclusions:

① 7" reactor, H/x = 65
 tapered except for 3"
 dia. area at top -
 critical at 31.1 cm -

② 7" reactor as above
 but with 30cm long
 3" dia section at
 top critical at
 28.8 cm -

③ Reducing this 30 cm
 to ca 7.5 cm did
 not noticeably
 reduce activity -

1376.

Soln # 7" cyl.	Soln. Ht. 3" Ann.	
0.8	30.8	
0.8	30.8	
6.8	36.7	
11.2	41.1	11:45A
14.3	44.1	1:15P
17.3	47.2	1:35P
20.4	50.3	1:52P
22.1	52.0	2:08P
23.7	53.5	2:25P
24.7	54.7	2:42P
25.2	55.2*	3:24P
25.2	57.2*	4:22P
25.2	55.2	4:29P
25.7	55.8	4:42P
26.6	56.6	4:56P
27.3	57.2	5:07P
28.3	58.3	5:20P
28.7	58.7	5:32P
28.9	57.7	5:35P

Inventory	H/x	
1	Empty	{values need}
2	Empty	{repair}
3	200	Dead volume + 7" - 8" cm - = 23cm
4	Empty	
5	65	23 7" cm.
6	200	?
7	65	29 7" cm
8	200	20 8" cm
9	65	2cm (7") + dead volume.

Lab. Sample 28.47% U by wt. $\frac{11/30/48}{\rightarrow} H/x = 61.9.$

4/14 - Values on 1+2 replace

132-4
3-15-48

Experiment 138 (a)

MURRAY
Morfit
Fox
CRONIN
PRESSEY

7" Reactor $H/x \approx 200$ with modified ^{top} Tamper
Meter scale #3 100X #4 10X #5 2X
Electrometer not working.
Same Experiment as #137 except H/x ratio.

Back ground counts #1 5.0 (6.0) #2 5.0 (5.0)

TAMPER AT top of soln level.

Time

Soln. level 1 #1 1 #2 1 1/2 1 1/2

TANKS

10:25 A.

DEAD VOL. from #8

10:45 A.

25 cm. The safety dump dumped while ^{sight} line was being blown out. #4 tripped. Activity level was $1\frac{1}{2}$ on the 10X scale. Previously set to dump at 6 on the 100X scale.

Filling from #6

Draining back to #6 +8?

2:28 pm

Refilling from #8
Back ground counts

#1 9.0 (9.0) #2 7.5 (7.0)

DEAD VOL. from #8

Soln level 1 2 1/2 1/2

7cm from #8

2:47p

25.1 16.5 14.5 .55 .48

filling from #6.

2:55p

36.4

#6 MT.

At 2:59 pm The dump dumped again. This time we found the trouble. The frame of #4 meter is hot and was grounded by the chain touching the #9 valve rod.

filling from #3.

4/20/48

Drain back on 4/15 into 6 + 8 for few

Experiment 138 b.

4/20/48

7" Reactor $M_x = 200$ with modified top temper. Standard Stainless Reactor.

Fox
Pressay
Callihan

Soln. 15cm high in 3" hole in Top Tamper.

Scales: ^{#3} 100x ^{#4} 10x ^{#5} 2x R.E. out of order. Source ca 12cm from bottom -
TRIP PTS - 9.5 ^{#3} 6.5 ^{#4}

TIME	SOLN Height. in 7" cyl.	Soln Height in 3" cyl	#1	#2	1/m	1/m ₂	
9:45 A							Filling from #8
9:50 A	0.2cm		6.0	5.0			
			5.5	5.0			
9:58	10.7	0	7.5	6.0	0.77	0.83	#8 Empty, Filling from #6
10:07	20.1	0	14.0	10.5	0.415	0.476	
115	32.2	32.2	12.0	10.0	0.483	0.500	
121	27.1	0	21.0	17.0	0.276	0.294	
25	24.2	39.2	18.5	16.5	0.313	0.303	
32	34.7	0	29.0	25.0	0.200	0.200	#6 Empty
38	31.7	46.7	28.0	25.0	0.207	0.200	Filling from #3
47	46.7	31.7	28.0	25.0	0.207	0.200	
47	43.0	0	44.0	39.0	0.132	0.128	
55	40.2	55.2	42.5	36.0	0.136	0.139	
11:05	50.1	0	72.0	61.0	0.081	0.082	
11	47.4	62.4	63.0	56.0	0.092	0.089	Limit of up motion of tamper.
25	49.8	64.7	71.0	70.0	0.075	0.071	#3 Empty.

DRAIN-

INVENTORY

- 1 - Empty
 - 2 - Empty
 - 3 - 22 7" cm $M_x = 200$
 - 4 Empty
 - 5 23 7" cm $M_x = 65$
 - 6 - 22 7" cm $M_x = 200$
 - 7 29 7" $M_x = 65$
 - 8 - 22 7" cm $M_x = 200$
 - 9 - 2 7" cm + Dead Volume $M_x = 65$
- 12"
7.8
9.9

Conclusion: Because of insufficient solution and because reactor was too short it was not possible to reach criticality.

at multiplication of ~ 13 a column of solution 3" dia + 15cm long reduced the 7" dia cylinder height ca 2cm at this activity -

134

4/20/48

EXPERIMENT 139

Presses

7" REACTOR: Normal Stainless Steel -

Fox

 $H_c \approx 200$ Tamped.

Calibration

(180.04)

To compare ~~to~~ normally tamped experiment
with modified tamped -

Scales - #3 - 100X, #4: 10X #5 - 2X - Read elec. out of order

Trip points - same as #138 b.

Source ca 12 cm from bottom of reactor.

	H	I	II	I	II	
1:40 P	0.1 cm	8.0	7.0			These values high because top tamped was not all way down.
		8.0	7.0			
		5.9	5.0	Background Exp 138		Filling from #8
1:48	8.6 cm			0.305	0.294	#8 Empty; filling from #6.
2:02	29.6	14.0	17.0	0.242	0.244	#6 Empty; filling from #3
2:10	37.7	28.5	23.0	0.203	0.217	Calculated from C = 5X 5.0 =
2:25	44.9	41.0	36.0	0.141	0.139	
2:31	50.0	63.0	44.0	0.092	0.093	
2:38	52.5	75.5	67.5	0.077	0.074	#3 Empty.

Conclusion: Insufficient solution to reach criticality -
Extrapolation of above data to M_{∞} gives approximately
same length (H_c) as modified tamped.

2:55	0.1 cm	5.0 4.0 3.0	3.5 2.5	Background values taken during draw back - Effect of background is to change curve slope - probably not other extrapolated values significantly.	
------	--------	-------------------	------------	--	--

Specific gravity 1.176

N/X

Analysis

12.78%

U by wt.

$H/X = 183.$
11.94% X by wt.
sp. g. = 1.118
0.141 gpt/cc.

Inventory: #8 - 8cm (7") + Dr. $H_c \approx 200$ -

Other - see #133

 $H = 52.5 + 1.9 = 54.4$ cm $V = 13.50$ L $M = 1.90$ kg

11/17/48

Estimated $H_c = 61$ cm + 1.9 = 63 cm $V_c = 15.6$ L $M_c = 2.2$ kg.

4/21/48
X

103

135

Experiment 140 -

12' Stainless Steel Cylinder - Tamped. $H/X \approx 60$. (61.49)

Beck
Fox
Crown
McLendon.

Instruments - Trip on # 30-90, #4 at $5\frac{1}{2}$ (scale of 7).
#1, #2, #5 OK, Process monitor OK - Read out of order.

Solution Level	Background	Counting Rate		Co/C		#5	MT
		#1	#2	#1	#2		
10:15		6	5.5				
		6	5.5				
	zero -	6	6				
10:45	9.4	46	37	0.13	0.16		
11:10	11.6 - not critical						
11:10	11.7 super critical						

Conclusion: Critical at $11.65 \pm .05$ cm. Completely Samped.

28.28 % O by wt.

11/17/48
11/26/48

$11.65 + 0.65 = 12.3$ cm = H_c bottom covered
 $H/X = 61.5$ 62.6
 12" Stainless Tamped.
 $wH \% X = 26.41 = 0.394$ gm/cc
 $\rho_{sp} = 1.49$
 $V_c = 8.97$ L.
 $M_c = 3.53$ kg.

H/X from Lab Analysis Report 1760A
4/29/48

28.28 % O }
 26.41 % X } by wt.
 $H/X = 62.6$
 0.394 gm/cc solution.

4/21/54 DC

Exp. 141. 12" Stainless Steel - Untamped $H/X \approx 60$
(61.49)

Beck
Metelson
Fox
Crown.

Instruments same as for former experiment.

partial drainback - then removed tampering
and began new experiment there.

Level	Rate		c/c		c/c	
	#1	#2	#1	#2	adjusted to true zero - determined after 4 ft.	
zero	14.5	12				
11:25 zero (9.6)	66	54.5				
12.4	114.5	99	.54	.55	.262	.252
14.1	167	142	.395	.385	.18	.187
15.6	235.5	197	.380	.375	.13	.122
17.1	322	294	.204	.186	.093	.082
18.5	575	481	.115	.113	.052	.05
	557	520	*	*		

True zero (30) (24)

Conclusion - (1) Did not become critical at 18.5 cm solution level.
(2) Undoubtedly would have become critical at
21. ± 0.5 cm solution level.

Background counts at zero level

#1	#2
47	43
47	43.5

Sample taken for lab Sp. Gr. - 1.486

11/17/54 DC
11/20/54 DC

$21 + \frac{0.7}{2.6} = 21.6$ cm estimated He bottom corrected

$H/X = 61.5 \approx 62.6$

12" Stainless untamped.

$wb\% X = 26.41 \approx 0.394 \text{ gm X/cc}$

$\rho_{\text{gr}} = 1.49$

$V_c = 15.83 \text{ L}$

$M_c = 6.24 \text{ kg}$

Dilution to $\frac{1}{4}$ 500

3:40

Solution run into 12" cyl to ht of 14.8 cm

drained into

	11.95	
into #1	2.85 cm =	2.06 liters
sol'n ht	9.05	
into #2	2.90 =	2.11 liters
#3	2.90 =	2.11 liters
#4	?	
#5	3.00	
#6	2.30	
#7	1.70 =	
#8	0	

Calculated: for each liter of sol'n add ^{1.74} ~~1.74~~ liter H₂O
 1 liter in 4" cyl = 2.83 cm in 12" cyl.

at ht. 6.15 #8 was emptied to ht of 7.90

Total sol'n ht = 16.55 cm = 12.05 liters
 $\frac{3.5}{15.55}$ dead Vol
 15.55 liters sol'n

in #4 + #8 dead Vol included (must be measured)

before dilution

	1	2	3	4	5	6	7	8
h	57.6	57.2	57.7	57.31	57.2	58.6	55.9	57.7
h ₂	45.2	45.5	45.1	45.9	45.5	46.9	46.9	45.0
ch	12.4	11.7	12.6	12.2	11.7	8.7	9.0	12.7

$\frac{296}{117} = 2.52$

ht in 4" cyl 31.2 29.5 31.8 30.8 29.5 21.9 22.7 32.0

area of 4" cyl 91.07

Vol. Sol'n 2.56 2.39 2.59 25.6 2.38 1.78 2.34 26.0

1000 4.40 4.15 4.50 4.35 4.15 3.10 3.20 4.50

6.96 6.54 7.09 6.85 6.54 4.88 5.04 7.10

12" cm = 9.55 9.0 9.7 9.4 9.0 6.7 6.9 9.75

Exp. 742 12" Stainless UNTamped $\frac{H}{X} \approx 500$
(493.6)

Murray
Murphy
PRESSEY
Fox

INSTRUMENTS #3 100X #4 10X #5 1X
Zero actually zero on sight glass.

Time

2:05 pm

Back ground. #1 30 (28) #2 20 (20)

Soln	Count.	c/c.	
Level	#1	#2	#1

Cyl #8 MT@53cm
Cyl #7 MT@11.8cm
Cyl #6 MT@18.4cm
Cyl #5 MT@27cm
Cyl #4 MT@36.5

2:27 pm	18.4 cm	29.5	24	.98	.83
2:42	21.9 cm	55	37.5	.53	.53
2:45	24.4 cm	68	51	.43	.39
2:52	27.1	91	68	.32	.295
3:02	30.9	132	95	.22	.21
3:12	34.9	203	144	.143	.139
3:22	39.0	322	240	.109	.083
3:35	43.0	618	452	.047	.043

3:41

3:45 45.6 #3 MT

3:47 45.6 Start #2

3:52 47.5 ~~778~~ 778 .0325 .0257 20.5 cm cl Rod in

4:07 49.9 (Not Critical with Rod out but could not count)

4:07 49.9 Super Critical rod 17.9 cm in

4:12 49.5 " rod 16 cm "

4:15 49.0 " rod 10.3 cm "

4:20 48.6 " rod 8.2 "

4:23 48.0 Sub Critical rod out.

4:27 48.2 Critical rod out

Conclusion: Crit. Height \approx 48.2 cm.

Sample taken for analysis Sp. 1.068 - 5.22% U by WT
See Lab D analysis Report 1760A 4/29/48

Draw back

	1	2	3	4	5	6	7	8	9
--	---	---	---	---	---	---	---	---	---

Inches in 12" Reactor 9.55 9.0 8.7 9.4 9.0 6.7 6.9 9.75

11/17/48 pc 48.2 + 0.65 = 48.9 = Hc bottom corrected

11/24/48 pc HX = 494 + 499

12" Stainless untamped.

Vc = 35.67 L.

Mc = 1.86 kg. 1.86 kg.

Sp. = 1.07

whl %U = 4.88 \approx $\frac{0.0522}{0.0522 + 99.9478} \times 100$

Callihan
Cronin
Fox
Morditt
Macelin

Exp 143 12" STAINLESS STEEL TAMPED #12 = 500 - (493.6)

Instruments - 3, - 100Y; 4 - 10Y, 5 - 2Y P.E - 25mv
Source - 11v.c. ⁶cm from bottom - #3 9/
Control Rod - Van of Co. #4 5.8

11:10 Filling dead vol. from number 8

Background - #1 5.0, 6.5, (5.5) ← used #2: 5.0, 9.5, (5.0)

	Soln Level	Count	C/c.	
11:25				
11:40	5.3	4.5	4.5	
11:50	7.5	6.5	5.5	.847 .908
11:55	9.2			
12:00	13.5	12.5	11.0	.440 .455
12:15	20.2	35.5	31.5	.155 .158
12:25	22.5	64.5	55.5	.092 .090
12:33	24.9	362.0	309.0	.015 .016
12:43	25.2	765	670	.0072 .0077
12:54	25.5	Not Critical with Vano out.		
1:11	25.7	Super Critical - Critical with rod 14 cm out from bottom.		

Filling from #5
#5 Empty
From 8 - 8 Empty.
#6 Empty
From #4

Conclusion: Critical Height 25.6 ± 0.1 cm.

Drainage: Same as #142

11/17/48 DC $25.6 + 0.7 = 26.3$ cm = He bottom corrected.

11/28/48 DC $Hx = 499$
12" Stainless tamped.

$\rho_{sp} = 1.07$
 $w\% K = 4.88 \equiv 0.0522 \text{ gmK (sol.)}$
 $V_c = 19.19 R$
 $M_c = 1.00 \text{ kg}$

Corresponding to DC 11/28/48.
 $Hx = 499.4$
 $w\% K = 4.88$
 $\rho_{sp} = 1.07$
 $0.0522 \text{ gmK (sol.)}$

140 4/23/48

Experiment 14A: 12" STAINLESS STEEL REACTOR

H₂O TAMPED - Cd SHIELDED - H₀ = 500

FOR
CRONIN
CALLINAN.

Instruments - #3 - 100 - #4 - 10 #5 - 2 RE 25m.
Source 6cm from neutron bottom -
Trap points - Same as 143

		I	II	M ⁻¹		
3:03P						Filling dead volume from #8.
07	H = 0.5cm	5.5	4.5			
		5.0	4.5			
		(3.3)	(4.5)			
15	= 5.7			I	II	#8 EMPTY, filling from #6
21	= 12.2	8.5	7	0.624	0.643	#6 Empty, filling from #5
36	= 17.5	14.0	12.5	0.379	0.360	
41	= 20.4	19.5	16.5	0.272	0.272	#5 Empty, filling from #4
55	= 24.9	32.5	28.0	0.163	0.161	
4:03	= 28.0	56.0	50.5	0.095	0.089	Ca 1.8cm left in #4; filling from #3
12	= 31.1	243.0	212.5	0.022	0.021	
18	= 31.7	NOT CRITICAL				
22	= 31.9	"				
33	= 32.1	CRITICAL WITH TOP TAMPER IN CONTACT -				

Conclusion -

12" stainless reactor - Tamped plus Cd shield - Critical with H = 32.1cm -

~~32.1 cm when counted~~
~~for system from top~~

INVENTORY	H ₀			
1	500	9.55	12" cm	= 13.7 10" cm
2	-	9.0	"	= 13.8 "
3	-	9.7	"	= 14.0 "
4	-	9.7	"	= 13.2 "
5	-	9.2	"	= 13.2 "
6	-	9.0	"	= 13.2 "
7	-	8.6	"	= 13.8 "
8	-	6.9	"	= 9.9
8	-	2.0 + dead volume		= 2.5 + DV.
9	60	?		

H/x = 493.6

11/17/48 de 32.1 + 0.7 = 32.8 cm = H_c bottom corrected

11/28/48 de H₀ = 494 499

12" stainless, tamped, Cd shield

ρ₀ = 1.07

with ρ₀ x = 4.88 = 0.0522 gm/cc

V_c = 23.93 L

M_c = 1.24 kg, 1.25 kg

H₂O tamped - H/x = 501

Pressey
Jov
Cronin
Callihan

Instruments: #3 - 100x #4 - 10x #5 - 2x RE - 25mm.
Top joint #3 - 82 x 10 #4 - 5.1 x 100.
Source - 15 cm from bottom of reactor.

10:40A

Filling from #8

45	H = 0.0 cm	I	II
		4.0	3.5
		3.5	3.0
		<u>4.0</u>	<u>4.0</u>
		3.8	3.5

	=2.4				
	=7.2	5.0	3.5	I	II
11:00		50.			
09	=15.8	7.0	6.5	0.544	0.538
18	=27.5	16.0	14.5	0.238	0.241
27	=28.1	21.5	18.5	0.177	0.189
35	=28.8	31.0	26.0	0.123	0.135
49	=35.1	76.0	68.5	0.050	0.051
12:10	=37.1	133.0	120.0	0.029	0.029
19	=38.6	276.0	246.5	0.014	0.014
29	=39.2	415.0	368.0	0.009	0.009

#8 EMPTY - filling from #6 -

#6 EMPTY filling from #5

#5 Empty filling from #4.

Stop filling from #4 - 7:40 AM; filling from #3.

Top tamped upper surface level with top of reactor.

At this point the top tamped, upper surface was ~ 2.5" above reactor top. There is a danger of losing solution through the annulus between the tamped + reactor, so no further solution was added - and present data were extrapolated.

Conclusion: Extrapolation of Mⁿ curve, from M = 100. gives H_c = 39.6 cm - 10" stainless reactor, tamped, H/x = 501 -

= 39.8 cm when corrected for soft glass zero eq.

Solution returned to cylinders from which it was removed.

H/x = 493.6

11/17/48 39.8 40.7
39.6 + 0.9 = 40.5 cm estimated H_c bottom corrected

11/28/48 H/x = 494 499
10" stainless tamped.

R_p ρ_w = 1.07

wht % X = 4.88 = 0.0522 gm X / cc.

V_c = 20.62 L

M_c = 1.08 Kg.

4/26/48

EXPERIMENT 146

Pressure

10" Reactor (Stainless). Untamped; $H/x \approx 500$. (493.6)

Crown

Top

Call har

Instruments: 3-x100, 4x10 5x1, RE - 25ms

Trip points - see exp 145

Source - 15 cm from bottom of reactor.

		I	II		
1.45 P	H=24cm				
	H=24cm	26.0	26.0		
		27.0	25.0		
		26.5	25.5		
				I	II
1:59	=16.0	15.0	15.0		
2:06	=25.3	38.5	37.0	0.689	0.689
16	=29.0	46.5	44.5	0.570	0.573
25	^{34.9} =35.0	57.0	56.0	0.465	0.455
33	=39.0	62.5	60.5	0.424	0.422
40	=42.5	67.5	63.5	0.393	0.402
50	=45.0	70.0	66.5	0.378	0.387

Filling from #6. #6 empty; filling from #5
 #5 empty; filling from #4.
 Stopped filling from #4
 Stopped filling from #4 (23cm left); filling from #3

Conclusion - 10" stainless reactor. untamped, isotropic at maximum height (45cm).
 + probably will not be at ∞ length.

Check of zero of sight glass showed it to be reading 2mm too low.

INVENTORY	H _x					
1	250	13.7	10" cm	= 16.9	9" cm	= 21.4 8" cm
2	"	13.0	"	= 16.0	"	= 20.2 "
3	"	14.2	10" cm	= 17.5	"	= 22.1 "
4	"	13.0	"	= 16.0	"	= 20.2 "
5	"	13.0	"	= 16.0	"	= 20.2 "
6	"	13.0	"	= 16.0	"	= 20.2 "
7	"	9.9	"	= 11.1	"	= 14 "
8	"	3.0	" + DV	= 3.7	"	= 4.7 "
9	60	?				

11/30/48 DC
 $H = 45.0 + 0.9 = 45.9$ cm
 $H/x = 499$ at $q = 1.07$
 $W \times 10^4 \approx 4.88$
 0.0522 gm/(cc)
 $V = 23.25$ cc
 $M = 1.21$ kg.
 Estimated
 $H_c = V_c = M_c = \infty$

EXPERIMENT 147

4/27/48

Pusaer

9" STAINLESS REACTOR - TAMPE, H/K = 500 (493.6)

Fox

Gromi
Calkin

Instruments # 3 x 100, # 4 x 10, # 5 x 1, RE - 25 mV.
 Trip points # 3 - 84 x 100 # 4 5.5 x 100
 Source 15 cm from reactor bottom -

	I	II	M ⁻¹		
8:48A					Filling from #8.
:55	H = -0.1 m	3.5	3.5		
		3.5	3.0		
9:05	= 4.2	3.5	3.3	I	II
11	= 15.4	5.5	4.0	0.637	0.825
20	= 20.0				
24	= 25.0	12.0	9.0	0.792	0.367
32	= 30.1	15.0	11.5	0.233	0.287
42	= 35.9	19.5	15.5	0.180	0.213
52	= 39.3	21.0	18.0	0.167	0.183

#8 Empty; filling from #6 -
 #6 Empty; filling from #5
 #5 Empty; filling from #3 -

Upper surface of top layer at top of reactor

Conclusion: With available cylinder height system was not critical and probably would not be at ∞ extensions.

Solution returned to cylinders as indicated on preceding pages.

11/30/48
JC

$H = 39.3 + 1.2 = 40.5 \text{ cm}$
 $H/K = 499$ (see preceding page)
 $V = 16.62 \text{ d}$
 $M = 0.87 \text{ kg}$

Estimates

$H_c > 75 \text{ cm}$
 $V_c > 31 \text{ L}$
 $M_c > 1.6 \text{ kg}$

144
4/27/48

EXPERIMENT 148

Cromin

8" Al Reactor, Tamped, $H/x = 500$ (493.6)

For

Pressure
Calculation

INSTRUMENTS 3x100 4x10 5x2 RE - 25ms.
TRIP PTS same as 147 -
Source 15 cm from bottom of reactor -

Time	H	I	II	Filling for #8		Notes
10:50 A						
57	H = -0.5 cm	3.0	2.5	I	I	
		3.0	3.0			
		3.0	2.8			
11:05	H = 5.6 cm					#8 EMPTY #6 - Supply -
16	= 15.1 "	5.5	4.5	0.546	0.622	
25	= 25.1	8.5	7.0	0.353	0.400	#6 Empty; filling for #5
33	= 35.2	11.0	10.0	0.273	0.280	
41	= 45.4	14.0	13.0	0.214	0.215	#5 EMPTY; filling for #4
51	= 55.1	16.0	13.5	0.188	0.207	(10.5 in. high 4) filling for #3 -
12:04 P	= 72.8	16.0	14.5	0.188	0.193	

Conclusion: 8" Al reactor - Tamped $H/x = 500$ NOT CRITICAL AT ∞ LENGTH -
With 8" Al reactor - sight glass reading are 2mm low.

INVENTORY	H/x	Reading	Correction	Result
1	500	13.7	- 10" cm	= 6.1 - 15" cm
2	-	13.0	"	= 5.8 -
3	-	14.2	"	= 6.3 -
4	-	13.0	"	= 5.8 -
5	-	13.0	"	= 5.8 -
6	-	13.0	"	= 5.8 -
7	-	9.9	"	= 4.4 -
8	-	3.0	" + D.V.	= 1.3 -
9	60	?		

11/30/48 DC
Sight glass correction
 $H = 72.8 + 0.2 + 1.5 = 74.5$ cm
 $H/x = 499$ (see following page)
 $V = 24.15$ l.
 $M = 1.26$ kg.

Estimated. $H_c = M_c = V_c = \infty$

EXPERIMENT 149

5/10/48 ¹⁴⁵

15" STAINLESS REACTOR, TAMPED, $H/X = 493.6$

Visner
Pessley
Fox
Cronin
Caalihan

Bottom of central skirt at level of reactor bottom when scale = 5 cm.

Source - 5 cm from bottom of reactor -

Trip points #3 - 85 x 100; #4 - 6.5 x 100.

Instruments #3 x 100, #4 x 10, #5 x 2, RE - 25 ms.

3:15 p

Filling from #8

3:20 p	H = 0.8 cm	I	II	#8 MT @ 1.8 cm.
		5.5	3.5	
		<u>5.0</u>	<u>3.0</u>	
		5.25	3.25	

3:37	H = 4.0	6.0	3.0	I	II	Filling from #7
			0.88	1.10		
3:40	H = 6.4	NG	4.0	-	0.77	#7 empty.
		NG	4.5			

Filling from #6

4:02	H = 10.1 cm	11.0	7.0	0.50	0.46	#6 empty at 12.2.

filling from #5

4:13	H = 13.8 cm	21.5	13.5	0.24	0.24
:25	= 15.3	30.5	20.5	0.17	0.16
:35	= 16.9	54.5	33.5	0.096	0.093
:45	= 18.3	116.0	78.5	0.045	0.045
:55	= 18.8	200.0	126.0	0.026	0.026

stopped filling from #5 - Filling from #3

5:03	H = 19.25	444.0	278.0	0.012	0.012
------	-----------	-------	-------	-------	-------

5:13 = 19.40 Not critical.

5:18 H = 19.7 Critical with Cd. sheet 18 cm from bottom of reactor.

Consider 19.6 cm just critical (= 19.0 cm when corrected for skirt glass zone).

Conclusion: 19.6 cm is critical in 15" cylinder of stainless steel at $H/X = 493.6$, tamped.

Draw back same as Exp 148

11/17/48
17/28/48
 $19.0 + 0.4 = 19.4$
 $19.4 + 0.4 = 19.8$ = He bottom corrected.
 $H/X = 494$

15" stainless, tamped.
 $\rho_{app} = 1.07$
 $H/H_0 X = 4.88 \approx 0.05229 m^2 / ce$
 $V_c = 22.80 \text{ L} \cdot 22.12 \text{ L}$
 $M_c = 119 \text{ kg} \cdot 1.15 \text{ kg}$

146 5/11/48

EXPERIMENT 150

15" STAINLESS REACTOR UNTAMPED $M/\bar{K} = 494$

For
Pressure
Mann
Martin
Carlson

Control rod in position. zero = zero.
Source: 8cm from bottom of reactor.
Trip point - #3 - 85 x 100, #4 6.3 x 100.
Seals - #3 x 100, #4 x 10, #5 x 2 RE 25 wt.

11:25A

Filling from #8.
Ck's zero of sight glass - 0 = ~~rod~~ edge of 6mm
i.e. all sight glass readings are 6mm high

	H = 0.7cm	I	II	M+	I	II	
		26.0	17.0				
		29.5	16.5				
		<u>27.8</u>	<u>16.8</u>				
11:35	= 2.0						#8 Empty at 2.0. filling #4
47	= 7.5						#4 " " 7.5. filling for #7
55	= 12.2	22.5	15.0				#7 Empty - filling for #6
12:03P	= 15.0	39.0	23.5	0.713	0.716		
10	= 17.7	60.5	38.0	0.459	0.442		#6 Empty filling for #5
18	= 20.0	95.5	57.0	0.291	0.295		
30	= 22.4	161.0	96.0	0.173	0.175		0.8cm ext Stopped filling from #5; filling from #3
37	= 23.9 = 24.9	270.0	151.0	0.103	0.111		
40	= 23.9	215.0	129.0	0.129	0.130		Control rod in - (= 0.5cm sel).
48	= 24.9	372.5	228.0	0.075	0.074		
11:00	= 26.0 = 26.5	131	437	0.038	0.038		(2.4cm) Stopped filling from #3, filling from #2.
10		Not gas critical.					
15	= 26.8	"	"				
18	= 27.0	"	"				
25	= 27.2	"	"				
30	= 27.3	Critical					8cm Cd rod below solution surface.

Conclusion - 15" Reactor - $M/\bar{K} = 494$ - Untamped - Critical at ~~27.6~~
(27.2 - 0.6) = 26.6 cm (corrected for sight glass zero).

Drambeck - Same as on page 144.

11/7/48 De 26.6 + 0.4 = 27.0 cm = Hc bottom corrected.

11/28/48 De $M/\bar{K} = 494$ 499

15" Stainless, untamped.

$\rho/\rho_0 = 1.07$

Wt % Y = 4.88 = 0.0522 gm/cc

$V_c = 30.78 L$

$M_c = 661 Kg$

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Page 8 Current measurements on Safety Rod and
Dump Valve Magnet

